

# BUFFALO FAN SYSTEM

# Heating, Ventilating and Humidifying

CATALOG No. 700

# Buffalo Forge Company

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# FOREWORD

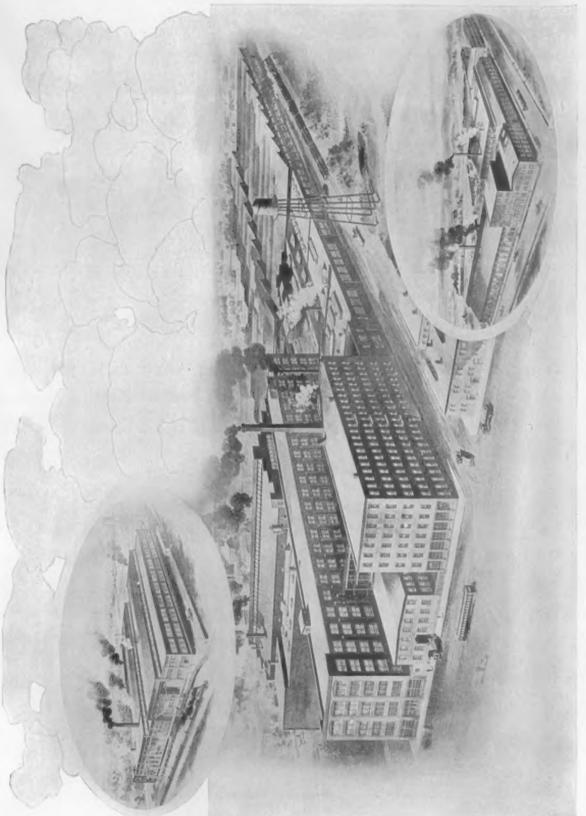
HE Buffalo Forge Company has always taken the stand that engineering data and developments should not be hoarded as hidden treasures but should be made available for the use and edification of the engineering profession in general.

In this volume we have laid stress on the principles underlying all the various steps in the determination of suitable apparatus to meet all conditions of heating, ventilating and humidifying. These principles have been proven by actual practice and are the ones used by our own engineers in the solution of problems of a similar nature.

To the host of friends who gave our previous Catalogs Nos 197 and 198 on Heating and Ventilating such a hearty reception we respectfully dedicate this volume.

Renew our acquaintance by letting our engineers help you with any problems you may have in Heating, Ventilating and Humidifying.

BUFFALO FORGE COMPANY



# THE BUFFALO FAN SYSTEM Heating, Ventilating and Humidifying

#### PART ONE

#### Public Buildings

T has been within the last decade that the heating and ventilating art has come into its own. Many articles had been written on the subject and its importance insisted upon in theory, but unfortunately theory and practice had taken diverging paths. Through the earnest endeavors of the leading engineers. architects and physicians practice has now been made to accord with theory.

The following pages will serve not only to emphasize the importance of proper heating and ventilating but will describe such methods and apparatus as our engineers have used with great success in its attainment.

Years ago when our methods of living and working followed the natural lines

and modes, usually those of least resistance, no need for ventilation other than by natural means was required. As our methods have become more artificial it has been found necessary to introduce artificial means to provide not only ventilation. but heating as well.

The progress of heating can be followed step by step from the rude fire of twigs down through the open fire place, the wood stove, and finally to the present day heating with steam, hot water and hot air. The development of methods of ventilation has been somewhat slower. The day when the opening of a window was ample ventilation has long since passed, and today we have grown accustomed to artificial means, such as fans, to supply positive ventilation.

#### Natural vs. Mechanical Ventilation

However there are very often times when some city official will fly up in arms and declare that the old style ventilation, that of the open window, is by far the best. It might be well at this point to give briefly the results obtained in a recent test. Taking a modern school, one half was ventilated by purely natural means, whereas the other half depended upon mechanical ventilation. Classes were conducted in the rooms under these conditions and observations taken at frequent regular intervals.

It was intended that these tests should cover the greater portion of one school year in order that all weather conditions might be experienced. The attitude of the teachers and pupils toward these tests was most favorable at the start and in



many instances certain teachers and pupils made their own choice as to whether they should be in naturally or mechanically ventilated rooms. Before the end of two months it was found necessary to discontinue the tests, this being due to the fact that teachers and pupils could not work to advantage in the naturally ventilated rooms and such stern objection developed that the tests could not be continued. The chief objections to natural ventilation were summed up by the impartial observers as follows:

- 1. "It was found impossible to keep the temperature and air motion conditions in the naturally ventilated rooms within the bounds of comfort.
- 2. The absence, because of illness of both pupils and teachers, in naturally ventilated rooms increased to an alarming extent.
- The air in the naturally ventilated rooms was for the most part stagnant and heavy which caused depression and headaches."

Although these tests are not conclusive due to the short time over which they extended it is very plain to see that no logical arguments can be advanced for any comparison of natural with mechanical ventilation.

The more crowded a building is, the more complex becomes the problem of ventilation, for the exit and entrance of air must be complete and uniform throughout and at the same time all objectionable drafts must be avoided. With mechanical ventilation we are able to place the air just where it is needed and in just the right quantities and to remove all foul air as fast as it becomes objectionable.

Let us now consider what constitutes good ventilation and how it may best be attained.

#### Ventilation

In the human body, as well as in other animal organisms, life is sustained by a process of combustion in which the oxygen of the air is combined with the hydrogen and carbon of the food and carbon dioxide is formed as a result of this combustion. Therefore, a continuous supply of air with the proper amount of oxygen is just as essential to the sustaining of life as it is to the combustion of fuel under a boiler. We cannot, however, solve the proper amount of air to sustain life by any chemical formula, inasmuch as the "Livable" limit is reached long before the chemical limit.

The percentage of carbon dioxide in the air is a good indication of its state of purity but the exceedingly harmful effects of impure air are not entirely governed by an excess of carbon dioxide. Physicians have shown that the poisonous effect of respired air is due almost entirely to the organic matter exhaled from the lungs. The following table gives the comparison of pure air and respired air.

	Pure Air	Respired Air
Oxygen	20.35%	16.2%
Nitrogen	78.10	75.4
Carbon Dioxide	0.03 to 0.04	3.4
Water Vapor	1.5 Variable	5.

The respired air is immediately diffused in the air of the room and cannot be directly removed, therefore the air must be continually diluted till it ceases to be harmful. There is no definite standard of purity and any line drawn between good and poor ventilation is purely arbitrary. Pure air contains from three to four parts of carbon dioxide in 10,000. With an increase to 11 parts in 10,000 the air becomes noticeably opressive whereas an increase of three or four parts to a total



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of six or seven parts is scarcely noticeable. Modern practice has been to consider good ventilation to exist when the air supply is so maintained that the total quantity of carbon dioxide does not exceed more than six to eight parts in 10,000.

It is estimated that the average adult at rest breaths 500 cu. in. of air per minute and exhales 17 cu. in. of carbon dioxide. From these figures we can determine the air supply necessary to maintain any standard of purity according to the following table.

# Cu. ft. of air to be supplied per person for various standards of purity of air

Parts Carbon Dioxide in 10,000	Cu. Ft. air per min. per Adult		Per cent. of Respired Air
5	100		0.29
6	50	1	0.58
7	- 33.3		0.87
8	25		1.15
9	20		1.45
10	16.7		1.74
11	14.3		2.03
12	12.5		2.32

There are certain applications where more than the normal amount of air is necessary due to unusual conditions. The following table gives the air supply per person under various conditions.

#### Specifications of usual air supplied per person

-										7											a. ft		
Hospitals (Ordinary).		6 6	6 0	0 0		 	 		2			 10	0 0	0 0	9	0	0 1	p p		0	.35	to	40
Hospitals (Epidemic)																							
Workshops																							
Prisons					* *	 * 0				 	 	 ,					w 3		-		.30		
Theaters	1 1 1					 		4					- 0								. 20	to	30
Meeting Halls																							
Schools (per child)																							
Schools (per adult)						 				 	 a .		0 5	0 0		0			0		.40		

Dr. E. Vernon Hill has devised a very good method for determining the effectiveness or efficiency of ventilation.

This is done by using the Synthetic Air Chart shown on page 8 and we will quote Dr. Hill's explanation of its use.

#### The Synthetic Air Chart

"This chart is designed as a convenient method of recording data and arriving at a final percentage of perfect ventilation. It serves as a standard, or measuring "stick" as it were, for determining the efficiency of a ventilating equipment, and eliminates personal opinion and guess work. The chart includes all of the known factors that influence the ventilation of a room. They are as follows: Temperature and humidity, which are recorded as the wet bulb difference; dust, bacteria, odors; air supply and distribution as measured by the CO<sub>2</sub> content. These factors, furthermore, are each given their appropriate weight or value as a part of the whole. If all the factors are ideal the percentage as shown by the chart will be 100. If all or any one of the factors represent conditions that are not ideal the final percentage will be reduced in a corresponding amount.

After the results of a test are plotted on the chart we can see at a glance the final percentage of perfect, and if the results are not what they should be



WET BULB DIFFERENCE		PARTICLES PER CUTOOT	1000 1000 1000 1000 1000 1000 1000 100	40%	BACTERIA COLONIES 730 MIN PLATE	RIA	ODORS PERCENT FREE FROM	PROT	PALE	08	8	SUBSTANCE	DISTRIB PERCINE OF PERCENT PERFECT	SAN E	800
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STATION	TEMPE	RATURE	200	AIR		BAC-			SUPPL	Y REGI	STERS	EXHAU	JST REG	ISTERS	
MAIIQE	DRY BULB	WET BULB	R.H.%	MOTION	DUST	TERIA	ODORS	CO <sub>2</sub>	AREA \$	VELOCITY	C.E.M.	AREA 16	VELOCITY	CEN	
1	70	540	34	35	5730	5	90	81	1.4	600	840	1,25	170	212	
2		53.5		35		2	90	7.2	1.4	520	728	1.25	140	175	
3		54.0		32	3680	5	90	6.1				1.25	130	163	
4								-				125	140	175	
5															
6															
7															
8															
9															
10	69.6	538	33.5	34	4705	4	90	7.1			1568			725	
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the factors that reduce the final percentage are at once determined. The longer the test line in any column the less favorable are the conditions represented. When the test line disappears conditions are perfect.

Under each factor there are three columns, a plus percentage column; the factor column proper, and the minus percentage column. The factor column proper is divided into appropriate units of measurement, as degrees for temperature, particles per cubic foot for dust, colonies for bacteria counts, etc.

The plus percentage is the percentage of perfect for the specific factor in the column; for example, in the chart shown in the illustration the dust count is 5,000 particles per cubic foot. This gives a plus percentage of 98, meaning that so far as dust is concerned the air is 98% free.

Reading the minus dust column we find the percentage as a part of the whole chart is only one-half of one per cent. This one-half of one per cent., together with the other minus percentages from the various columns, is deducted from 100 in arriving at the final percentage for the entire test.

The curves at the bottom of the chart headed 'Temperature, Humidity and Air Motion' are for determining the wet bulb difference. To do this proceed as follows:

Mark a point on the curve indicating the wet bulb temperature determined by test. This point should be located at the intersection of the wet and dry bulb lines. This is done as a matter of convenience, as the point will then give the wet bulb, the dry bulb and relative humidity.

Next mark by a point on the line denoting the physical state of the occupants, the air motion from the test. This point will be at the intersection of the appropriate physical state curve designated by 'At Rest,' 'Light Work,' 'Moderate Work' and 'Hard Work' with the vertical line of air motion. The vertical distance between the two points is the wet bulb difference, that is, it is the variation in degrees between what the wet bulb should be and what it actually was by test. This wet bulb difference is plotted in the first column of the chart.

The distribution factor is the percentage of distribution in the room. It is determined by an analysis of the air samples at various points for CO<sub>2</sub> and the average of all samples taken is the average distribution for the room.

The percentage of distribution is the percentage of variation of the different samples from the average.

The reverse side of the chart, illustration No. 2, is arranged for recording test data."

#### HEATING

Closely associated with the problem of proper ventilation is that of satisfactory heating, in fact it is very hard to draw the line of separation between the two problems.

#### Room Temperature

The physical principles involved in heating buildings are more complex than usually supposed, and exhibit an admirable nicety in the balancing of forces.

The first factor to be considered is the heat generated by the human body and the methods for its disposal. These are important conditions which determine the most desirable room temperatures and in densely peopled buildings, largely determine the result of vital processes dependent in part upon the activity of the individual. This amount of heat extends over considerable limits as shown by the following table.

Child six years old	В.	T.	U. per	hour.
Adult at rest	-	3.0	4.6	11
Adult at work		4.6	4.8	4.6
Man 30 years old in an atmosphere with a temper-				
ature of 68° F	)	44	1.1	11
The same in a atmosphere of 51 F	,	6.6	44	w *1
Woman 32 years old	)			
Adult in old age360	)	× 4	4.4	0.0

We have found that a good average value for the amount of heat in B. t. u.'s given off per person per hour in an atmosphere of 70°F. is 400 for adults and 200 for children, these figures being generally used when the heating of densely peopled buildings such as schools and auditoriums, is considered. The average normal temperature of an adult in health is 98° F. and since heat is continually being generated, it must be disposed of as fast as generated. This disposal may be accomplished in three ways:

First: By direct transmission or radiation to the surrounding air. Second: By the absorption of heat in the evaporation of perspiration.

Third: By the evaporation of moisture through the lungs.

Radiation depends upon the difference in temperature between the body and the surrounding air, but it is also affected by the amount of clothing and the humidity of the air. It is evident that the temperature of the room should not be so low that the body will radiate more heat than produced under normal conditions. In fact, from a hygienic standpoint, less heat should be absorbed than is generated, thus allowing part of the heat to be absorbed by perspiration. The following room temperatures have been found to give the best results.

Public buildings					68 to	72° F.
Machine shops					60 to	65° F.
Foundries, boiler shops and all	places	where	physical	labor is done	50 to	65° F.

#### Heat Losses

In order to maintain a fixed temperature within a building, it is necessary to supply heat in sufficient quantities to compensate for the heat loss through the walls and roof of the building, and also to heat up the outside air brought in for ventilation. The subject of heat transmission in buildings has been thoroughly investigated so that the laws governing it and the factors for heat transmission of various building materials and building constructions are now quite accurately known. It has been found that the loss of heat by transmission is proportional to the difference of the temperature on the two sides of the material. The table on page 109 shows the accepted factors of heat transmission.

#### Humidity

The amount of moisture that a given quantity of air can hold increases very rapidly with the temperature. The amount per cubic foot of air is the measure of its humidity and this humidity has a great bearing upon livable conditions in schools and public buildings. It may be to advantage to explain at this point how the relative humidity of air may be determined. If a thermometer bulb is covered with a damp cloth a drop in apparent temperature of the surrounding air will ordinarily result. This temperature is called the sensible or wet bulb temperature. The less the humidity the greater the difference between the actual and the sensible temperatures, while at 100% saturation they are the same.



To determine the wet bulb and dry bulb temperature a sling psychrometer is used. This is clearly shown in the cut and consists of two thermometers, one having the bulb covered with a thin gauze. In taking the readings the gauze is moistened and the psychrometer is then rapidly whirled around until the mercury readings in the two thermometers stay constant. It is essential that the instrument be moved rapidly or held in a current of air for an air movement across the wet bulb is necessary to obtain a true reading.

From the hygienic standpoint it is evident that the means for regulating the humidity is just as important as the problem of proper ventilation and proper heating in every school and public building.

#### **Psychrometric Charts**

The relation between the temperature as measured by the wet and dry bulb of air and the moisture content is clearly shown in the psychrometric chart on page 13. It will be seen that a cu. ft. of air at 70° will hold eight grains of moisture while at 32° it will

hold only two grains and at zero only five-tenths of a grain. The normal limits of humidity vary from 50% to 75% of saturation. It has been found that when the humidity goes above or below these points the condition becomes very uncomfortable and in fact injurious to health. Hence, it will be seen that air at 70° should contain from four to five and one-half grains of moisture per cu. ft. to be in the best condition for ventilating purposes. In the ordinary methods of heating with the air temperature 32° outside, the humidity of this air when heated to 70° without the addition of any moisture would be only 15.5% which is far less than the humidity of the driest climate known. It is this extreme dryness of the air in a heated room which produces the commonly noticed discomforts, such as extreme thirst, a parched feeling in the nose and throat, lassitude and headache. This extreme dryness has been a contributing source to many throat and pulmonary diseases.

The Psychrometric Charts on pages 16A and 16B are taken from the catalogue of the Carrier Air Conditioning Company of America, one of our associates in business. These two charts should be used when calculations are made in terms of pounds of air, while the chart on page 13 should be used when the pound cubic foot is a unit. For most purposes of calculations it will be found preferable to use the pound as a unit.

The various curves shown on these charts will be found especially valuable in making air calculations. The grains of moisture per pound of dry air are read by passing directly from the dew-point, or intersection of the wet- and dry-bulb temperatures, to the scale on the left edge of the chart. The B. t. u. required to raise one pound of dry air one degree when saturated with moisture, as also the vapor pressure, may be determined by passing vertically from the dew-point to the proper curve, and then to the corresponding scale on the left edge of the chart. The total heat, in B. t. u., above zero degrees contained in one pound of dry air saturated with moisture may be found by passing vertically from the wet-bulb temperature to the total heat curve and then to the left edge of the chart. The volume of air in cubic feet per pound may be found by passing vertically from the dry-bulb



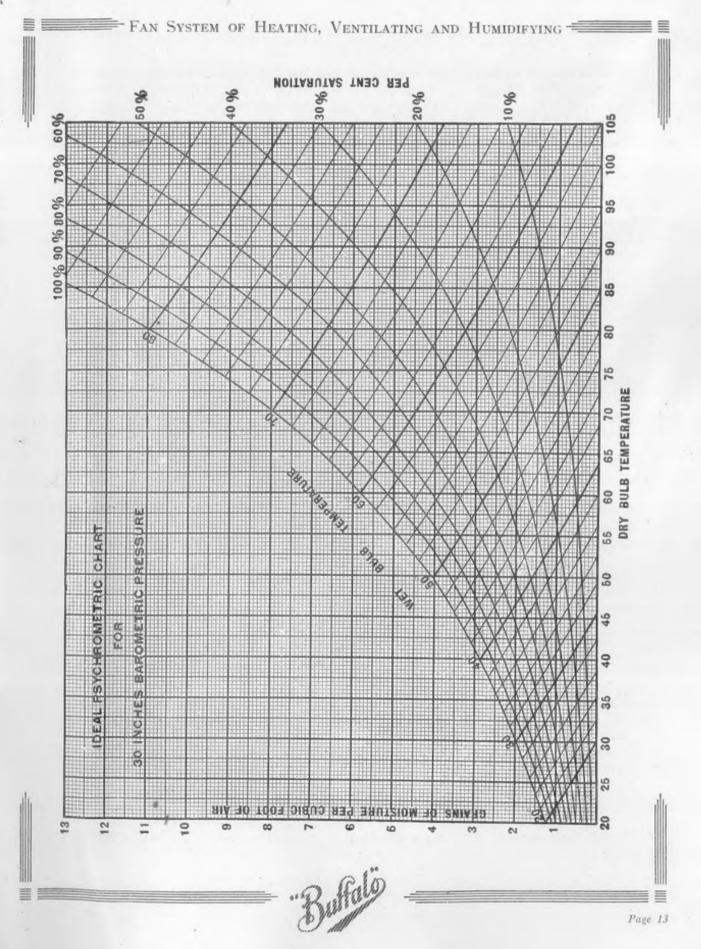


temperature to either of the two volume curves and then to the left edge of the chart. One curve gives the volume of dry and the other of saturated air.

Example. As an example of the use of this chart we will assume air at 75° dry-bulb temperature and 60 per cent. relative humidity. From the chart we find that the wet-bulb temperature will be 65.25°, the dew-point 60°, the grains of moisture per pound of dry air 77; the heat required to raise one pound of dry air saturated at 60° through one degree is 0.24664 B. t. u.; and the vapor pressure of air saturated at 60° is 0.523 inches of mercury. Passing vertically from the wet bulb temperature of 65.25° to the total heat curve and thence to the scale on the left, we find the total heat above zero in one pound of dry air when saturated at 65.25° to be 29.75 B. t. u. This, then, is also the measure of the heat in a pound of air at 75° and 60 per cent. relative humidity, since the wet-bulb temperature is the same.

The cubic feet per pound of air may be found by passing vertically from the dry-bulb temperature to either of the two volume curves, depending on whether the volume of dry or of saturated air is desired. To determine the volume of one pound of partly saturated air as here assumed, we will have from the chart.

As an example of the use of the chart on page 13 we will assume a case where the dry-bulb temperature is 80° and the wet-bulb thermometer reads 70°, or a 10° depression. From the intersection of the corresponding lines through these two temperatures we find the relative humidity to be 62 per cent. Passing horizontally to the left from this point of intersection to the wet-bulb temperature line (called the saturation curve) we find the dew-point temperature to be 64.5°. If the temperature of the air should be reduced both the dry- and wet-bulb readings will be lowered until they both read 64.5°, when the air will be saturated. The grains of moisture contained in each cubic foot of this air will be found by continuing to the left on the horizontal line through the 64.5° dew-point to the left edge of the chart, where we have a reading of 6.65 grains. If the temperature of the air be further reduced, part of the moisture content will be condensed, the dew-point or saturation temperature will be lowered, and the grains of moisture per cubic foot will be correspondingly less.



#### Methods of Heating, Ventilating and Humidifying

The old fashioned fire place was the first attempt at heating and ventilating. The draft produced by the large chimney gave ample ventilation, but the heat loss along with this ventilation was very large and hence, as a heating system, the open fire place was most uneconomical. The next step, the old stove, afforded practically no ventilation, although its economy from a heating standpoint was fairly high. The modification of the old stove, namely, the hot air furnace afforded a certain measure of ventilation but this measure was far too limited and unreliable to make its use permissable in large or crowded buildings. A serious objection to the hot air heater is the liability of coal gas leaking into the air. The hot air furnace is the chief offender in heating with extreme dry conditions of air as described in the paragraph on humidity on page 11.

The next step is marked by the introduction of direct radiation with steam or hot water furnaces. Owing to its cheapness this method has been extensively introduced but it provides for no ventilation other than by windows and doors, and the resulting close, stuffy, heated rooms in office and other public buildings have doubtless increased materially the world's death rate.

The use of indirect radiation permits a certain amount of ventilation and elaborate systems have been devised on this basis. Aspirating shafts for removing foul air in connection with indirect systems have given positive results. In the latter system radiators are placed in the ventilating shafts to produce a draft by increasing the temperature of the foul air. The cost of ventilation by this method is expensive and the use of aspiration flues as substitutes for fans is indefensible.

#### The Buffalo Fan System

It is today universally acknowledged that the fan system has solved the problem of the successful heating and ventilating of public buildings. In recognition of this the legislatures of practically all states have passed statutory laws, requiring the use of the fan system of ventilation in school buildings. The question no longer is "Shall the fan system be used?" but "How may it best be applied?"

For the past 35 years the Buffalo Forge Company has been engaged in designing heating and ventilating systems and in the construction of such equipment. This company has its systems in successful operation in thousands of buildings in this country, Europe and Japan, in fact in all parts of the civilized world. The improvements put forth by this company have brought the art of heating and ventilating to a degree of perfection not previously known. One of the most important of these improvements is the Carrier Air Washer and Humidifier, which removes all impurities from the air and imparts to it the proper humidity.

#### Public Buildings

There are two arrangements of the Buffalo Fan System as applied to public buildings.

The first, in which the fan system handles both the heating and ventilating requirements and the second, sometimes called the split system, in which the heating requirements are taken care of by direct radiation in the room and the fan system handles the air required for ventilation only.

The apparatus used in the two applications differs only in the amount of heater surface required. The equipment consists of a boiler for the generation of

steam, a centrifugal fan, driven by an engine or motor, for the propulsion of air, an air washer for purifying and humidifying, a steam radiator for heating and a system of ducts for distributing the heated air and for removing the foul air.

The boiler may be of any customary type and may be operated at any pressure between one-half and 100 pounds per square inch, however, a pressure of 20 pounds is most desirable when a steam engine is used as the prime mover for the installation.

The fan is of the centrifugal type and is usually constructed as an exhauster, i.e., with only one inlet. The use of a steam engine as the prime mover allows for great economy since the exhaust steam can be utilized in the heater, this greatly reducing the cost of power used. The Buffalo heater described in detail on pages 52 and 53 consists of vertical coils of one inch full weight steel pipe screwed in cast iron manifold bases. Steam is supplied to the coils on one side of the manifold and exhausted from the other side, both the inlet and exhaust connections being on the same end of the base. Separate steam and exhaust connections are provided for each of the several sections into which the heater unit is divided, each connection being supplied with valves allowing as many or as few heater sections to be in operation as are needed.

The fan may be placed so that the fresh air is either forced through or drawn through the stacks of heater coils. In public buildings it is the general practice to separate the heater into two parts, one part known as the tempering coils, containing from six to ten rows of pipe, the amount being just enough to heat the incoming air to a temperature of from 60° to 70° before it reaches the washer or fan; the other part known as the heater proper is placed at the fan outlet. The size of the heater is governed by the amount of air to be handled and the temperature required on leaving the fan. Between the tempering coils and the fan is placed the Carrier Air Washer and Humidifier. The air, after being tempered, cleaned and humidified is discharged under pressure into two chambers known as the hot and tempered air plenums, respectively. In the hot air plenum chamber are placed the heater coils, while the supply to the tempered air plenum is carried by a by-pass either above or underneath the heater. In the split system no by-pass around the heater is necessary. After leaving the heater the air is distributed by means of ducts leading to the room to be heated and ventilated.

It is customary to place the outlet registers so that the heated air enters the room about eight feet above the floor, this height being sufficient to prevent drafts and still allow for the proper air velocities through the registers. The cold or foul air is removed by vent registers placed at the floor line usually on the same side of the room as the hot air flue. The heated air enters above at a higher temperature than that of the room, and a complete and practically uniform diffusion to all parts of the room occurs. The cooling effect of the outer walls and windows produces a downward circulation at these points with a consequent flow from the hot air registers toward the outer wall in the upper stratum, and a flow from the outer walls to the vent registers in the lower or breathing stratum. This flow occurs over such large areas that the velocity is most imperceptible.

Inasmuch as the heated air is positively supplied to the room, the foul air must be positively forced out through the only channels available, namely, the vent register, flues, and leakage cracks around the windows and doors in the outer walls.



Exit by the latter means is necessarily restricted in properly constructed buildings, but it serves the purpose of preventing the undesirable infiltration of cold air which would otherwise occur. The above method is often spoken of as the plenum system.

It is just as important to positively remove the foul air as it is to positively introduce the fresh air but the same progress has not been made in this end of ventilation. The usual method is to have vertical flues with roof ventilators and depending entirely upon the stack effect to remove the foul air.

Many of the best installations provide a supplementary fan system for exhausting the foul air.

#### Advantages of the Buffalo Fan System

The contrast between the methods and effects of the old system of direct radiation depending upon windows and doors for ventilation on one hand, and the Buffalo Fan System of Heating and Ventilating on the other is very striking. With direct radiation all air for ventilation must be admitted at the windows through the lower sash. This is made necessary because any opening of the upper sash will allow the escape of the stratum of heated air in the upper parts of the room. This method is both unsanitary and uneconomical. It is unsanitary, first, because it is impossible to admit sufficient fresh air by means of windows without objectionable drafts; second, the ventilation is not uniform, and depends entirely upon atmospheric conditions outside the room, being mostly affected by the direction and velocity of the prevailing winds; and third, an undesirable layer of cold air tends to settle along the floor, which does more harm than an entire lack of ventilation. It is uneconomical because the coldest air remains along the floor, and the heated air rises and flows out of the window openings. The heated and cold air do not get an opportunity to intermingle and most of the heat produced is not used to advantage. Further the heat is not equally distributed, the better ventilated parts of the room are too cold, and poorly ventilated parts are too hot; the room temperature cannot be kept uniform or regulated to any extent and the loss due to overheating is great.

The Buffalo Fan System, on the other hand, is sanitary and economical and overcomes all the objections voiced against natural ventilation, because it maintains a uniform temperature, prevents all drafts and secures a warm floor. It is economical, because the temperature is readily and absolutely controlled either automatically or by hand, and any overheating is prevented. This latter advantage is very much greater than is generally supposed.

#### Carrier Air Washers

One objection that is frequently raised to the use of the fan system is that dust is drawn in with the air and blown into the room. This objection can be very easily overcome by the Carrier Air Washer which positively removes all traces of dust, soot and smoke, and the foulest germ-laden air of the city is thus made as clean and pure as that of the country. The advantage of this process wherever cleanliness and sanitary conditions are desired is easily appreciated and renders this system particularly valuable in libraries, hospitals, schools, in fact in all buildings where clean air is a requisite.

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING :



These pails contain dirt, mud, soot, bacteria of various sorts, and disease-breeding filth of all kinds which was washed from the air used for ventilation of Public School No. 6, Brooklyn, New York, and shows the result of one week's run of the Buffalo Fan System.

This mud was shoveled from the bottom of the Carrier Air Washer settling tank after the water had been drained off. Of course all the finest dirt floating in the water had been carried off.

Had it been possible to strain the water as it was drained, no doubt five more pails would have been filled. These pails each contained approximately twenty-five pounds of dry dust so this washer was collecting approximately one hundred and twenty-five pounds of dirt-carrying disease every five days.

Another big advantage of the air washer is that the humidity of the air used for ventilation can be positively controlled. The advantage of this has been described under the subject of humidity on pages 10 and 11.

#### **Humidity Control**

The Carrier Air Washer and Humidifier described on page 50 effectively overcomes the dryness of ordinary heated air and places the humidity of the air under accurate and automatic control. In this system the humidity of the air entering the building is regulated to the finest nicety through the control of the temperature of the spray water.

This method of regulation is the only simple and direct form of humidity control. By means of the spray water temperature regulation every demand for variation is immediately taken care of and there is no delay between the demand and response as is evident in all other methods of regulation. The temperature of the spray water is raised by the introduction of steam through a device similar to an injector, or by a closed water heater.

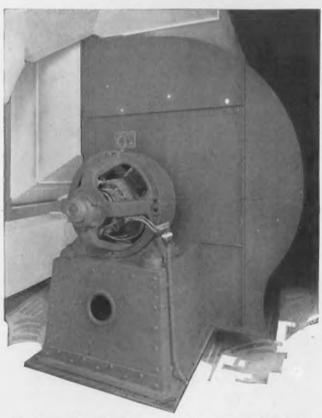
It has been proven by numerous tests that the temperature of the spray water is a greater factor in the amount of moisture which the air will absorb than the temperature of the air itself.

Regulation of the temperature of air entering the ventilating system as a means of controlling the amount of vapor absorbed is inadequate, and attempts to secure a constant relative humidity by regulating the temperature of the body of water in the settling tank of the air washer fail on account of the time element before this water is sprayed into the air. In these and other systems two thermostats jointly aim to give the control desired, bringing in a double error, and a considerable lag of regulating effect behind the outside atmospheric changes which cause it.

The Carrier Dew-point System of humidity control uses one thermostat of very simple and accurate design exposed to the temperature of the washed air, controlling directly the temperature of the water as it is sprayed, not of the whole volume of the settling tank. There is no lag, cause brings instant effect, and literally any relative humidity may be maintained automatically.

Reduction of the humidity is not desirable except for special processes in the industries, but may be accomplished by the use of refrigeration for cooling the spray water. The average winter temperatures in our Northern States set a practical upper limit for humidity at 40% to 45% above which the coldest weather will cause condensation on windows. See discussion on page 30.

The Dew-point System indicates by its name that the air must be saturated, thus fixing absolutely the number of grains of moisture per cubic foot at a given temperature which leaves only the temperature of the saturated air to be controlled. No air washer that will not give saturation can be used with the Dewpoint System, but Carrier Air Washers have spray systems which make saturation possible when using heated spray water.



Buffalo Ventilating Unit in Bowery Branch Y. M. C. A., New York City



Page 18

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

#### Hospitals

The necessity of ample ventilation in hospitals is not receiving the proper attention by those most concerned. Although absolute cleanliness is paramount in the mind of the physician it is really surprising that this question is so frequently lost sight of when hospital ventilation is considered. This matter is being brought forward by the leading engineers and is gradually coming into its own.

The extreme importance of maintaining the proper humidity in the treatment of certain diseases is just being realized by physicians. In diseases of the heart and the respiratory organs, in fevers and especially in all nervous disorders, patients are extremely sensitive to changes in humidity and adversely affected by the dryness of the air ordinarily existing in heated buildings.

When used for cooling the hospital rooms in the heat of summer the Carrier Air Washer in connection with the Buffalo Fan System proves efficacious and convenient.

#### Libraries

The Buffalo Fan System in connection with the system of air purifying is applied to the heating and ventilation of library buildings with most satisfactory results. Not only does it afford positive ventilation, but it frees the air from all traces of smoke and dust so objectionable in libraries; besides, outward pressure of air in the building prevents the entrance of dust from without.

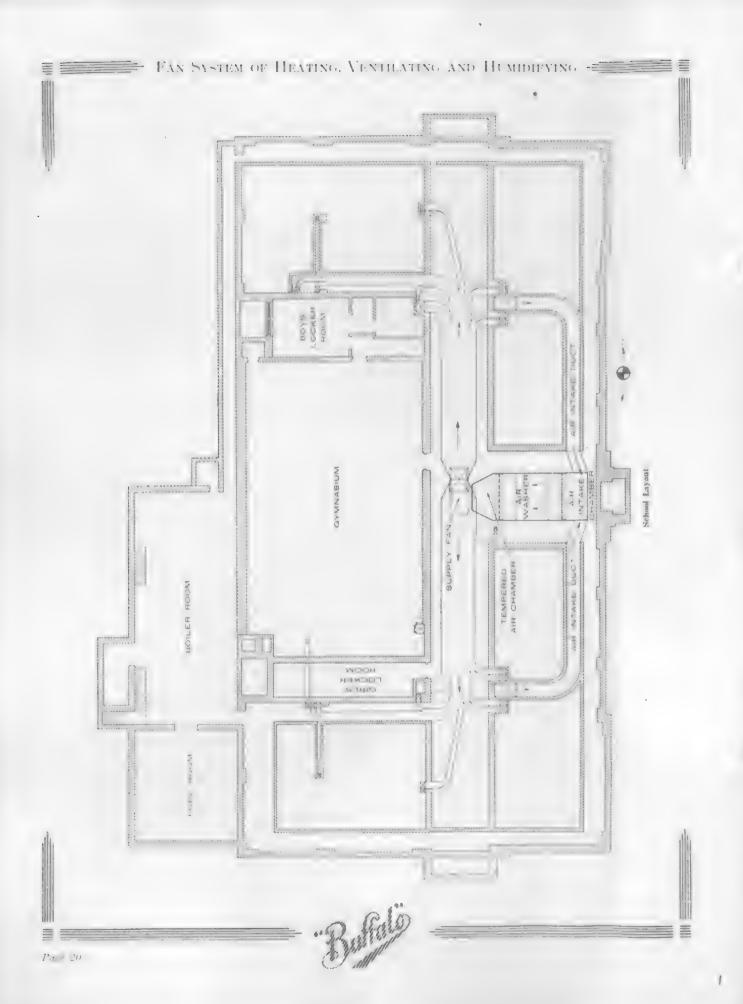
In one instance tests were made of the temperature of the water in circulation and of the air at various points with the results shown in the following table:

#### Carnegie Branch Library, St. Louis, Mo.

Room	2:30	Time P. M. 2:50	3:15
Auditorium, basement	75	75	74
Stall room, basement	79	80	771/2
Stall room, basement	77	77	76
South reading room, main floor	78	78	78
North reading room, main floor	78	78	7814
Stock room	79	80	791/2
Average	77.7	78	77.2
External air			86
Air entering rooms			73
Circulating water	S		69

It is interesting to note the effect of this apparatus in cooling the building. Although the temperature of the external air was 86° F., it entered the rooms at 73, and kept their temperature down to between 77 and 78, a cooling of about 8½°.

During the first two series of readings the windows in the three basement rooms were open. Before taking the 3:15 P. M. reading they were closed. The result shows that the temperature of these rooms was noticeably lowered by excluding the external air and supplying only the washed air from the fan.



FAN System of Heating, Ventilating and Humidifying

#### Application to Schools

The modern school building offers the most exacting requirements in heating and ventilating. The large number of pupils seated in one room require a very rapid air change, and this must be accomplished without causing any drafts. A uniform temperature must be maintained throughout the room and the ventilation must be adequate.

The Buffalo Fan system adapts itself very readily to the accomplishment of the former but the latter is somewhat more difficult to attain. Even elaborate system cannot secure an entirely perfect distribution of air and the only practical and successful method has been to supply air considerably in excess of the theoretical requirements. The necessity of this extra requirement or factor of safety as it might be called, is often overlooked in writing specifications for school ventilation.

Thirty cubic feet of air per pupil, which is the amount usually specified, will keep the CO<sub>2</sub> content down to from six to seven parts in 10,000. This supply would be ample if the air distribution were perfect but it has been found advisable that 40 cu. ft. per minute per pupil be introduced to insure the best results.

The Buffalo System has been installed in schools throughout the world with marked success.





#### Theaters and Churches

Audience halls, such as theaters, churches and lecture rooms though in use but for a short time are as a rule notorious for their poor ventilation. The introduction of the Buffalo Fan System has effectively relieved this disagreeable and unsanitary condition. Owing to the large dimensions of such buildings, and to the density to which they are peopled the problems of air distribution and avoidance of drafts are greatly increased.

Two plans have been found to give the best success in the ventilation of audience halls, these are usually distinguished as the upward and downward systems. In the downward system the air is admitted through registers in the walls at a height of several feet above the floor, and removed through vent registers in the walls at the floor line in the same manner as in school buildings or the air may be exhausted by means of separate disc fans placed in the walls of the building. In the upward method the air is admitted through duct outlets in the floor underneath the seats and is exhausted by means of disc fans in the walls or ventilators in the roof.

The upward method is to be desired wherever the architectural design makes it permissable. A perfect distribution of air can be secured, and the air flow is upward in accord with the natural air currents induced by the heat of the body and the breath. The products of respiration, and eliminations of the body are immediately carried away, and the incoming air is uncontaminated. This method of ventilation is exceedingly efficient, as a high standard of purity can be maintained at the breathing line with a comparatively small air supply. One objection to this system is that the air being introduced at the floor tends to carry up with it all loose dirt which may be raised from the floor by the action of people walking or moving their feet while seated.

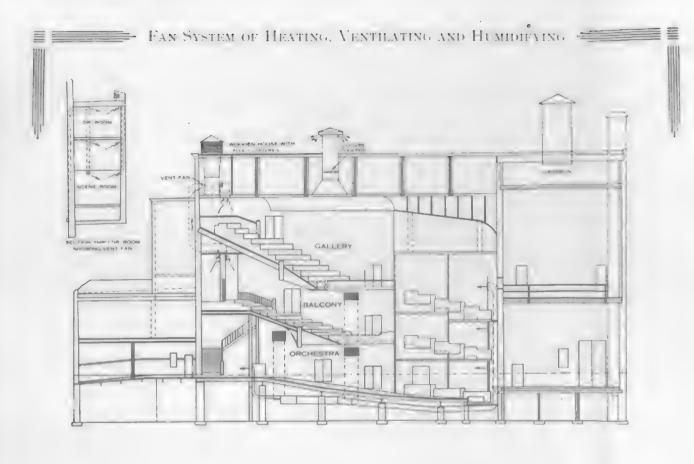
With ordinary precautions as to the cleanliness of the floors this objection is for the most part overcome.

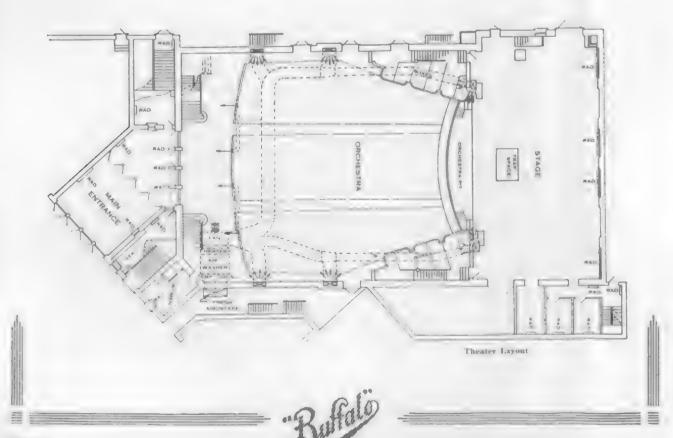
The moving picture theater has offered the largest field for theater ventilation in the last few years. The system most in vogue for these installations is the downward system. The air is introduced through registers in the side wall and exhausted by means of disc fans or ventilators. The ventilation requirements for audience halls and theaters are now very fully covered by legislation in most of the states.

Upward ventilation, to be successful, requires a very careful arrangement of the supply openings on account of the greater liability of drafts. The velocities are necessarily low, and the registers are so small that a very large number is needed to convey the necessary air.

The plenum chamber for supply is sometimes out of the question, and on this account the downward system, which is in almost universal use in schools, is extended to churches, theaters and halls with high ceilings. With a proper arrangement of fresh air and vent registers, and ample air supply excellent results are obtained. To insure such results exhaust systems are frequently relied upon, the vent registers being connected with suction fans which maintain a steady draft.

The design of theaters and churches often prevents the location of vent flues except in outside walls, the cooling effect of which seriously impairs the efficiency of the natural draft. It is always advisable to connect flues so located with suction fans.





Bufalo

In theaters which are in use during the summer, the air washer provides the means of securing freedom from distressing heat. In order to maintain the best cooling effect, refrigerating apparatus for lowering the temperature of the water sprays is sometimes necessary, and may be economically installed and operated, but even without the use of refrigerated water, the cooling effect is considerable and of decided practical value.

The air washer and cooling apparatus enables the temperature to be lowered about 10°, converting the theater from the most uncomfortable to the most comfortable place in warm weather, while in winter it gives a cleanliness and an increased freshness to the air supplied.



St. Paul's Cathodral St. Paul, Minn.

BALL

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

#### Department Stores

Department stores offer an especially useful field for the application of the fan system. In cold weather there exist disagreeable cold drafts along the floors. Although on account of the crowded condition ventilation is most urgently needed, no provision as a rule is made for supplying it. The fan system fills both of these needs, first, by furnishing warmer air in large volumes without the production of drafts, and second, by creating an outward pressure which effectually prevents the entrance of cold air at the doors. The objection to the fan system previously existing on account of the dust carried into the building by the fan is entirely overcome in the Buffalo Fan System by the use of the air purifying apparatus, while at the same time the store is made very attractive in the hot days of summer by the effect which may be obtained when using this system of cooling.

The department stores shown below reap the benefits of Buffalo heating and ventilating systems. The Lord & Taylor installation admirably meets the varied weather conditions of New York City while, on the other hand, the delightful climate of Los Angeles is further enhanced by the Buffalo system in the Broadway Department Store.



# THE BUFFALO FAN SYSTEM OF Heating, Ventilating and Humidifying

#### PART TWO

#### **Industrial Plants**

THE apparatus used in industrial building application is similar to that used in public buildings. The heating system ordinarily consists of three elements, namely; the heater, the fan and the system of air distributing ducts. In such installations where pure air and humidity control is required, an air washer is installed in addition to the equipment mentioned above. The draw through system is most commonly used in industrial work inasmuch as higher velocities are used than in public building application, and also due to the economy effected by the fan discharging directly into the duct system.

#### Heat Losses

In industrial buildings the heat losses are due to two causes; first, by the direct transmission of heat through the walls and exterior surfaces of the building, and second, by the infiltration of cold air from the outside. The loss due to the first cause may be calculated very closely in accordance with the method described on page 74, but the heat loss due to infiltration differs so greatly in various sizes and construction of buildings that no definite rule can be laid down. The allowance to be made for this is necessarily the result of experience and of careful tests of previous installations. The most effective remedy to reduce this loss to a minimum is to maintain a slight pressure or plenum within the building by means of a fan.

#### Fan System vs. Direct Radiation

In all heating systems difficulty is experienced due to the rise of heated air before its heat has been utilized to the fullest extent. This heated air forms a stratum just beneath the roof. In the modern type of factory construction with its height and great amount of skylight surface, the loss due to this action of the heated air may be considerable and its prevention is a serious problem. In direct radiation where the air current is entirely due to the difference in temperature, the attendant loss, which is relatively great, is unavoidable. Practically, the only way in which this heated air can be made use of is by placing the coils next to the wall near the floor, and allowing the heated current of air to pass upward along the walls, but this method is extremely wasteful, due to the fact that part of the heat is applied directly to the walls, causing a loss estimated as great as 25% of the total heat supplied.



Bulfalo

With the fan system on the other hand, the method of distributing the air is entirely mechanical, and thus an opportunity is afforded for utilizing its heating effect to the very best advantage. The method of distribution may be so devised that the effect of a rising current of heated air is almost entirely avoided, this being secured by diffusion of the heated air along or near the floor line.

The Buffalo Fan System possesses a great advantage over direct radiation systems in its flexibility of operation. With direct radiation a building heats up very slowly, and it is usually necessary to maintain a normal temperature all night in order to have it sufficiently warm in the morning. On the other hand the fan system with the proper amount of reserve can heat a building up in a short time. This allows the building to be cooled down during the night to just above freezing point, say an average temperature of 35° or 40° where the manufacturing process will permit.

Another important point of economy in the Buffalo Fan System is the utilization of waste sources of heat. The most common form of waste heat in an industrial building is from steam engines and other steam driven machinery.

The ordinary simple steam engine running non-condensing has a water rate of about 32 pounds per horse power. Of the total heat supplied by the steam only about 20% is utilized in work leaving 80% of the heat unused. A great portion of this remaining 80% is available for use in heating apparatus, a small part being lost due to radiation.

Since the mean effective pressure in an ordinary engine cylinder may be placed at 40 pounds per square inch it will be seen that an increase of one pound per square inch in back pressure will reduce the effective horse power of the engine two and one-half per cent. and correspondingly increase the cost of the power produced.

In a compound engine the effect of back pressure is still more noticeable since the mean effective pressure, referred to the low pressure cylinder, may be placed at 30 pounds per square inch; each pound of back pressure therefore reducing the power of the engine three and one-third per cent. It is therefore unprofitable to introduce any system that will greatly increase the back pressure on the engines.

The ordinary system of direct radiation places a back pressure on the engines which is prohibitive. On the other hand the Buffalo Fan System Heater is designed for use of steam at low pressure and can be operated successfully with one-half pound back pressure on the engine.

#### Heating with Exhaust Steam

The question is frequently brought up whether it is cheaper to run an engine non-condensing and use exhaust steam for heating or to run the engines condensing and use live steam for heating purposes. With the average compound Corliss engine the water rate at full load is about 20 pounds per horse power when running non-condensing and about 14 pounds condensing, so that a saving of 30% in the water rate is effected when running condensing.

The amount of heat available in the exhaust steam is about 80% of the total. Hence it will be seen that the saving of steam when running condensing is only six pounds per horse power, while the heat available in the exhaust steam is equivalent to 16 pounds of steam per horse power and therefore a saving of the equivalent ten pounds of steam per horse power could be saved by running the engine non-condensing and using the exhaust steam in the heater. In this manner a saving is

effected as long as 38% of the steam is utilized in the heater. With engines whose economy is less than that assumed above, the saving effected by running non-condensing and using the exhaust steam in the heaters is even greater.

With the steam turbine the water rate increases much more rapidly with a decrease in vacuum than in the case of the steam engine. A steam turbine having a water rate of 20 pounds of steam per horse power with 28 inches of vacuum will require 50 pounds of steam per horse power when running non-condensing. From this it is readily seen that the use of exhaust steam from a turbine running non-condensing is economical when the heating requirements are more than 60% of the steam consumption of the turbine when running non-condensing.

Besides these distinct advantages in economy over direct radiation there is usually a considerable advantage in first cost in favor of the Buffalo Fan System. This is due in part to the compactness of the system, requiring fewer connections and shorter lengths of steam mains, but more particularly to the great saving in amount of radiating surface required owing to its greater effectiveness in the fan system. A determining factor in the rate of heat transmission of any heating surface is the velocity of air over the surface. This is shown by the curve on page 72, exhibiting the relation between air velocities and heat transmission as determined by accurate tests on the Buffalo Fan System heater. In direct radiation the heat is transmitted by convection currents and radiation only, while with the fan system an air velocity over the coils of from 1,000 to 1,200 feet per minute is usual; the former transmits only from 2 to 2.6 British Thermal Units per square foot per hour, per degree difference in temperature, while the fan system heater as shown by the curve on page 73, transmits from 10.4 to 11.5 B. t. u. per square foot per hour, per degree difference in temperature or about five times as much as direct radiation. Hence a correspondingly smaller amount of radiating surface may be used, which more than offsets the additional cost of fan, engine, and hot air piping.

The question often arises as to the relative cost of heating, ventilating, and humidifying. As an example, assume a fan system of heating in a schoolroom, where outside temperature is 0° and room temperature is to be kept at 70°. Air must be raised to 70° before any heating will be done by it, therefore consider this amount of heat added for ventilation purposes.

The temperature of the air has to be raised still further for heating the room, and it is ordinarily assumed that air entering a room at 120° with outside temperature 0°, will probably take care of heating requirements, and also furnish a sufficiently rapid air change.

Accordingly 70° of 120° total or 58%, is used for ventilation and 42% for heating; and approximately the cost of ventilation is 60% and the cost of heating 40%, where humidifying is not considered.

Assuming that this same proportion holds for other temperatures, when the outside air is 40° and the room is to be kept at 70°, 30° or 58% is the amount of heating required for ventilation, and 22° or 42% for heating; and temperature of air entering the room should be 92°.

The amount of moisture which air will contain depends on its temperature. The amount of moisture actually contained at any temperature is called the absolute humidity; and the ratio of moisture which air actually contains at any temperature compared to what it could hold at that same temperature, is called the relative humidity. Thus, if a cubic foot of air contains 0.5 gr. of moisture at 0°,



this being its absolute humidity, the absolute humidity will be 0.5 gr. when the air is heated to 70°. But a cubic foot of air at 70° would be capable of containing 8.0 gr. of moisture, therefore its relative humidity at 70° would be only about six per cent.

When outside air is about 30°, it is well to have about 4 to 5.5 gr. of moisture per cubic foot of air, when temperature is raised to 70°; but with outside temperature 0° it is ordinarily considered that relative humidity should be about one-half the difference between outside and indoor temperatures, or where outside air is 0° and room temperature 70°, the relative humidity should be about 35%. This is the practical value which will not cause steaming of windows.

Assume in the above example that 35% relative humidity at 70° is to be maintained. The air then would leave the humidifier completely saturated at 41°, containing 2.85 gr. of moisture per cubic foot, and then could be raised to any desired temperature by passing over heating coils. As air entered at 0° containing 0.5 gr. of moisture per cubic foot, 2.35 gr. of moisture should be added to each cubic foot of air. Through the ordinary range of temperatures the absorption of one grain of moisture per cubic foot lowers the dry bulb temperature 8.5°, or 8.5° are necessary to raise moisture in a cubic foot of air one grain or 20° will be necessary to raise moisture per cubic foot 2.35 grains.

This will be in addition to the 120° for heating and ventilating, or 140° will be required for heating, ventilating, and humidifying. Therefore 70° of 140° total, or 50%, is required for ventilating, 36% for heating, and 14% for humidifying, and it can be stated approximately that cost of ventilating will be 50%, cost of heating 35%, and the cost of humidifying 15%.

#### Systems of Air Supply

The method of distributing the air in an industrial building is a consideration of chief importance. The methods usually applied are as follows:

First, the air is taken entirely from without and after being heated is forced directly into the building through the distributing ducts, this method being generally known as the Plenum System. The pressure produced within the building causes continuous exit of the air from the building, either through the natural openings, as is usually the case in factories and other large buildings, or through special vent openings provided for the purpose as described under Public Building Application. This method effectually prevents the entrance of cold air from without.

A second and by far the most common method used in industrial plants is to draw the supply of air entirely from within the building, raise it to the proper temperature and force it through the distributing ducts thus causing a continuous circulation within the building itself. This method can be used in industrial applications since the question of ventilation is not of as great importance as in public buildings, inasmuch as the relative amount of air per occupant is very much greater in industrial plants.

The ideal arrangement is a combination of the two mentioned above and should be used wherever possible. In this method, the greater portion of the air is returned to the apparatus, but sufficient fresh air is taken from the outside to create a plenum within the building and thus prevent the inward leakage of cold air. In this manner the amount of air loss by leakage is made up—not by the infiltration of cold air through the crevices around the doors and windows—but by air that has passed through the apparatus and has been heated to an effective

degree. This combination has been found to be more economical than where all returned air is used. The proper amount of air to be taken from outside is determined by securing a condition within the building so that the noticeably inward flow of air around the doors or windows ceases. If the plenum is carried beyond this point, there will be a loss due to the heating of an excess amount of outside air drawn through the apparatus.

#### Systems of Air Distribution

The vertical duct system such as usually used in public and office buildings is frequently employed in factory buildings. In this system the air is admitted through vertical ducts or flues built in the walls and opening into the room at a point about eight feet above the floor line; suitable openings being supplied at the floor line connecting either with vents opening to the roof, or an exhaust duct system through which the air is drawn out. By this method the heated air is continuously forced downward as it cools, and the cool air is removed at the floor line.

This system may be modified by placing the ducts in the room along the walls and either blowing the air out at a height of about eight feet or very close to the floor and blowing directly downward along the floor. The latter method secures a perfect diffusion of the heated air at the floor line and avoids any draft which would be objectionable. In buildings having a large open area a system of overhead piping is installed to the best advantage. Excellent results are obtained by this method providing the pipes are not placed at too great a distance from the floor. The chief advantage of the overhead system is a saving of initial cost, since on account of the high temperature and velocity of air in the distributing pipes, a great amount of heat can be transferred with a very small amount of material necessary, thus the cost of the galvanized iron distributing system air ducts is relatively small. The best results are secured with outlets at from 12 to 18 feet above the floor line. When running the ducts at this height the air may be blown out directly by means of short connections. Above this height it is preferable to use drop pipes extending downward along the structural columns so that they will not interfere with any moving mechanism.

Another system which has proven very satisfactory is that in which a distributing air return duct is employed. This approaches in principle very close to the plenum system as used in public buildings and is a combination of both the plenum and exhaust systems. In this system no distributing ducts or piping for the heated air are used but small fan units are placed at intervals throughout the building. The air is blown directly into the building at about eight or ten feet above the floor through an outlet coming directly from the fan and having short outlets branching in several directions. Return vent ducts are placed at frequent intervals along the wall, these leading into large return air tunnels or ducts through which the air is drawn by the heating fans. In this method the circulation is effected entirely by the return vent ducts rather than by the hot air ducts. This method is to be recommended where an elaborate duct distributing system is impracticable or undesirable.

This system has marked advantage over all other systems in that piping cost is cut to a minimum due to the high velocities and high temperature of air handled by the fan and that a positive circulation of air is produced.



#### **Industrial Applications**

The world is progressing and working conditions of years ago are no longer tolerated. The progress in machine tool design and increased production has bettered the class of workmen. The former artisan is now a specialist.

It is a recognized fact that atmospheric conditions have a marked effect upon the comfort and efficiency of a workman. Thus the maintenance of proper atmospheric conditions within a plant pays big returns in comfort and contentment of the workmen themselves and in increased and better production.

The Buffalo Fan System of Heating and Ventilating is in successful operation in every type of factory building and in connection with every form of industry. A mere list would take up more space than advisable in this volume so we will content ourselves with the recital of just a few applications as given below.

#### Machine Shops

The requirements of the modern machine shop are most admirably met by the Buffalo Fan System of Heating and Ventilating. The modern construction with its large areas of glass roof and large single room volumes presents a very perplexing problem in both air distribution and pressure balancing. How successful our engineers have been can best be shown by describing the system as in operation at the National Acme plant at Cleveland, Ohio.

This plant consists of a one story building of saw tooth construction and covers seven and three-fourths acres. This ranks as one of the largest machine shops in the world. The whole floor is covered very compactly with automatic machines for making bolts and nuts.

The heat losses from the side walls of brick and glass are taken care of by direct radiation and the Buffalo System takes care of the other heat losses which are by far the greater portion.

There are four sets of apparatus each consisting of an exhaust fan returning air from the floor line and discharging it either into the inlet of the air washer for supply or into the atmosphere through ducts through the roof, a supply fan taking air from the exhaust fan or from outdoors as the conditions require, an air washer and the heater units. Both fans are driven by silent chains from a 12"x14" engine. The exhaust fans are provided with an auxiliary motor drive so they can be driven independently when the supply fans are not in operation. Each unit handles 28,000 cubic feet of air per minute and has 6,720 square feet of heater surface.

The fresh air inlet dampers and the exhaust fan discharge dampers are automatically controlled by a thermostat located in the discharge of each air washer.

A considerable quantity of oil vapor and fumes are given off by the automatic machines and the apparatus when in operation keeps the building remarkably free from any traces of these.



Buffalo

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FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

#### Dye Houses

The dye house presents a problem in ventilation that is peculiar and distinctive. The large amount of steam present has always caused trouble by condensation of all cool surfaces throughout the building, making a most undesirable atmosphere to work in and also causing excessive deterioration of the building itself.

Our engineers have made a successful study of this problem and the introduction of the Buffalo Fan System has made the dye house so equipped just as livable as any other part of the factory and removed all traces of condensation on the interior of the building. The entire secret of successful dye house installation is to apply the correct amount of air at the right place.

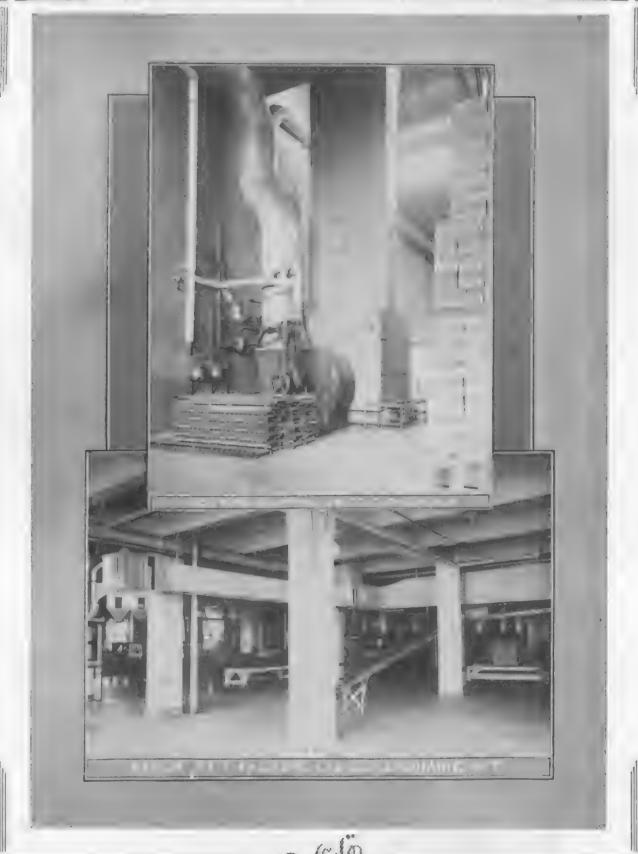
This is accomplished by blowing heated air into the room just above the dye vats and machines and blowing a current of heated air along the surface upon which the vapor has a tendency to condense.

The air blown across the vats and machines dissipates the steam and the other forms a current or film of heated air along the cool surface so that the moisture-laden air is insulated from these cool surfaces. The air is removed by means of ventilators in the roof or disc fans placed at various points in the walls or by a combination of both ventilators and fans. By this method a rapid absorption and removal of all moisture is effected.



Buffelo





FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

The dye house of the Pacific Mills at Lawrence, Massachusetts is Buffalo equipped. This dye house ranks with the largest in the country and is absolutely free from steam and condensation due to the efficiency of the Buffalo System.

The apparatus consists of one No. 12 double width Turbo Conoidal fan, two No. 16 Niagara fans and one No. 19 Niagara fan, sixteen 48" propellor fans and 11,000 square feet of Heaters.

#### Paper Mills

Paper Mills present one of the most fertile fields for air heating, ventilating and humidifying.

In the machine room we have the cold damp portion around the wet end of the machine, the hot humid portion around the driers and the cool portion around the calendar end. The center of the room is over-heated while the ends require additional heat to make them livable. Along with these we have the constant dripping of condensed moisture from the roof. This condensate drops down upon the paper and causes great loss by injuring the finished product in addition to the rapid depreciation of the roof construction. The grinder rooms are extremely cold and damp and the roof condensation is also quite a problem.

The problem met in paper mills is similar to that in dye houses. Warm air must be introduced into the room without conflicting with the natural air current tendencies and ample provision must be made for exhausting the moisture-laden air without allowing it to come in contact with the cool surfaces of the building.

The S. D. Warren Co., Cumberland Mills, Maine, and the Eastern Manufacturing Co., at Brewer, Maine, head the list of paper mills reaping the benefits from Buffalo Heating and Ventilating.

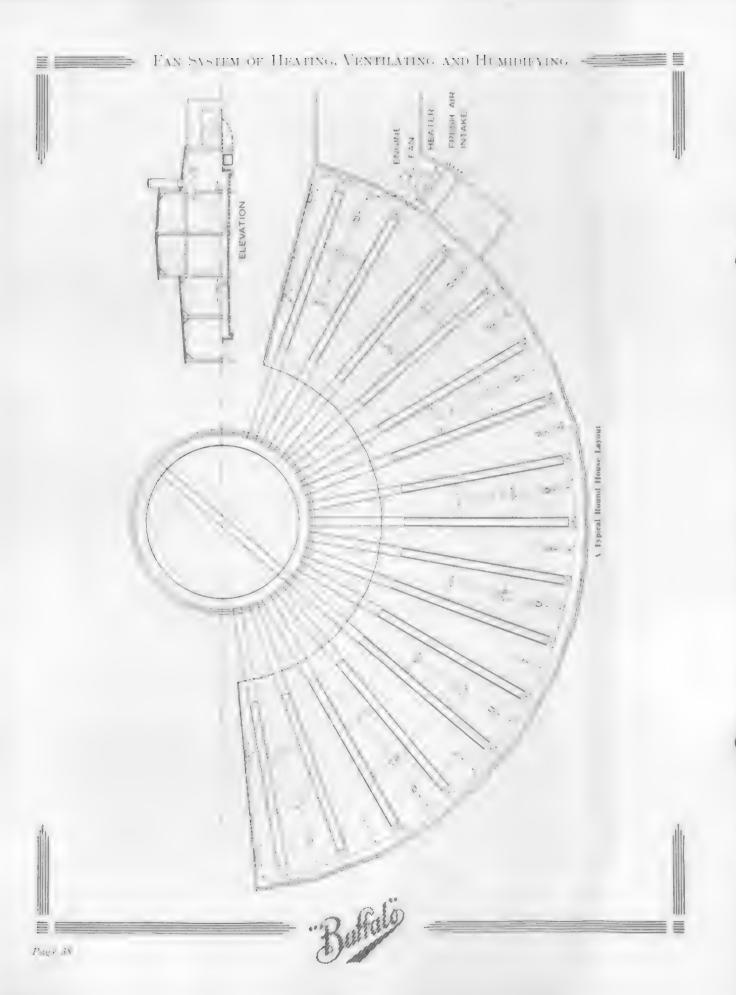
#### Food Product Plants

In plants where food products are handled, the chief requisite of the heating and ventilating apparatus is that the air delivered to the workrooms be absolutely clean. In addition to this a uniform atmospheric condition must be maintained, for it has been found that the quality of the product changes with variations in the atmospheric conditions under which they are prepared. Both of these requirements are admirably met with the Buffalo system of heating and ventilating equipped with a Carrier air washer. The effectiveness of the Carrier air washer is shown by the picture on page 17.

The well known products of the Beech Nut Packing Company at Canajoharie, New York, are all prepared and packed in the presence of pure, clean air delivered by Buffalo Apparatus. Not only is the air washed and heated but is also delivered to each room at the exact humidity required for the process taking place in the room.

Campbell Soups are also benefited by Buffalo heating and ventilating.





FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

#### Railroad Round Houses

Round houses present a very difficult heating problem due to the large volume of warm air carried off through the open smoke jacks which act as ventilators. A great amount of heat is absorbed, too, in the melting of the snow and ice on the locomotives and in the evaporation of the moisture thus produced. Ample ventilation is required to carry off the smoke and gases and considerable heat is required due to the excessive ventilation requirements.

The usual method employed is to draw the air direct from outside and after passing through the coils of the heaters to distribute the air by means of underground ducts discharging into the pits directly under the engines. The outlets are often fitted with volume regulating dampers.

This is very clearly shown in the drawing on the opposite page. In addition to the outlets in the pits the cold outside walls are taken care of by outlets along some of the columns and blowing toward the cold walls.

The cut below shows the Buffalo Fan used for heating and ventilating the N. Y. C. R. R. round house at Gardenville, N. Y.



Buffalo

#### Advantages of the Fan System

The chief points of superiority of the Buffalo Fan System may be summarized as follows:

- 1. Perfect ventilation regardless of exterior conditions.
- 2. Uniform and proper distribution of heat.
- 3. High efficiency of heating surface (three to five times that of direct radiation).
- 4. Greatest economy in operation.
- 5. Utilization of exhaust steam.
- 6. Prevention of cold drafts from without by production of a plenum.
- 7. Independent regulation of heating and ventilating effects.
- 8. Great flexibility in operation to suit varying conditions, affording a maximum economy.
- 9. Ease of control, which prevents over-heating.
- 10. Great compactness, affording an economy of space and reducing the cost of steam connections.
- 11. Perfect drainage, making less repairs necessary and giving a lower rate of deterioration than with direct radiation.
- 12. Low cost of installation.
- 13. The entire apparatus is easily portable and is, therefore, a permanent asset.

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

#### THE BUFFALO FAN SYSTEM

OF

# Heating, Ventilating and Humidifying

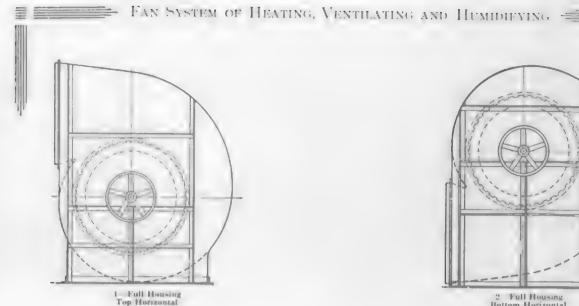
#### PART THREE

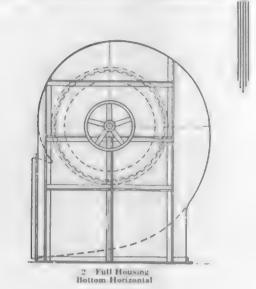
#### Buffalo Apparatus

THE Buffalo Fan System Apparatus consists of a fan, an engine or motor, some form of indirect heating coil, and a Carrier Air Washer and Humidifier. The general arrangement may be either the EXHAUST or DRAW THROUGH system in which the air passes through the heater before reaching the fan, or the BLOW THROUGH in which the fan is in front of the heater and blows the air through the heater coils. The selection of the arrangement to be used depends upon the individual requirements of the location, each arrangement having its own peculiar advantages. The exhaust through apparatus possesses the advantage of greater compactness and a more convenient arrangement. On the other hand, the blow through apparatus is larger but occupies a more narrow space. The former requires the use of an exhaust fan, one having only one inlet, which is slightly less effective than a blower having two inlets such as is used in the blow through type; however, the exhauster discharges directly into the duct system without any reduction in the velocities of the heated air so that all the energy of velocity of discharge is utilized. The blow through system on the other hand requires a change from the relatively high velocity at the fan outlet to a low velocity through the heater and back again to a high velocity upon entering the air ducts which causes an unavoidable loss in pressure.

Due to its compactness the exhaust through apparatus is customarily employed in factory buildings. The blow through apparatus is necessarily used in public buildings and elsewhere wherever independent temperature regulation is demanded as the use of a by-pass around the heater permits the independent distribution of hot air and tempered air in any desired proportions.





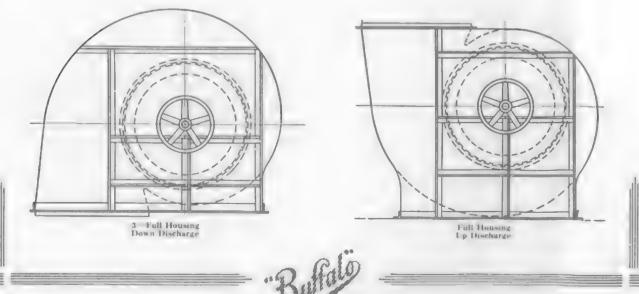


#### Fans

Fans and blowers are designated by the position of the discharge opening and are class fied as follows:

Top or bottom horizontal discharge, up or down blast, and special, the latter being described by giving the angle of discharge from the horizontal. The hand of a fan or blower is determined by the side on which the pulley or engine is located. When facing the discharge outlet, the fan is either left or right hand according to whether the pulley is on the left or right side as seen from this position.

A brief description of the various types of fans manufactured by the Buffalo Forge Company follows.



FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING





Buffalo Cone Fan

Buffalo Planoidal Fan Wheel

#### Cone Fans

For the introducing of cooled or tempered air into rooms where no distributing system is required or for exhaust ventilation where the resistance to be overcome is moderate a type of fan known as the cone wheel is suitable. This special form of fan wheel is used without a housing and is shown in the cut above. This fan wheel must not, however, be compared with the disk or propeller fan, since it is purely of the centrifugal type. Tables of performance are found on page 76.

#### Planoidal (Type L)



Buffalo Planoidal Fan Type L

One of the first developments of the centrifugal type of fan wheel was the steel plate fan. In this fan the blades consist of flat radial plates and are few in number. As the result of extensive experimenting and testing by our engineers the Planoidal (Type L) steel plate fan was developed which was a distinct improvement over the old style steel plate fan. This fan is provided with an inlet cone on the housing and the proportions of the wheel, housing, inlets and outlets were so designed as to materially increase the capacity and efficiency, at the same time reducing the power consumption. Tables giving the ratings are found on pages 78 and 106.



#### Niagara Conoidal (Type N) Fans

With the increase in the speed of prime movers it was found necessary to design fans to operate at a higher speed and one of the marked developments in this line was the Buffalo Niagara Conoidal Multiblade fan. This fan derives its name from the prevalence of conical shapes in its design. The blades are made to conform to the tapering surface of a cone, the inlet is conical and the blast wheel forms the frustrum of a cone.

These characteristics are very clearly shown in the adjacent cut.

Fans from No. 3 to No. 6 in size are made with cast iron inlet bearing stand and cone as shown below. All sizes over No. 6 are made with sheet iron inlet cone and flat steel bearing standards as shown in cut below.

Performance data will be found on pages 79 and 107.

No. 3 to No. 6 Niagara Considal Fan, Right-Hand Up Discharge

#### Turbo Conoidal Fans

The increasing demand for air at high pressure was forseen by the Buffalo Forge Company, and a new type of Multiblade fan known as the Turbo Conoidal was developed. This fan differs from the Niagara Conoidal, only in that its blades are of double curvature instead of single curvature. This

fan is particularly suited for on-

cration where both high speeds and high pressures are essential. The various points considered in the design of the Niagara Conoidal fan were also taken into account by our engineers in the design of the Turbo Conoidal, and all parts are co-ordinated with the view of obtaining the highest efficiency with the lowest power consumption. Performance tables are found on pages 80 and 108.

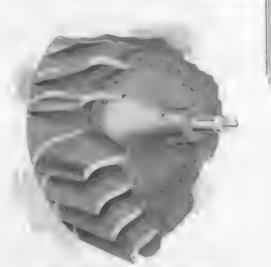
All parts of the Niagara and Turbo Conoidal fans have been designed with the view of obtaining the best efficiency under practical operating conditions.



Three-Quarter Housing Ningara Conoidal Fan. Left-Hand Top Horizontal Discharge



The wheels, blades and hub are designed so that the air shall have a smooth easy flow from inlet to outlet without any abrupt change of direction at any point; also, the width of the blade is so proportioned that the back part cannot take up any greater part of the air, this prevents uneven pressure and eddy currents, and effects an even distribution of the air over the entire surface of the blade. Our success in this design has been proven by practical, tests, and our standard guarantee is that the velocity of air issuing from any part of the fan outlet as measured by a Pitot tube is not more than 15% above or below the average velocity across the entire opening.



Turbo Conoidal Fan Wheel Partly Assembled. Showing Double Curvature of Blades

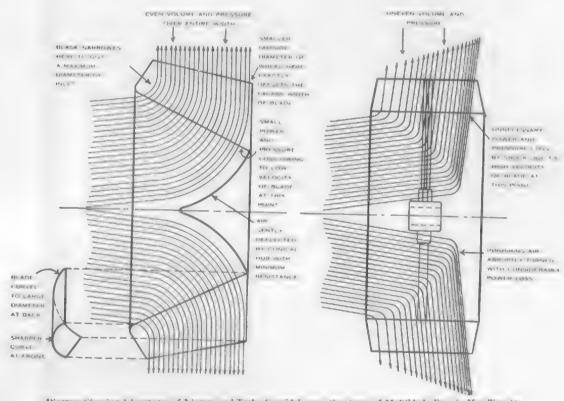


Diagram Showing Advantages of Niagara and Turbo Conoidal over other types of Multiblade Fans in Handling Air





#### Buffalo Spherical Type Fan Bearing

One of the prominent features of Buffalo Fan construction is the type of bearing used. It was proven early in the history of fan construction that the reliability of operation of a fan was in a large measure determined by serviceability of the bearing used.

The type of bearing described below is by far the best fan bearing on the market today.

This dust proof and oil tight bearing consists of a split sleeve lined with babbitt and completely encased in the bearing housing. The sleeve is mounted between spherical surfaces which allows the bearing to adjust itself in every direction, and the housing provides a large oil reservoir in which two oil rings dip; overfilling is

prevented by the position of the opening through which the oil is supplied and which also indicates the oil level.

In the interest of safety the thrust collar is placed inside the housing, running against a babbitted shoulder; grooves on the outside surface of the thrust collar throw off all oil and absolutely prevent it from creeping along the shaft and being drawn into the fan.



FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

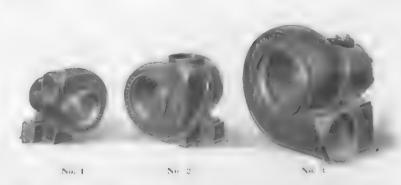
#### Selection of a Fan

It has been proven both in theory and practice that the length of blade in a straight blade fan wheel is the deciding factor in the pressure obtained at a fixed rotative speed and that a curvature of the blade in the direction of rotation tends to increase the pressure. Whereas the curvature against the direction of rotation tends to decrease the pressure. It is often stated that the forward curvature of fan blades will increase the efficiency over that obtained with radial blades or backward curvature blades, this however is not true. Each type is admirably suited for a certain purpose; It has been found that short curved blades require a greater number for good efficiency than blades of the radial type, similar to the steel plate and Type L fans. With the steel plate or planoidal fan having a small number of radial blades usually from five to twelve depending upon the size, the pressure tends to build up as the capacity falls off, that is, at a constant speed the pressure is greater at half capacity than at normal rating. With the multiblade type, such as the Niagara Conoidal having single curvature blades, the pressure is developed more by change of direction and impact of the blades against the air, rather than by centrifugal force, the pressure is greatest at the normal load for which the fan was designed and decreased for any load, either above or below this normal capacity, This feature has been overcome in the fans having double curvature blades, e. g., the Turbo Conoidal in which the pressure builds up as the capacity falls off, in this respect being very similar to the steel plate fans. These points are very clearly brought out in the characteristic curves of these various types of fans as shown on pages 81 to 83.

From this it will be seen that in systems where a uniform air quantity is desired, whether for heating, ventilating, forced drafts or drying processes the steel plate fan and turbo conoidal fan will come nearer giving this uniform quantity in spite of variations in resistance brought about by throttling of dampers or similar conditions. On the other hand, it is sometimes very desirable to be able to cut down the capacity of a fan without increasing the pressure and velocity, as for instance, if one part of a building should be shut off; in a case such as this, the steel plate fan would deliver an increased amount of air into the remaining part of the system on account of the increased pressure, whereas the multi-blade fan of the Niagara type would be more sensitive to the increased resistance and would fall off in capacity due to this. In general multi-blade fans of equal capacity and efficiency require less space than steel plate fans and have the advantage of operating at higher speeds.

When specifying a multi-blade fan with single curvature blades extreme precaution must be taken in designing the duct system, in determining the frictional resistances of the entire system, and selecting the proper speed for the size of fan to be used.





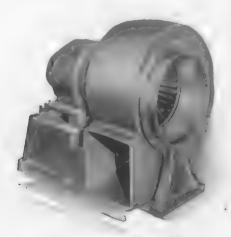
#### Buffalo Baby Conoidal Fans

The Baby Conoidal fan is of the high efficiency multiblade type with blast wheel of the same design as the Niagara Conoidal (Type X) which has met with such marked success. Housing is cast iron and can be swung around to discharge in any desired direction. This fan furnishes a large volume of air at a relatively low pressure with moderate speed. The wheel is accurately balanced, assuring a smooth-running, noiseless machine.

It is unexcelled for all kinds of drying and cooling purposes, for supplying fresh, cool air to offices, homes, staterooms, telephone booths, etc., and for exhausting smoke, fumes and foul air from kitchens, restaurants, lavatories, etc.

Cord and plug are furnished with No. 3 and smaller; no expense for installing, simply attach to an electric light socket. Outfits are furnished with 110 or 220 Volt D. C. motors and 110 or 220 Volt single phase, 60 cycle, A. C. motors. Nos. 4, 5 and 6 are also furnished with 110 or 220 Volt, two or three phase, 60 cycle motors.

Tables of dimensions and performance on page 76.



No. 6. Baby Considal Fan



FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING



Motor Driven (Type D)



Pulley Driven (Type D)

#### Disc Fans (Type D)

The ordinary disk or propeller fans are designed for use where low pressure heads are operated against. This type of fan should never be used in connection with a pipe system but should discharge directly into a room, or exhaust from it without obstruction. The characteristics of the Type D fan are very clearly shown in the above cuts.

Performance tables are given on page 77.

#### Disc Fan (Type CM)

Where a disc fan is used to overcome a moderate resistance, the Type CM with overlapping blades is recommended. This type of fan is used as a booster in mine ventilation, or for producing air flow in cooling towers for condensing plants. The casing and bearings are self-contained.



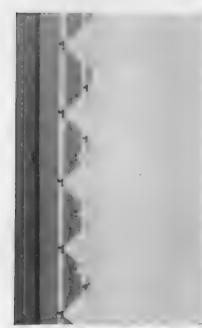
Tyne ( M



#### The Carrier Air Washer and Humidifier

The Carrier Air Washer consists of a spray chamber, a series of spray nozzles and eliminator plates. The air is drawn through the spray chamber where it comes in intimate contact with an atomized spray of water.

The number of nozzles is ample



Spray Nozzles in Operation

to insure a uniform distribution of the mist as shown in the cut to the left. The water is so finely divided that the

Interior of Carrier Air Washer

air mixes thoroughly with it and all dirt and dust particles are saturated. The air and water then pass through the eliminator plates.

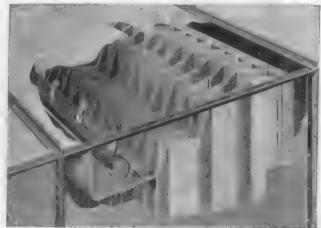
The eliminators consist of a series of zig-zag plates, a portion of which are flooded with a continuous film of water. The air impinges on these flooded plates, leaving the dust and dirt which are caught in the film of water and washed into the

settling tank in the lower part of the washer.

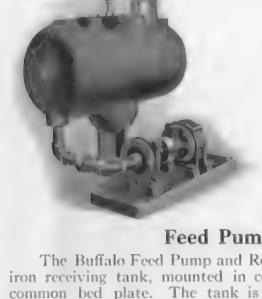
The clean air passes through the dry part of the eliminators where all entrained water is removed by the lips crimped into the plates and leaves the washer with the exact amount of moisture as predetermined by conditions of temperature and humidity.

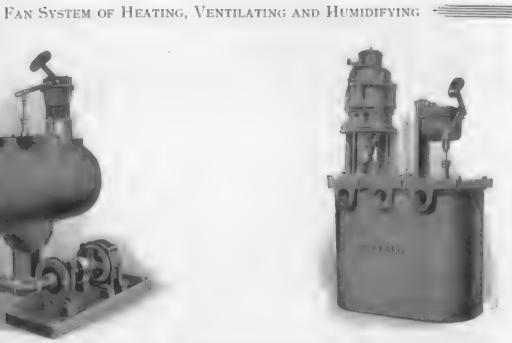
Turn back to page 17 and see the five pails of dirt removed by the Carrier Air Washer in Public School No. 6, Brooklyn, New York.

Data relative to the sizes and capacities of the Carrier Air Washer and Humidifier will be found on pages 84 to 95.









#### Feed Pumps and Receivers

The Buffalo Feed Pump and Receiver consists of a suitably constructed castiron receiving tank, mounted in combination with a Boiler Feed Pump on a common bed plate. The tank is mounted slightly above the pump, giving a sufficient head of water above the suction valves to insure the pump always receiving a full supply of water.

Within the tank is provided a float connected to a chronometer valve controling the steam supply to the pump. Inflowing water causes float to rise, thereby opening the steam supply and starting the pump. When the water level has been lowered, the float automatically cuts off the steam. In this way the condensation water is returned to the boiler as fast as it accumulates.

A Buffalo Vertical Centrifugal Condensation return pump in its scheme of operation is similar in every way to the ordinary horizontal shaft outfit except, that the pump is vertical and submerged within the receiver. The motor is controlled by means of a ten-inch seamless copper float, operating a float switch. This style of design is more convenient in many installations as it avoids providing large pit to carry the pump in order to get it sufficiently low to admit gravity drainage.



#### The Buffalo Standard Heater

The Buffalo Fan System Pipe Coil Heater has been designed to meet the peculiar requirements found in forced ventilation and also to secure the maximum effectiveness in connection with such work.

First: A perfect circulation of the steam is obtained which removes all air from the coils, carrying it to a single chamber in the base from which it is easily removed through the exhaust connections. Air binding, the greatest enemy of radiation efficiency, is thus prevented.

Second: The heater is so arranged to insure perfect drainage. The design of the base allows no opportunity for pocketing of water, and the pipes are immediately relieved of all condensation, thus avoiding any chance of damage by freezing. The drain ports are made large to allow for an unusually rapid condensation without choking and filling. This feature allows the coil to be used over a great range of radiation.

Third: The proportion of the air passages between the coils is so designed as to secure the highest efficiency of radiating surface and the lowest resistance to air flow. In this respect the air is brought in intimate contact with all parts of the heating surface and a uniform and maximum velocity of air is maintained throughout the coil. The velocity of the air is a determining factor in the rate of heat transmission, this being conclusively shown in the curve on page 73, this curve being derived from data obtained from actual tests made on Buffalo Coil Heater. By maintaining uniform velocity through the heater any unnecessary loss of pressure due to changes in velocity is prevented.

Fourth: Each section is independently connected to the steam main and the steam supply controlled by valves so that as few or as many sections as desired may be in operation giving the operator a convenient and absolute control of air temperature and heater effect. By this method of connection any section may be removed for repairs without interfering with the operation of those remaining. This construction also enables the use of live steam in a number of sections and exhaust steam in the remaining, or live and exhaust steam may be introduced in any one section at the same time.

The condensation and heating capacity from a given amount of properly designed radiation, is from three to five times greater with a forced circulation of air than in ordinary radiation. It can readily be seen that a heater designed for a fan system must provide for positive and rapid condensation in order that the coils may be invariably hot. This condition is admirably met with the Buffalo Heater.

The Buffalo Heater is made in two styles known as the Open Area and Return Bend patterns, the difference being very clearly shown in the cuts on next page.

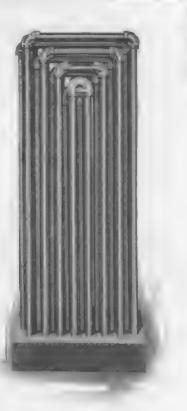
On pages 96 to 108 are given the tables which show the characteristics of Buffalo Heaters and also various combinations of heaters and fans. This



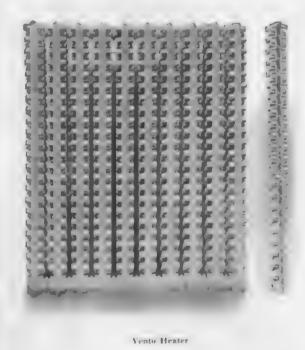


Return Bend Heater

information will be found very useful for use in industrial heating and ventilating work. All Buffalo Heater Sections are made with four rows of pipes. From the table on page 96 it will be seen that the size and number of pipes vary over wide limits so that it is readily possible to obtain a size of heater to meet practically any requirements. When an apparatus is required having a clear area through the coils greater than the largest heater shown in this table, two smaller coils may be chosen and placed back to back, this arrangement can be further extended, and a triplex arrangement of three groups used.



Open Area Heater



#### Vento Heaters

The Vento low pressure cast iron heater, which is very clearly illustrated in the cuts, is designed especially for use in the fan and blower work. These heaters are made in sections of various heights and widths which may be assembled so as to make a heater of any desired size and depth. Ratings are found on page 104.

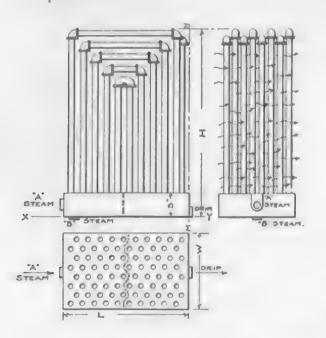
#### Indirect Heaters

It is sometimes desirable to locate the fan outside of the building to be heated, either in the power house or a specially built apparatus room. If the distance is considerable



it will be found more economical to place the heater unit in the building itself, carrying the unheated air over the intervening space rather than heating it before.

For special indirect heating work where the fan and heater are placed some distance apart a larger base is used for the heater than when used in close proximity to the fan. The table following will give the details of the various sizes of indirect heaters built by this company. Under the heading of "Size" the first row of figures gives the numbers of pipes across the steam supply and drip ends, and the second column the number of pipes in the length of the coil. Cast iron manifold bases are used as in the regular fan system heater, however the steam and exhaust connections are on opposite ends of the manifold instead of on the fan and as in the fan system heater, this enables the heater to be used in either an upright or horizontal position according to the requirements. These heaters are known as the solid base type, the base being divided into two chambers by means of a diaphragm which compels the steam to flow evenly through all pipes. These coils are designed for the use of either live or exhaust steam, being effectively applicable for low pressures.



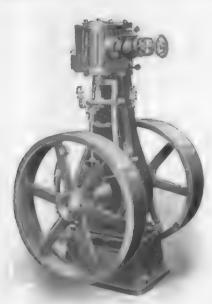


#### Actual lineal feet one-inch pipe in each section

Sizi	1012"	4612"	52121	5812"	6412"	//	L
6 x 8	133	184	177	198	221	121.,	
815	177	206	236	265	205	161	1313
8 x 10	221	255	295	332	256559	161	27
10 x 10	276	323	231559	415	462	20	
10 x 12	346	387	143	1115	22.3.3	20	- 3
10 x 14	387	451	517	551	645	20	37
12 x 12	398	46.4	532	500	1963	12131	32
12 x 14	464	542	618	697	774	231	37
12 x 16	532	618	709	79%	886	2711	12
14 x 14	542	15.12	723	N11	\$HH;	273	117
16 x 16	708	827	945	1061	1181	301	42









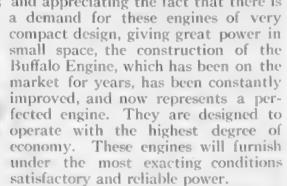
Class "A"

**Buffalo Steam Engines** 

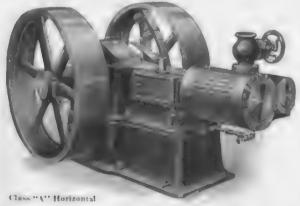
During many years of constant service in the building of engines it has been possible to bring the Buffalo Engine to a high state of perfection. Those who have directed its growth have aimed at the development of a simple, economical and, above all, a substantial engine, built in several types, each suited to its individual work. The limitations of floor spaces and heights, together with different engineering practice in mills and power plants, have been met with appropriate designs which evince a careful consideration of all the requirements.

The design of a steam engine calls for a series of compromises. To make these compromises in favor of the most beneficial results is the evolution of the best engine design, and to carry out these plans in a shop is the evolution of the best engine. Thus it is that the Buffalo Engine has a piston valve and bored guides, that the connecting rod has a small angularity, that the eccentric strap and simple transmission of its motion are used.

The very great extent of the use of the high-speed automatic steam engine makes it applicable to almost any service; and appreciating the fact that there is



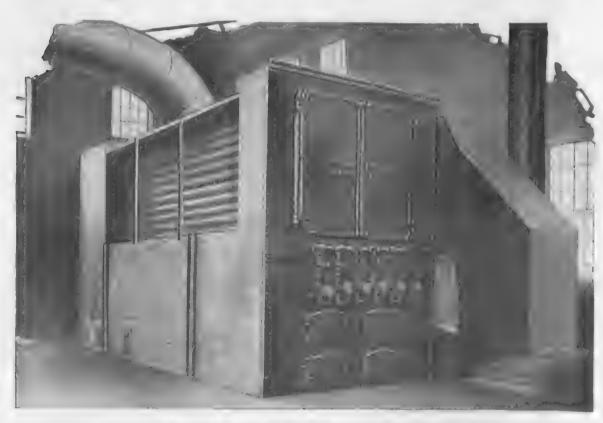
Tables of horsepowers and dimensions are given on page 105.



#### Gas and Coal Heaters

This company has been very successful in the installation of several large heating plants where the heat generated by the combustion of coal or natural gas is transferred direct to the air used for heating and ventilating without the use of an intermediate medium such as water. The heater used in this connection resembles a horizontal water tube boiler, each heater consisting of a bank of iron boiler tubes expanded into a heavy tube sheet at each end. These tubes are set in a brick housing similar to a boiler and the products of combustion passed through the tubes while the air to be heated is passed around the tubes. The furnace and combustion chamber in the housing is so designed that complete combustion will occur before the gases reach the tubes, and thus the greatest possible amount of heat is available for transmission to the air to be heated.

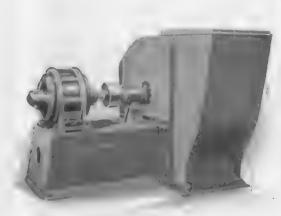
Heaters of this type are in successful operation at the American Rolling Mills, Middletown, Ohio. In these heaters the hot gases at the back of the combustion chamber at a temperature of 3000° F. are mixed with two-thirds of the exhaust gases taken from the front breeching and this resulting mixture is forced through the tubes by means of a fan. This has been found to be the most economical procedure. The gases coming directly from the combustion chamber are too hot to be introduced into the tubes without some cooling and in the method above described no loss of heat is entailed. The pure air for distribution through the building is drawn through the clear area around the outside of the tubes and then forced



Buffalo Gas Heater at American Rolling Mills, Middletown, Ohio



through the duct system by means of another fan. The heaters mentioned above have been tested and show an average operating efficiency of 85% without considering radiation losses. In many places the heating efficiency obtained by this method makes it advisable to use gas or coal heaters instead of steam boilers. Stokers have been used with great success in heaters of this type.



Overhung Fan

Fan Bearing on Inlet Side

#### Motor Driven Fans

We have found it advisable in most cases to install engine driven fans, preferably direct connected, this method being most economical and permits of a wide speed variation. There are however, innumerable cases where the steam pressure necessary to operate the engine is not available, or the location desired for the fan apparatus is such that as little attention as possible shall be required for its operation; in cases such as these motor drive affords the solution and special fan designs have been made for use in connection with motors. A motor base is constructed in connection with the fan housing, either of a heavy cast iron onepiece box construction or built up of heavy sheet iron and reinforced with angles. The base is stiffened across the interior by ribs if made of cast iron, or heavy angle braces in the built up construction and made with rounded corners thus combining the necessary strength with a pleasing appearance. In the case of the smaller size of fans with one inlet the fan wheel may be overhung on the motor shaft,

which is extended for this purpose; however, it is preferable to use a coupling and place a bearing on the side of the fan farthest from the motor. Wherever alternating current is used, the high speeds at which the regular motors run, make it impossible to use a direct connected unit for heating and ventilating work, except in very rare cases. For direct current, motors may be obtained for any desired speed, and although a slow speed motor is more expensive than a high speed motor of the same power, the advantage gained is sufficient to warrant the adoption of the slow speed motor except in the largest sizes of ventilating fans which operate to best advantage at slow speeds.



Fan Overhung on Motor Shaft



FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING



Schenley High School, Pittsburgh, Pa-

Buffalo

Buffalo Equipped

FAN System of Heating, Ventilating and Humidifying

# THE BUFFALO FAN SYSTEM OF Heating, Ventilating and Humidifying

#### PART FOUR

THE Buffalo Forge Company takes great pride in its hand book "Fan Engineering" which is, without exception, the authority in its field. The following subject-matter and data has been condensed from the text of this hand book and the reader is referred to it for a complete discussion of the various principles involved.

#### Relation of Velocity to Pressure

The laws governing the flow of air are less understood than any other branch of engineering. The flow of air under high pressure must be investigated thermodynamically and the formulae are therefore complicated.

For low pressures such as are met with in ordinary fan work very little error is introduced by applying the same formulae to the flow of air as to the flow of water.

The basic formula for such calculations is

$$V_s = \sqrt{2 \text{ gh}}$$
 or  $V = 60 \sqrt{2 \text{ gh}}$  where

V<sub>s</sub> = velocity in ft. per second. V = velocity in ft. per minute.

g = acceleration due to gravity in feet per second.

h = Head in feet causing the flow.

We also have

$$U = h' \frac{d}{12W}$$

where

h' = head expressed in inches of water.

d = density of water

W = weight of air in pounds per cubic foot.

Then with dry air at 70° F and 29.92" Barometer, weighing 0.07495 lbs. per cu. foot.

$$\frac{d}{12 W} = \frac{62.31}{12 \times 0.07495} = 69.28$$

and we have

$$V = 60 \sqrt{2 gh'} \frac{d}{12W} = 4005 \sqrt{h'}$$

From this we see that the velocity due to one inch of water at standard conditions for air will be 4005 feet per minute and for a pressure of one ounce per square inch will be

$$4005\sqrt{1.734} = 5273$$
 ft. per minute

The following tables give the pressure and velocity for air first, at constant temperature of 70° and second, at various temperatures.



#### FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

### Corresponding pressures and velocities of dry air at 70° and 29.92 inches barometer

INCHES OF WATER	Ounces per Sq. In.	VELOCITY Ft. per Min.	OF WATER	PER SQ. IN.	Fr. per Min
.05	.0289	Stri	4.77	2.750	8745
10	.0577	1266	5 00	2.884	8943
.20	.1154	1791	5.20	3 (100)	9134
		2003	5 50	3.172	9392
. 25	.1443				9810
.30	.1730	2193	6 00	3 180	
.40	.2308	2533	6.07	3.500	11561
.43	.2500	2637	6.50	3 749	10210
.50	.2884	2832	6.94	4,000	10545
.60	.3460	3102	7 00	1057	10595
.70	.4037	3351	7 50	4 326	10968
.75	.4826	3468	7.80	1.500	11187
80	.4614	3582	8 00	4.611	11328
87	,5000	3729	8.67	5 (00)	11792
90	5190	3800	9 00	5.190	12015
1.00	.5768	4005	9.54	5,500	12367
1 25	.7209	4478	10.00	5.768	12665
1.30	.7500	4566	10 40	6 000	12915
1.50	8650	4905	11 00	6.344	13282
1.73	1.0000	5273	11.27	6.500	13445
1.75	1.0092	5298	12.00	6.921	13875
2.00	1.1535	5664	12.14	7.000	13950
(۱۹۱) ند	1.1000				
2.17	1.2500	5895	13 00	7.497	14440
2.25	1.2975	6007	13.87	8 (000)	14913
2.50	1.4418	6332	14.00	8 074	14985
2.60	1.5000	6457	15 00	8.650	15510
2.75	1.5860	titi-11	15 61	9 (000)	15820
3.00	1.7300	6937	16 00	9 227	16020
3 03	1.7500	6976	17.00	9.805	16513
3.25	1.8740	7220	17.34	10.000	16675
3.47	2.0000	7457	18 00	10 380	16990
		7400	10.00	10 960	17456
3 50	2 0185	7492	19 00 19 07	11 000	17488
3.75	2 1630	77.56	20.00	11 555	17910
3 90	2 2500	7910	20.00	II (12)(1	
4,00	2 3070	8010	20.81	12.000	18265
4.25	2.4510	8256	22 54	13 000	19012
4.34	2 5000	8337	24.28	14.000	19730
4.50	2,5950	8496	26 01	15 (00)	20420
4.75	2.7395	8729	27.74	16 (60)	21090

## Corresponding velocity for dry air at various pressures and temperatures and 29.92 inches barometer

Pres	SUITE	503	60'	70°	HIO°	1.50)	300	2(0),	550
INCHES	OUNCES	*****							
.25	.1113	1965	1986	2003	2059	2149	20049	2606	2895
.5	2551	2778	2505	2832	2941	3005	2.391	3812	\$100.7
.75	43126	3402	3439	21 1115	3565	3720	1153	Tritis	5()2(
1.0	.5768	39029	3897.1	41415	4117	1-1-10	47566	5.390	5795
1 25	.7209	4393	1110	4478	1602	1801	5002	6027	6470
1:50	50,50	4812	1564	1905	5042	5262	17.47	tit (1)2	7100
1.75	1 0092	5197	5254	3298	5146	50553	6,004 1	7131	7655
2.00	1.1535	3,5365	5616	Telef 4	76.313	6076	6753	. 7624	5197
2.25	1.2975	5892	5956	66007	6174	6143	71101	×11×5	561.1



FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

Some writers have endeavored to correct for the effect of compression by introducing certain constants in the above formulae but the results obtained by the use of these formulae are more in error than when the equations given above are used.

To obtain a more correct formula which will apply to higher pressures up to one-half of an atmosphere, we may assume the air is discharged under isothermal expansion, when we obtain the formula

(a) 
$$V_0 = k \sqrt{\frac{1}{d}} \sqrt{\log_{10} \frac{P_0 + P}{P_0}}$$

where

 $P_0$  = the barometric pressure in pounds per sq. in.

P = the pressure of the air above atmospheric pressure expressed in inches of mercury.

d = the density in pounds per cu. ft.

If a more exact expression is required, which allows for the adiabatic expansion, the thermodynamic equation is used which gives

$$V_0 = 109.2 \sqrt{T_1 \frac{1}{11} - \left(\frac{P_0}{P_0 + P}\right)^{0.29}}$$

This latter formula is inconvenient in application, and varies so little from formula (a) with pressures under one pound per square inch that formula (a) is always preferable.

#### Measurement of Air Flow

The quantity, velocity and pressure of air discharged by a fan or flowing through a pipe may be determined by various methods.

The anemometer is used where extreme accuracy is not required or where the velocity of the air is low as in the duct or register entering a room.

#### Friction of Piping

A subject of great practical importance in fan work is the loss of pressure by friction in conveying air through piping. The expression for the flow of air in smooth circular metal pipes may be taken as approximately

$$F = \frac{1}{50d} \left( \frac{V}{4005} \right)^2$$

where

F = the loss of pressure in inches of water.

V = the velocity in feet per minute.

1 = the length of the pipe in feet.

d = the diameter of the pipe in feet, 1.e. d = length of the pipe in diameters.

From this formula it will be seen that 50 diameters of smooth pipe produce a loss which corresponds to the velocity head. This formula is of the same general



form developed by Weisbach but recent experiments have shown his coefficient to be considerably too high for smooth pipe and in this formula it has been corrected accordingly. For pipes with rough or uneven surfaces the coefficients must be decreased accordingly. For tile and brick ducts we recommend that the coefficient be decreased 25%.

The tables of pipe friction below will be found very useful in estimating friction losses.

# E				1,03%	- 411 PH	ESST HE.	PER 100	111.15	1501115	OF RY	111;			
Valedity, arr in tech						DEAME	TER OF I	PIPL IN	15(11) 5					
i le	3 in.	4 in.	5 in.	6 in.	7 in.	8 in.	Oin.	10 in.	12 111	H in.	10 lu	1× in	2010	22 m
200	,026	.019	.016	.012	.010	.009	.005	,007	.007	,005	.005	.003	.003	,00
200	.057	.043	.035	.029	.024	.023	.019	.017	.014	.012	.010	.010	.(10)	(10)
4(10)	.102	.076	.062	.050	.043	.038	.033	.031	.026	.022	.019	.017	.0]6	.01
500	.161	.120	.097	.080	.069	.061	.054	.049	.040	.035	.029	.027	.024	.02
600	.231	.173	.139	.116	.099	.087	.076	.060	.057	.(150)	.043	.038	.035	.03
700	.314	.239	.189	.158	.135	.118	.104	.094	078	(1655	.059	.052	.047	.04
800	.411	.309	246	.206	.177	.154	.137	.123	.102	11:10	.076	4889	.062	,(),"
5000	.520	.390	.312	.260	.224	.194	.173	.156	.130	.111	.097	.087	.078	.07
1000	.642	.482	.385	.321	.276	.241	.213	.192	,160	.137	.120	.108	,097	.05
1500	1.444	1.083	.867	.723	.619	.541	.482	.434	.361	.312	.277	.243	.225	.11
2000	2.568	1.927	1.542	1.285	1.101	.964	.855	.770	.642	.550	.482	.428	.385	.3.
2500	4.013	3.004	2,409	2.006	1.748	1.505	1.337	1.205	1.004	.860	.753	.(1611)	.603	,
3000	5.774	4.335	3.468	2.890	2.478	2.168	1.927	1.734	1.444	1 238	1.084	.1054	.867	.73
3500	7.872	5.902	4.722	3.820	3.373	2.956	2.624	2.360	1.966	1.685	1.476	1.311	1.179	1.07
4000	10.276	7.706	6.166	5.138	4.405	3.853	3.425	3.083	2 568	2.202	1.926	1.713	1.542	1.40
1500	13.005	9.754	7.803	6.560	5.573	4.878	1.335	3.728	3.251	2.787	2,438	2.168	1.951	1.7
5000	16.055	12.051	9.634	8.084	6.880	5.934	5.351	4.852	1.014	3.440	3.010	2.676	2.409	2.19
5500	20.643	14.577	11.656	9.713	8.340	7.288	6.477	5.827	4.857	4.162	3.642	3.237	2.913	2.6
ENDO		17.340		11.561	9.908	8,670	7.706	6.936	5.780	4.985	4.335	3.853	3 468	3.1.

The same	loss of pressure per 100 pt. in inches of water											
Velocity if in feet	DIAMETER OF PIPE IN INCHES											
65	21 in.	26 111	28 in.	30 in.	34 in	38 in.	42 in.	40 in	50 111	51 in.	58 in.	b° in
200	.00322	.00296	.00274	.00257	.00225	.00205	.00184	.00166	.00156	.00139	.00139	.00121
200	.00711	200668	,00619	,00577	00510	.00456	.00413	.00376	.00317	(00053	.00295	.00277
400	.01281	.01183	.01099	.01025	,00905	.00810	.00732	.00668	.00607	00572	.00538	.00486
500	.02005	01850	.01719	.01604	.01415	.01266	.01146	.01046	,00954	.00884	.00815	.00763
600	.02890	.02667	.02476	.02311	.02039	.01826	.01651	.01491	.01387	.01283	.01179	01127
700	,03929	,03628	.03388	.03144	.02773	.02481	.02245	.02046	.01873	.01751	.01630	.01526
800	.05134	.04744	.04401	.04108	.03624	03243	.02934	.02670	.02462	.02289	.02133	.4019904
\$1000	.06503	.06003	.05571	.05202	.04590	.04106	.03716	.03399	.03121	.02575	.02688	.02514
1000	.08021	.07404	.06876	.083417	.05661	.05067	.04583	04214	.00850	.03555	.03312	.0.3104
1500	.15061	.16677	.15482	.14450	.12750	13-4499	.10320	.061427	.08653	.08010	.07473	.463955
2000	.32105	29638	.27271	.25451	.22460	.20002	.18182	.16732	.15417	.14270	.13282	.12415
2500	.50129	, 16.100	12005	.40129	.35402	.31678	.28660	.26167	,24069	.22251	.20740	.19403
3000	.72250	,695623.5	61900	57800	51000	. 15631	.41270	.37680	12011.	.32096	234895	.27970
3500	98030	.90761	.84282	.78661	,60415	.62102	.56190	.51295	.17181	.43700	.40650	.38051
1000	1.2841	1.1853	1 1006	1.0274	340650	.81111	.733581	66985	.61575	57086	.53131	.49696
\$05000	1 6257	1.5051	1.39014	1/3059	1.1476	1 0267	35734	1212010	.78032	.72135	.67106	.62925
5000	2 DUNGS	1 8525	1.7201	1.5986	1.4166	1.2300	1.1467	1 (1462)	,980037	201122	23055	7713/113
5500	2.4284	2 2411	2.0814	1.9426	1.7140	1.5318	1.3873	1.2667	1.1604	1.0791	1 0016	.93980
6360000	2 <900	2.6611	2.4771	2 3121	2 0 102	1.8252	1 6473	1 5075	1/3872	1.2814	1.35447	1 1167

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#### Sizes of Main and Branch Pipes

Most published rules involve arbitrary constants and tables without giving the basic formula or reasons in determining flue, register and pipe sizes. The most efficient arrangements can be made only when the hypothesis of calculation is understood. The essential data is here given and while its application requires more than merely taking sizes from tables, the whys and wherefores are known, and in this knowledge there is considerable satisfaction.

The piping systems for industrial buildings and those for public buildings are figured according to two distinct methods. In industrial buildings the problem is chiefly to convey the heat units with as great an economy of power, material and space as possible, while in public buildings there are the additional requirements of freedom from noise and prevention of drafts. In industrial buildings the air is usually conveyed through one or two main lines extending lengthwise of the building, the areas of such pipes decreasing as they extend, to give a uniform distribution of air throughout. On the other hand in public buildings, individual ducts are carried from the apparatus to each room, so that it is evident the same method is not applicable to both systems.

#### Proportioning Pipes in Industrial Buildings

In proportioning the main and branch pipes in industrial buildings, the primary aim is to secure as uniform a distribution as possible without the necessity of damping; secondly, to secure economy of power and economy of material. It has been found good practice in proportioning piping systems to decrease the velocity in the main pipes as the air quantity decreases. This principle of proportioning has three advantages.

First: It utilizes the velocity of the air in producing static pressure in the system.

Second: By this means a nearly uniform static pressure may be secured in all parts of the pipe line, giving a very uniform distribution of air throughout.

Third: It reduces the friction in the smaller pipes, which would otherwise be excessive.

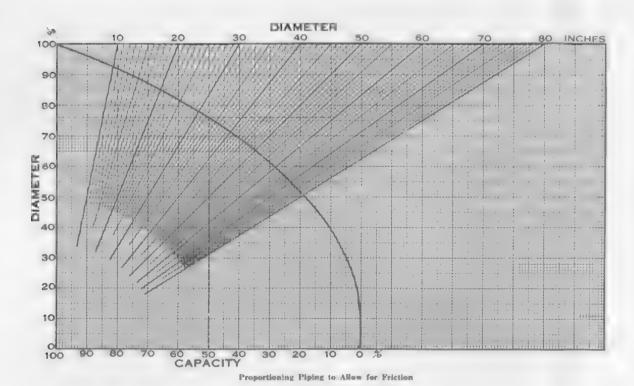
In carrying out this idea in the proportioning of the piping this company employs an original and accurate method. This method has been carefully tested and has been found to give an almost ideal distribution; the principle involved is to so proportion the velocities in the various pipe sizes as to give equal friction in all air pipes per running foot regardless of their size. It may easily be shown that the equation which relates the carrying capacity of pipe to its size to suit this condition is

$$\frac{\mathrm{d}_2}{\mathrm{d}_1} = \left(\frac{\mathrm{C}_2}{\mathrm{C}_1}\right)^{\frac{1}{16}}$$

Where  $d_1$  and  $d_2$  are the relative diameters of two pipes and  $C_1$  and  $C_2$  are the relative carrying capacities. As an equation in this form would be difficult of computation, the chart on page 64 is conveniently employed. In using this chart we start with the main pipe equal in area to the fan outlet, or 10 to 20% larger as circumstances may require. All sizes are proportioned directly from this main pipe



# size. It will be noted that the curve is plotted for per cent. capacity and for per cent. diameter according to the formula for constant friction per foot of length. For instance if we have a branch pipe which is required to carry 50% of the capacity of the main pipe, we find the point on the curve which corresponds to 50% capacity and which gives a corresponding point of 76% diameter; that is, a pipe to carry 50% of the capacity with the same friction per foot must have 76% of the diameter, which may be easily calculated or be read directly from the tables for various pipe sizes on page 113. It will be seen that straight lines are drawn for pipe sizes from 20" up to 80" in diameter. Supposing the size of the main pipe is 60" in diameter, then following from left to right along the line of 76% diameter to the line of 60" pipe we find from the scale above a diameter of 46", which is the size of pipe which has half the capacity of 60" pipe with the same friction per foot. By this method the sizes may be read off rapidly without any intermediate figuring whatever.





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#### Application

Take the following example which shows the method: Let the main pipe from the fan be 48" in diameter and suppose a straight duct having ten equal outlets. The first section of piping is 48", the second section has a capacity of 90%, the third section 80%, the fourth 70%, and so on; corresponding to 90% we find a diameter of 96% which for a 48" pipe gives us 46" for the second section. For the third section we have 80% capacity corresponding to 91% diameter or again following from left to right to the 48" line, we find a diameter of approximately 44". For the fourth section we have 70% capacity with a corresponding pipe size of 86½% of the main pipe and a diameter of between 41" and 42", determined as before. For the last section we have 10% capacity or 40% diameter which gives a diameter of between 19" and 20". The outlets may of course be proportioned independently; the same is true of exceptionally long branches which after having been figured in the ordinary way should be increased by a certain percentage throughout as judgment may determine, to decrease the friction.

#### **Determination of Friction**

For perfectly smooth, straight galvanized iron pipe it has been found as stated above that the loss of pressure in a length equivalent to 50 diameters is approximately equal to the pressure corresponding to the velocity, i. e., to the velocity head. This holds true for all gases under usual velocities and also for water. In brick and concrete ducts, however, it is advisable to figure 25% more friction or in other words a loss in pressure corresponding to the velocity head for every 40 diameters, i. e., in a 12" brick duct 40 feet long or 24" brick duct 80 feet long, the loss in pressure will correspond to the velocity. For instance, 2000 velocity under those conditions will cause a loss in pressure of one-fourth inch. In addition to the above it is necessary to figure the loss in elbows. The factor for elbows is difficult to determine exactly, but from the best information obtainable it appears that one elbow with usual radius is equivalent to a length of pipe of approximately ten diameters.

Now by the foregoing method of proportioning piping, it becomes unnecessary to figure the resistance of each section of pipe independently as the friction is constant per foot of length. It is simply necessary to know the length of the longest run of piping in feet, the number and sizes of elbows and the diameter and velocity in the largest pipe, as the loss is exactly the same as though the entire amount of air was carried through the largest pipe the entire distance. It is usual to figure the area of the main duct approximately equal to the area of the fan outlet. It should be noted that the velocity at the outlet of a Buffalo fan at the rated capacity is equal to one-half of the peripheral velocity, so that the velocity head in the main pipe will be  $(\frac{1}{2})^2 = \frac{1}{4}$  the total fan pressure. For convenience we may assume the fan to operate at one inch, that the loss in piping thus proportioned is one-fourth inch for every length equal to 40 diameters of the main pipe. As an example of this method of figuring suppose our main outlet is 48" in diameter and that there are ten sections proportioned as in the previous example. We will also say that the main section contains one elbow, and that there is also an elbow in the section 39" in diameter, one elbow in the section 30" in diameter and another elbow in the section 20" in diameter. Let the length of the pipe to the farthest outlet be 120 feet. We compute the friction in the following way.

120 feet is equivalent to
One 48" elbow is equivalent to
One 39" elbow is equivalent to
One 39" elbow is equivalent to
One 20" elbow is equivalent to
One 20" elbow is equivalent to

Total equivalent length 58.55 diameters of 48" pipe The equivalent loss in velocity head will then be

$$\frac{58.55}{40} = 1.46$$

times the velocity head in the 48" main. Further there is the velocity remaining in the 20" pipe which gives an additional loss evidently of 20% of one velocity head or .42 times the velocity head in the 48" main. This gives a total loss in the piping system of

$$1.46 + 0.42 = 1.88$$

times the velocity head in the 48" main. Assuming that the velocity in the 48" main is 2000 feet per minute corresponding to a velocity head of one-fourth inch, the loss of pressure in the piping system is then

$$0.25 \times 1.88 = .47$$
 in.

This amount is to be deducted from the total pressure of the fan instead of from the static pressure when the piping is connected directly with the fan outlet, as by the reduction of velocity in the piping we have utilized practically all the velocity pressure at the fan outlet. In a "blow through" apparatus, however, this loss in pressure must be deducted from the static pressure; allowance must likewise be made for the loss in entrance to the piping which may be estimated at 45% of the velocity head. It will thus be seen that a "blow through" system requires larger piping than the "draw through" system for the same results.

In ordinary "draw through" heating system apparatus it is usually advisable to limit the pressure loss in piping to 50% of the total pressure. In the above example it has been shown that 0.47" out of the total pressure of 1" is lost if we make the pipe the same size as the fan outlet, and therefore this is safe. However if pressure loss had been 0.65" and we wished to reduce to 0.5" we could use the following formula as a loss in pressure varies approximately as the square of the velocity

$$C_2 = C_1 \sqrt{\frac{P_2}{P_1}} = C_1 \sqrt{\frac{0.50}{0.65}} = 0.88C_1$$

Thus we get the same capacity with .5" loss as with .65" loss it would be necessary to increase the area of the piping throughout nearly 13%, or the diameters of all the pipes approximately 6%. Then instead of a 48" pipe it would be necessary to use a 51" pipe, inside of a 46" pipe a 49" pipe, etc.

#### Proportioning Ducts for Public Buildings

In public buildings the sizes of air-conveying ducts from fans or heaters to vertical induction flues, and the sizes of these flues, depend upon the velocities of the air flowing in such ducts and flues. The essential factors in determining these velocities are: the limitations of economical rotative speed of fans from the

Bulfalo

standpoint of power, the limitations of air velocities on account of noise or by reason of increasing friction as velocities increase; limitation of velocity of inflowing air through registers into rooms; the desirability of as high a velocity of air as is permissible under the limitations referred to in order to get as quick a conveyance of heat units from the heater to the rooms to be heated as possible and to keep down the size of ducts required; and the necessary initial and intermediate velocities to overcome the resistance existing in each particular system.

The size of vertical flues to the registers in the rooms is determined by the maximum velocities allowable in avoiding drafts and noise in the rooms. Practice has shown that the best velocities for the wall registers should be from 200 to 400 feet per minute over the face of the register depending upon the size and location; and for floor registers should be from 125 to 175 feet. The velocity in the vertical flues leading to the registers should be from 400 to 750. The size of these vertical flues is determined largely by the size of register desirable. In general, the velocity in these risers should be low, in order to obtain as uniform a velocity as possible over the register area.

The velocity in the horizontal ducts leading from the apparatus to the vertical risers is determined chiefly by the resistance of the duct. In practice these velocities will vary anywhere from 700 feet to 1200 feet depending upon the size, length of the duct, number of elbows, etc. A designer with considerable experience may proportion these ducts so as to give very uniform distribution without going into any extended calculation. However, it is desirable to have a correct method as a basis. For the benefit of engineers and architects we give here the method employed by this company in the determination of duct velocities and sizes.

The principal losses in piping systems for public buildings are in the horizontal ducts where the velocity is the highest. The losses in these ducts depend upon the velocity, the size and length of duct and upon the number of elbows. There is also considerable loss in pressure as the air enters the duct. An ideal system should take all these factors into consideration, and so proportion the velocities that the resistance would be practically equal in all ducts regardless of the length.

The system which we employ accomplishes this in a practical manner and at the same time avoids any laborious calculation. For each duct a factor may be obtained by inspection in accordance with the following formula:

$$F = 2\frac{1}{2} + \frac{1}{4W} + \frac{N}{5}$$

This factor represents the loss by friction in terms of velocity head. The first term, two and one-half, is approximately the number of times the velocity head lost by entrance to the pipe, entrance to the vertical flue, and loss in riser and register. The second factor represents the loss due to length and size of pipe; L is the length in feet and W is the approximate width in inches. The third term represents that proportion of the pressure lost in elbows, and N is the number of long radius elbows. One square elbow is figured equal to two long radius elbows. In checking over the piping layout the factors for the various ducts are first found as above and from these factors the velocity in the respective ducts are ascertained directly. In determining these velocities it is usual to allow a loss not exceeding one-fourth of the total fan pressure. This in practice usually amounts to about one-fourth of an inch. The velocity corresponding to a pressure of one-fourth of an inch is 2000,

and since the velocities vary as the square root of the pressure, the factor F and the velocity V will give a loss of one-fourth of an inch since

$$V = \frac{2000}{V \text{ F}}$$

In this manner the velocities are accurately and conveniently proportioned.

# The Following Table from an Actual Case Illustrates the Variation in Velocities which occur in a Correctly Proportioned System

No of Rooms	Contents Cubic Feet	B. T. U.	A. P. M. Required for Heating	A P M Required for Vent	A. P. M. Allowed	Min. Air Change	A. P. M. for Loca Duct	Pactor	Velients in Duct	Area of Digit Sq. Foot
1	5290	13020	260	352	352	15	352	3	950	3.71
9	25700	50380	1008	2570	2570	10	1285	5	730	1.75
3	6070	36240	725	405	760	8	760	6	670	1.14
4	3530	14015	280	235	250	13	280	3	950	.3
5	1860	7987	159	913	159	12	160	31,	850	.19
6	3400	13255	265	227	265	13	265	5	730	.37
7	6070	30370	726	405	726	9	726	7	630	1.16
8	1860	7960	159	903	159	12	150	4	820	.19
4)	55400	167000	3340	4440	4440	1219	2220	7	670	3.6

#### Heating Requirements of Buildings

Before deciding on the heating capacity required, the engineer must make an estimate of the heat losses from the building under the severest conditions of cold weather. The principal loss is by radiation, and as the result of exhaustive tests we have accurate data on the factors for various building materials and types of construction.

The values given on page 109 cover the various types and constructions most frequently met with in ordinary practice. These factors are subject to modification to allow for exposure to winds, unequal distribution of heat, and any extraordinary condition.

The heat required for ventilation is easily computed when the air supplied per hour is known. Since the specified heat of air at constant pressure is 0.238 and the weight of one cubic foot of air at 70° F. is 0.07495 pounds, one British Thermal Unit of heat will raise the temperature of one cubic foot of air

$$\frac{1}{0.238 \times 0.07495} = 56^{\circ} \,\mathrm{F}$$

#### Infiltration

Loss of heat through infiltration may properly be classed with ventilation losses. It varies greatly with the construction of the building and ranges from one air change in half an hour in a small and poorly constructed building, to one air change in two to three hours in a large well constructed building. This infiltration is caused in part by winds, but chiefly by the chimney-like effect of the column of air in a building at a higher temperature than that outside. The difference in pressure produced is proportional to the difference in temperature and the



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amount of infiltration is proportional to the square root of the difference in temperature, hence the heat losses due to infiltration may be expressed by the equation

$$H = C (t_2 - t_1)^{a_2}$$

#### Heater Performance

In modern methods of determining the size of apparatus, whether for heating or drying, the heat losses are first calculated in the manner just described. In public buildings the amount of air is usually specified and the required temperature of air for heating may be determined from the equation

$$t_2 = \frac{k \, l}{0.238 \times 60 \times wa} + t_r$$

in which  $t_2$  = the temperature of the air leaving the heater.

1 = the B. T. U. per hour hour lost by transmission through walls, glass surfaces, roofs, etc.

a = the cu. ft. of air required for ventilation.

t. = the temperature of the room.

w = weight of one cu. ft. of air (which taken at a temperature of 70° F. and 29.92" Bar., is 0.07495 lbs.)

k = is an assumed factor of safety chosen with reference to the particular conditions.

This formula may also be used in determining the volume of air required when the temperature of the air is specified.

Where "return air" is used, that is, air is recirculated from within the building instead of from without, the formula is modified as follows to give the total heat units required with a view of choosing a standard size of apparatus to meet the conditions.

$$H = 0.238 \text{ w n C } (t_r - t_1) \text{ k l}$$

in which n = number of air changes per hour due to the infiltration of cold air from without. This is dependent upon the size and construction of the building and must be chosen as a result of experiments and tests upon various types of buildings.

C = the cu. ft. contents of the room.

 $t_1$  = the outside temperature.

#### **Heating Surface**

The next step is to determine the total amount of heating surface in lineal feet of one-inch pipe.

Having previously determined the amount of air to be handled, we determine the size of heater by the free area required to allow the passage of the desired quantity of air at the velocity chosen, according to the following table.



#### Maximum Velocity Advisable Through Heater for Different Installations

Depth of Heater in Sections	In Public Binkhings	In Industrial Plant
-		
4	1140	1500
.5	1020	1350
ti	4636)	1230
7	560	1140
<b>\</b>	\$10	1070

The proper velocity for the air through the clear area of the heater will vary with the different conditions such as pressure carried and character of the installation. The table of velocities given above is based on the assumption that the pressure loss through the heater should not exceed 50% of the total pressure on the fan.

The velocities here given are intended merely to indicate the practical limit, and except where the ducts are very short it will be found advisable to keep below this. This is especially true in the case of public buildings, where the limit should not exceed 90% of the above.

Having determined the velocity through the heater the size of heater required can be readily chosen from the table of sizes and dimensions of Buffalo Standard heaters given on page 96. The same method can be used in connection with the Vento Cast Iron Heater tables given on page 104.

#### Friction of Heaters

It is even more essential to take account of the friction of the air passing through the heaters than through the piping. The loss of pressure here is much greater than ordinarily imagined and consequently many designers make the mistake of assuming higher velocities than are possible. The following table is compiled from careful tests on Buffalo Heaters.

#### Friction of Air Through Buffalo Standard Heaters

loss of air pressure in inches of water per square inch—air at  $70^{\circ}$  f

Velocity Threagh				NUMBER OF	SECTIONS			
Area	1	2	3	4	5	6	7	8
300	0.009	0.017	0.026	0.035	0.043	0.052	0.060	0.069
400	0.015	0.034	0.046	0.062	0 077	0.092	0.108	0.128
5(R)	0 024	0.049	0.073	0.095	0.104	0.144	0 168	0.192
450K)	0.035	0.069	0.104	0.138	0.173	0 207	0.242	0.276
7(10)	0.047	() ()514	0.141	0.188	0.235	0.282	0.329	0.376
500	0.061	0.123	0.184	0.245	0.306	0.368	0.429	0.490
1000	0.078	0.155	0 233	0.311	0.388	0.466	0.511	0.621
1000	0.096	0.191	0.287	0.382	0.479	0.574	0.670	0.765
1100	0.116	0.232	0.347	0 463	0.579	0.695	0.810	0.926
1200	0.138	0.276	0.414	0.551	0.689	0.827	0.565	1 108
1300	0.162	0.324	0.486	0.648	0.510	0.972	1.133	1 296
1 (H)	0.187	0.375	0.562	0.750	0.986	1.124	1 311	1.500
1500	0.215	0.431	0 646	0.861	1.077	1 293	1.508	1 722
16600	0.245	0 490	0 735	0.980	1.226	1.471	1.716	1.961
1700	0.277	0.555	0.831	1.110	1.387	1.664	1.940	2 218
ISONE	0.310	0.620	0.930	1.240	1.550	1.860	2.167	2 480



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The losses are figured for air volumes at  $70^{\circ}$ . For accurate estimating, correction should be made for the increase in volume due to rise in temperature. The preceding table enables us to read very readily the loss of pressure through the heaters. It is usually advisable to keep the loss in pressure in passing through the heaters down to 50% of the total pressure or less. Therefore for various pressures and various numbers of sections, the figures given in the previous table and based on 50% pressure loss should not be exceeded.

#### **Heater Connection**

Care should be taken to have the connection between the fan and the heater case of such a character that it will not restrict the flow of air or offer unnecessary resistance. This precaution is frequently overlooked, either throwing excessive pressure on the fan, or cutting down the quantity of air handled.

The following table gives the approximate lengths of connections advised for draw through installations.

#### Length of Heater Connection-For Draw Through Equipment

Size Fan Plan, whil	Size Fan Nia and Turbo Comidal	Distance from Fan- to Heater
Up to 70"	Up to No. 7	18" to 24"
70" 100"	No. 7 No. 10	24" to 30"
100" 130"	No. 10 No. 13	36"
130" 170"	No. 13 No. 17	42"
170° 200°	No. 17 No. 20	48" to 54"

#### Rate of Condensation

The effect of air velocity and temperature upon the rate of condensation is shown very nicely by the graphical representation of an actual test, on page 72. It will be noted that the rate of transmission decreases with the increase in the temperature of the air in passing through successive sections of the heater but increases very rapidly with the increase in air velocity.

#### Heater Size

The next step is the determination of the amount of heating surface or the number of heater sections required.

A most convenient method has been devised by our engineers. By means of the curves on page 73 the size of Buffalo Heater can be very readily determined. The use of these curves may best be illustrated by an actual application.

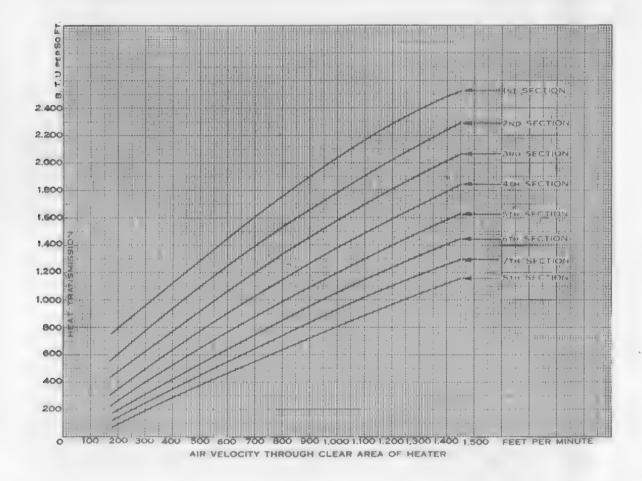
Assume:—Steam pressure on the coils to be 40 pounds, the air to enter at 20° F, and leave at 130° F, and pass through the heater with a velocity of 1000 feet per minute.



From the small curve we see that steam at 40 pound gauge pressure has a temperature of  $287^{\circ}$  F.

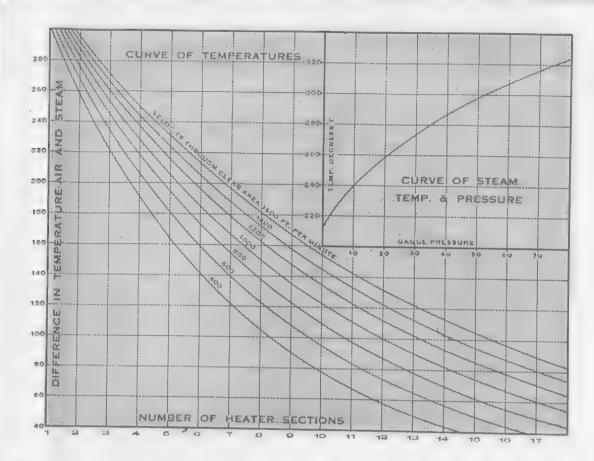
The difference between the temperature of the air entering and the steam will then be 267° and the difference between the air leaving and the steam will be 157°.

Taking the first difference, 267°, and following the line over to the 1000 vel. curve and then down we find 2.55 heater sections. Following the same procedure for the second difference, 157°, we obtain 7.57 sections. The difference between these two results will give the number of sections required which in the case in hand is five.



Buffelo

FAN System of Heating, Ventilating and Humidifying



### Condensation in Heater Coils

Having determined the amount of air passing through the heaters and the temperature use of this air the amount of steam condensed per hour can be readily calculated by raising the following formula:

$$C = \frac{\mathbf{a} \times (\mathbf{t}_2 - \mathbf{t}_1) \times 60}{55.2 \times 1}$$

#### When

a = cubic feet or air per minute.

t<sub>1</sub> = temperature of air entering coils.

t<sub>2</sub> - temperature of air leaving coils.

latent heat of steam.

55.2 = cubic feet of air raise 1.1° F. by 1 B.t.u.

### **Determination of Guarantees**

The case often arises that a guarantee to heat a building to a certain specified temperature must be demonstrated at a much higher outside temperature than called for in the guarantee. It then becomes important to know the exact relation between increase in inside temperature when apparatus is operated to its full capacity. This relation has been published for heating with direct radiation, but



it varies considerably from the results obtained with the fan system. Naturally the rise in the indoor temperature will be less than the rise in outdoor temperature owing to the fact that the condensing capacity of the apparatus decreases with the temperature. With a fan system heater the condensing capacity has been shown to be directly proportional to the difference in temperature between steam and air, while with direct radiation it is not directly proportional owing to the variation in convection currents. The same relation between indoor and outdoor temperature may be shown to hold true whether the system was designed to take the air from outdoors entirely or to recirculate air within the building. The formula expressing the relation between indoor and outdoor temperature in either case is,

$$T_r = \frac{T_r' (T_s - T_l) + T_o (T_l - T_l')}{T_o - T_l'}$$

 $T_r = T_{emperature}$  of building obtained with outside temperature  $T_1$ .

 $\Gamma_1$  = Any outside temperature at which test is made.

T,' = Temperature of building guaranteed.

 $T_1'$  = Specified outside temperature.

T. = Temperature of steam at pressure specified.

The table following shows corresponding indoor temperatures for various outdoor temperatures with guarantees at 60° to 95° in zero weather.

Table of Average Indoor Temperatures

MAINTAINED AT VARIOUS OUTDOOR TEMPERATURES WITH 5 LBS STEAM PRESSURE

-10	Dutdonr Temp.				Average Indoor	Temperatures			
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	~15 ~10	48.9 52.9	54.3 57.9	59 7 63.1	64 9 68 3	70.3 73.5	75.6 78.7	80 9 86 0	87.3 89.2
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	0	60°	65°	70°	75°	80-	851	90°	95°
65 107.8 111.4 115.0 118.6 122.1 125.7 129.3 132	10 15 20 25 30 35 40 45 50 55	67.4 71.0 74.7 78.4 82.1 85.8 89.4 93.1 96.8 100.5	72.1 75.7 79.3 82.9 86.4 90.0 93.6 97.1 100.7 100.4 3	76 9 80 3 83 9 87 3 90 8 94 3 97 7 101 2 101 7 101 8 1 111 6	81 7 85.1 88.4 91.8 94.1 97.5 101 8 105.4 108.5 111.0 115.2	86 5 89.7 92.9 96 2 96 4 102.6 105 9 109 1 112.4 112.5 6	91.3 94.4 97.5 100.7 103.8 106.9 110.0 113.2 116.3 119.4	96.0 99.1 102.1 105.1 108.1 111.2 114.2 117.2 120.2 123.3	100 8 103 7 106.6 109 5 112.4 115 3

### Specimen Problem

To heat a machine shop to 60° F. when 0° outside using all return air from the building. One complete air change every 30 minutes, 20 pound steam pressure at the heaters.

### Data

The building consists of three bays 35 feet wide, 215 feet long and 35 feet high, each bay having a saw tooth roof with a pitch of eight feet in the width of the



### FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

bay. The floor is of cement with wood above, the walls of brick  $17\frac{1}{2}$  inches thick with 20% of the wall area single thickness glass and the roof of paper, tar and gravel laid on two-inch planks.

### Solution

Surface	Area	Transmission Lector B. T. U. per 1 per Hour	Transmission Less B T U per P per Hour
Floor Walls Glass Roof	25,720 24,300 6,080 24,460	0.10 0.25 1.09 0.26	• 2,572 6,075 6,030 6,880
cubic contents =		1 003 275	64

Total cubic contents =	1,003,275 cu. ft.	
Infiltration, one air change per hour =	1,003,275 cu. ft.	
B.T.U. per $1^{\circ} = \frac{1,003,275}{55.2} =$	18,200	
Total B.T.U. per 1° difference =	40,375	
Total B.T.U. loss per hour = $40.357 \times 60 =$	2,421,420	
Add 15% margin =	2,784,633	
B.T.U. per minute = $\frac{2,784,633}{60}$ =	46,411	
Air required per minute = $\frac{1,003,275}{30}$ =	33,442	

Final temperature of air leaving heaters =  $60 + \frac{46,411 \times 55.2}{33,442} = 137^{\circ}$  F.

Assume a velocity of 1200 ft. per minute through the clear area of the heater, this will require a heater having

33,442 = 27.9 sq. ft. clear area.

1200

From the table on page 96 we find we can use either the 7'-0"x8'-4" section having 27.2 sq. ft. clear area or the 7'-0"x8'-10" section having 29.0 sq. ft. clear area.

The first section will give a velocity of

 $\frac{33.442}{27.2}$  = 1,230 ft. per minute,

which is close enough to the original assumption of 1200 ft. per minute.

Turning to the table on page 99 we find that with air entering at 60° F. and a velocity of 1200 ft. per minute through the free area of the heater 5 sections of heater will raise the temperature of the air to 143° F. This will decrease slightly due to the actual velocity through the heater being 1230 ft. instead of 1200 ft. per minute.

Let us assume the static resistance of the entire system as two inches and choose a fan to meet our requirments.

From the table on page 78 we find we can use a 120° planoidal fan which will give 37,050 A.P.M. at 351 R.P.M. by running slightly under rating, or a 110° planoidal fan which gives 31,000 A.P.M. at 382 R.P.M. by running over rating.

From table on page 79 we can use No. 9 N.C. rated at 35,050 A.P.M. at 364 R.P.M. running under rating.

From table on page 80 we can use No. 9 T.C. rated at 31,800 A.P.M at 621 R.P.M. running over rating

### Buffalo "Baby Conoidal" Fans

	I	DIMENSION:	s		Air	PRES	SURE		FREE DE	LIVERY
Number of Fan	Dimeter of Wheel Tuches	Diameter of Talet Outsides Taches	Deam ter of Outlet (Outside Inches	Revolutions per Minute	per Minute Cuba Feet	Statis Inches Water	Total Inches Water	Power	Air per Minute Cubic Feet	Horse Power
1	4	4	3	1740	80	0.17	0.43	0.012	135	0.030
2	434	512	4	1140 1740	88 135	0.17	0.25	0.009	150 230	0 025 0.073
3	67.8	78	53 <sub>3</sub>	1140 1740	260 400	0 38 0 88	$0.54 \\ 1.25$	0 050 0 180	450 690	0.120 0.440
4	1014	1135	834	870 1140 1440 1740	700 915 1155 1400	0 50 0 86 1.37 2 00	0.72 1 23 1 96 2 86	0 14 0 31 0.63 1.10	1200 1575 2000 2400	0.34 0.75 1.50 2.65
5	$13\frac{1}{16}$	1414	10 <sup>7</sup> q	690 870 1140 1440	1080 1360 1785 2255	0.49 0.78 1.35 2.15	0.71 1.13 1.94 3.08	0 22 0.41 0.90 1.81	1870 2350 3050 3880	0.53 1.00 2.16 4.35
6	15 <sup>5</sup> k	1712	Rectangle	690 870 1140 1440	1855 2340 3065 3875	0.71 1.13 1.94 3.10	0.98 1.56 2.67 4.25	0 51 1.00 2.26 4.55	3260 4075 5335 6740	1.21 2.36 5 43 11 00

### Capacities of Buffalo Steel Plate Cone Wheels

Under Average Working Conditions at 70° F. and 29.92° Barometer.

S.	I per M at res very	1,8	Static Pre	н	K	Static Pre	۹۲,	1 7	Static Pre	۹,	3	Static Pre-	7
Sales.	APM R.P.M Dealy	R.P.M.	Vol.	Н. Р.	R.P.M.	Vol.	H. P.	R.P.M.	Vol.	н. Р.	R P.M	Vol.	н. Р.
30	10	393	2,300	0.43	480	2,810	0.79	555	3,250	1.21	GSO	3,990	2.23
36	17	328	3,330	0.62	400	4,060	1.13	463	1,700	1.75	568	5,760	3.22
42	27	252	4.530	0.85	343	5,530	1.55	396	6,390	2 39	486	7,840	4.39
48	40	246	5,900	1.10	300	7,210	2.02	347	8,350	3.11	425	10,220	5.72
54	57	219	7,480	1.39	266	9,150	2.54	308	10,550	3.92	378	12,950	7.22
60	78	197	9,200	1.71	240	11.250	3.14	278	13,000	4.84	340	15,950	8.90
66	105	178	11,150	2 10	218	13,600	3.83	252	15,750	-5.90	309	19,300	10.9
72	136	164	13,300	2.48	200	16,250	4.51	232	15,500	7.00	284	23,050	12.9
84	214	141	18,100	3.38	172	22,100	6.19	199	25,500	9,55	244	31,350	17.6
5166	322	123	23,600	4.40	150	25,500	8.07	174	33,350	12.4	243	40,900	22.9
108	459	100	29,050	5.55	133	36,600	10.2	154	42,250	15.8	150	51,900	29.0
120	631	118	36,800	6.85	120	45,000	12.6	138	52,000	19.4	170	63,800	35.6
144	1085	82	53(000)	9.90	100	64,850	18.1	116	75,000	, 28.0	142	91,850	51.5
168	1730	71	72,400	13.5	86	88, 150	21.8	100	102 000	38.2	122	125,200	70.2
180	2100	66	83,250	15.5	80	101,800	28.1	93	117,500	13.9	114	144,200	80.6

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

### Buffalo Disc Wheels (Type D)

5111	Velents Through	Cubic Feet	0.1"	S.P.	() 💬 *	SP	0.3"	S.P.	11-4"	S.P.	0.5*	SP.	0,75	* S.P.
Litte	Wieel	per Minute	R P.M	H. P.	R P.M	Н. Р.	R.P.M.	H F	R.P.M.	н. Р.	R.P.M.	H. P.	R P M	HP
18"	74 (0) 20 (0) 2 (4) (1) 2 (4) (1) 2 (4) (1)	\$\$2 1,762 2,170 3,660 1,590	739 1100 1375	0.051 0.142 0.281	\$71 1267 1365 1966	0.104 0.23 0.40 0.80	978 E385 1670 2080 2507	0.163 0.32 0.52 1.00 1.73	1466) 1477 1772 2200 2600	0.227 0.41 0.61 1.15 1.92	1132 1558 1870 2200 2003	0.30 0.51 0.76 1.32 2.29	1297 1730 2045 2484 2968	0.50 0.77 1.08 1.68 2.67
21"	1400 0 1400 0 1400 0 240 0 240 0	1,570 3,140 4,400 6,280 5,170	554 825 1030	0 091 0 25 0 50	655 950 1150 1475	0.185 0.11 0.71 1.43	7.54 1040 1255 1560 1880	0.29 0.57 0.92 1.77 3.08	796 1408 1430 1650 1950	0 41 0 73 1.14 2.04 3.42	\$50 1168 1402 1718 2020	0 53 0 91 1 36 2 34 4 08	972 1298 1534 1564 2150	H 88 1.38 1.92 2.99 4.76
.50°	\$1.000 \$1.000 \$3.000 \$1.000 \$2.000 \$1.000	2,350 4 940 6,880 9,840 12,767	111 6/0 822	0 142 0 39 0.78	524 760 920 1180	0.29 $0.64$ $1.11$ $2.24$	588 830 1000 1247 1505	0.45 0.89 1.43 2.76 1.81	635 886 1062 1320 1500	0.63 1.14 1.78 3.19 5.35	934 934 1121 1373 1645	0.83 1.12 2.12 3.65 6.35	777 1039 1227 1391 1745	1.37 2.16 3.00 4.67 7.43
Jt,"	5000 (51000) (5000) 2000) 2000)	3,535 7,060 9,966 14,156 18,340	1666 550 687	0 21 0 37 1 13	436 642 765 981	0.12 0.92 1 60 3 22	188 692 837 1040 1255	0 65 1 28 2 66 3 95 6 92	530 740 888 1400 Jano	0 92 1 64 2 56 4 60 7 70	566 778 935 1116 1318	1 20 2.04 3 05 5 27 9:20	648 865 1024 1243 1454	1 98 3 00 4 32 6.73 10.71
12"	Gapen 1 (m.)e r 3 (be)e r 2 (m.)e r 2 (m.)e r	4,868 9,646 13,475 19,232 25,025	116 472 555	0.28 0.77 1.58	374 514 656 814	0.57 1.25 2.17 4.37	420 594 715 592 1074	0.89 1.71 2.50 5.43 9.43	456 632 760 944 1114	1 24 2 24 3 48 6.25 10 45	486 668 802 982 1151	1.63 2.78 4.15 7.17 12.50	556 742 876 1066 1246	2 60 4 21 5 58 9 15 14.58
187	5000 1(000 13(0) 2(0) 2(0)	(i,250) 12.560 17.560) 25.120 32,680	277 412 315	0.36 1.01 2.00	327 173 373 737	0.74 1.63 2.84 5.72	567 520 627 780 910	1 16 2.27 3 67 7 68 12 32	388 364 665 825 975	1 62 2 92 4 56 8 16 13 68	125 584 701 859 1010	2 13 3.63 5 42 9 35 16 33	186 649 767 933 1000	3 52 5 50 9 68 11 96 19 04
]w	500 1000 1400 2000 2600	7,948 15,890 22,275 31,795 41,390	216 366 157	1.28	201 122 510 655	0 94 2 07 3 60 7.22	326 461 557 694 836	1 47 2 88 4 66 8 95 15 60	354 491 500 734 806	2 05 3 72 5 77 10 30 17 30	377 518 623 713 898	2.70 1.60 6.56 11.55 20.65	132 577 682 828	1.46 6.96 9.72 15.14 21.10
60"	5001 10001 14001 2000 20001	9,842 19,025 27,500 39,230 <b>51,061</b>	201 70 412	0.57 1.58 3.13	232 350 450 590	1 16 2 55 4.44 8 94	293 416 502 624 751	1 81 3 54 5 74 11 10 19 30	519 113 532 660 780	2 52 4 57 7 13 12.80 21 4	310 107 761 688	3 3 3 5 67 8 53 1 4 62 25 5	389 519 614 716 872	5.50 8.60 12.00 18.70 29.8
72" (	500 1400 1400 2000 2000	14,130 28,200 39,600 56,520 73,530	185 275 311	0.82 2.36 4.50	218 317 383 490	1.66 3.67 6.40 12.90	215 347 417 520 627	2 61 5 12 5 26 15 90 27.7	265 370 442 550 650	3 63 6 58 10 20 18,30 30 8	28.1 389 468 573 674	4.80 5.16 12.20 21.1 10.5	123 133 512 622 727	7.92 12.38 17.29 26.9 12.8
×1.	Gene 1600a 2310a 2000a 2000a	19,2332 38,166 53,900 76,950 100,100	1 15 2 16 21 4 5	1 11	187 272 328 432	2 27 5 00 8 68 17 50	210 297 478 416 547	3.55 6.95 11.20 21.70 37.7	228 316 380 472 107	4 95 8 95 1 1 90 25 00 H S	243 334 401 401 577	5 51 11 14 16 61 25 7 50 0	275 371 185 533 623	10.78 16.55 33.5 36.6 38.1

Buffalo

Buffalo

### Capacities of Buffalo Planoidal Steel Plate Blowers (Type L) Under Average Working Conditions

70° F. 29.92" Barometer

	Dinmeter of	Arrys		Static Press 0,288 Ounc			statue Press 0.433 Ounc			tane Press 0.577 Oune			static Pro 0 865 Out	
P124	River Wheel Inches	Outlet Square Ft	RPM	Volume   Cubic Et. per Min	H 1'	RPM	Volume Cubic Ft per Min	н Р.		Volume Cubic Ft. per Min	H.P.		Volume Cubic I t per Min.	н.Р.
.( . 3.5 14)	$\frac{10^{\frac{1}{4}}}{22^{\frac{1}{4}}}$	0.77 1 01 1 35	1175 550 500	1,360 1,570 2,065	023 031 031	710 623	1,420 1,425 2,530	0.42 0.58 0.75	958 820 719	1,640 2,530 2,630	0.65 0.87 1.16	1174 1005 551	2,010 2,720 3,580	1 19 1 63 2.13
45 50 55	297 4 421 4 35 1 4	1.75 2.16 2.61	451 107 300	2,640 3,220 3,890	0.52 0.61 0.77	553 498 1 452	3,185 3,940 4,765	0.986 1.18 1.42	639 575 522	3,680 4,550 5,500	1.47 1.82 2.49	783 705 640	4,510 5,580 6,740	2.70 3.35 4.03
70 20	350g 45 5125	3.13 4.26 5.54	239 290) 254	1,630 6,320 8,230	$\frac{0.92}{1.25}$ $\frac{1.25}{1.64}$	415 355 315	5,675 7,730 10,080	$\frac{1.70}{2.31}$ $\frac{3.02}{3.02}$	179 110 359	6,550 8,930 11,630	2 61 3 55 4,65	387 302 140	\$,030 10,920 14,250	1.80 6.52 8.55
10(1 1130) 1](1	$\frac{577}{64}$ $\frac{641}{703}$	7.10 8.75 10.57	226 203 185	10,440 12,880 15,650	2 08 2 56 3 10	276 248 226	12,750 15,750 19,100	3.82 4.71 5.71	319 287 261	14,730 18,200 22,000	5 88 7.25 8.78	391 352 320	18,050 22,300 26,950	10 80 13.32 16.12
120 130 130	77 14 5(3 1 2 (90)	13.00 11.85 17.20	166 156 145	18,530 21,600 25,200	3 69 4 31 5 02	1 207 192 177	22,700 26,450 30,850	6.78 7.98 9.24	239 221 205	26,200 80,550 85,650	10.44 12 26 14.20	293 271 251	32,080 37,110 43,700	19.18 22.40 26.10
150 Foli 170	965 <sup>1</sup> 2 103 104 <sup>1</sup> 4	19 70 22 10 25 10	135 127 120	28,956 32,500 37,150	5.76 6.57 7.42	165 154 146 138	35,400 40,200 45,500	$\begin{array}{c} 10\ 60 \\ 12\ 10 \\ 13\ 65 \end{array}$	191 179 100	10,900 46,150 52,550	16 30 18 60 21.00	234 219 207	50, 150 56, 900 64, 100	29 95 34 15 35 60
150 190 200	$\frac{115^{8}4}{122^{1}4}$ $\frac{122^{1}4}{128^{1}2}$	28.50 31.70 35.30	112 107 102	41,700 46,300 51,500	8.31 9.26 10.25	131   125	51,100 56,700 63,100	15 25 17 05 18 85	150 151 144	59,000 65,500 72,850	23 50 26 20 29 00	195 185 176	72,250 90,250 90,200	43 15 48 10 53 30
	Diameter of Blast	Area		Static Press 1 151 Outo			Static Pre I 442 Oun			tatic Pres 1 734 Cun		315"	Statue Pro 2.019 Out	
Nager	Wheel Inches	Outlet Square Ft	R.P. M.	Volume Cubic Ft per Min.	H.P.	R.P.M.	Volume Cubic Ft per Min.	н.Р.	R.P.M.	Volume Cubic Pt. per Min.	н.Р.	R.P.M.	Volume Cubic Ft. per Min.	н.Р.
30 35 40	$\begin{array}{c} 10^{1} 4 \\ 22^{1} 4 \\ 25^{3} 4 \end{array}$	0.77 1.04 1.36	1 1355 1 160 1018	2,320 3,140 4,135	1.84 2.52 3.25	1515 1295 1135	2,595 3,510 4,620	2 57 3 48 4 58	1660 1420 1245	2,840 3,845 5,060	3 38 4 63 6 03	1792 1534 1345	3,070 4,155 5,160	4 26 5 %3 7 60
45 50 55	2074 821 <sub>8</sub> 851 <sub>9</sub>	1.75 2.16 2.61	904 814 738	3,210 6,440 7,750	4 15 5.15 6.19	1010 910 826	5,825 7,200 8,700	5 81 7 20 8 66	1108 996 904	6,375 7,580 9,580	7.63 9.45 11.38	1195 1076 976	6,890 8,510 10,290	9 63 11 91 11 34
60 20 50	$\frac{3816}{45}$ $\frac{45}{51^{3}}$	3.13 4 26 5 54	678 580 508	9,260 12,630 16,450	738 10 02 13.12	758 648 565	10,370 14,120 15,400	10 31 14 03 18 10	530 710 621	$\begin{array}{c} 14,340 \\ 15,360 \\ 20,150 \end{array}$	13 55 15 45 24 20	896 767 672	12,250 16,700 21,750	17 10 23.25 30.50
90 100 110	$\frac{5778}{64}$ $\frac{641}{8}$ $\frac{703}{4}$	7 10 8.75 10.57	451 406 369	20,850 25,750 31,100	16/60 20/48 24,80	505 454 413	23,300 28,800 34,800	23 30 25 70 34 70	553 497 452	25,500 31,530 38,100	30 55 37 70 45 60	5/47 5/37 4/5/5	$\begin{array}{c} 27,550 \\ 34,050 \\ 41,200 \end{array}$	35 50 47 50 57.50
120 330 150	7716 8012	13.00 14.85 17.20	338 313 290	37,050 48,250 50,400	29 50 34 50 40.15	378 350 324	\$1,400 \$5,350 56,100	41.30 48-25 56-15	814 383 355	45,400 52,90 t 61,750	54-25 63-40 73-80	447 113 3×1	49,000 57,200 66,700	88.40 80,00 43.00
150 1140 170	10/1 L	19.70 22 10 25 10	270 253 239	57,300 65,700 74,300	46 10 - 52 60 59 40	BrQ 201 207	64,750 73,500 83,200	64 50 73 50 53 00	331 310 293	70,900 80 100 91 000	84 70 96 60 109 00	358 345 316	76,600 86,900 (18,100)	121 80
150 190 200	$\frac{115^{4}_{4}}{122^{4}_{4}}$ $\frac{122^{4}_{4}}{128^{4}_{2}}$	28.50 31.70 35.30	225 214 204	\$3,500 92,650 104,000	145 40 74 2 1 82.00	251 239 224	93, 100 103, 700 115, 100	93 00 103 60 114 70	277 252 250		122 20 133 00 150 80	2654 2654	110,100 122,500 136,300	154 00 171 50 190 00

| Dotal Pressure is 126' of the Rated Static Pressure.

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

# Capacities of Buffalo Niagara Conoidal Fans—(Type N) Under Average Working Conditions 70° F and 29.92° Barometer

	Diameter Blast	No. is	1 **	State Pro- 0 288 Chine	HARITE	1 d ma	Static Pres 0.433 Our	nn 11/81* . e. e.n.	1"	State Pres 0 577 Our	* III (* * * * * * * * * * * * * * * * *		Static I'm  () Say Chiz	
Sin	Wheel Inches	Outlet Square Ft.	R.P.M	Volume Cubic Ft. per Min.	H.P.	R.P.M.	Volume Cubic Ft. per Min.	н.г.	R.P.M.	Volume Cubic Ft.	н.г.	R.P.M.	Volume Cubic Ft per Min.	H.P
3	157	1.31	511	1,945	0.25	668	2,380	0.51	7711	2,730	0.78	943	3,365	1.1
3! <sub>3</sub>	187	1.79	115	2,642		572	3,240	0.69	660	3,740	1 06	809	4,380	1.1
4	201	2.33	108	3,459		500	4,230	0.90	577	4,895	1 39	709	5,980	2.3
412 5 512	231 <sub>2</sub> 291 <sub>4</sub> 281 <sub>4</sub>	2.95 3.64 4.41	3345.2 34293 25045	\$,375 5,400 6,540	0.77 0.94	445 400 364	5,350 6,610 8,000	1.11 1.41 1.71	514   462   420	6,195 7,645 9,250	1.75 2.16 2.62	630 566 515	7,575 9,350 11,320	3 ; 4,4 8 2
	31 1 . 36 1 2	5.25 7.14 9.33	27.2 233 204	7,780 10,590 13,520	1.11 1.52 1.98	334 286 250	9,525 12,950 16,910	2.63 2.77 3.61	386 330 289	11,000 14,980 19,550	3.12 4.24 5.54	472 105 351	13,450 18,330 23,950	5.8 7.5 10.3
10 10	\$7 52 58	11.81 14.58 17.64	181 103 148	17,500 21,600 26,150	2.51 3.00 3.74	222 200 182	21,400 26,450 32,000	4.57 5.65 6.85	256 231 240	24,750 30,550 37,000	7 01 8 65 10 48	314 283 287	30,300 37,400 45,250	13 ( 16 1 19.4
12	613	21.(a)	136	31,100	4.45	167	38,100	8.15	193	44,050	12 48	236	53,900	23 2
13	65	21 (6)	125	36,500	5.22	154	44,700	9.56	178	51,650	14 62	217	63,200	27 2
14	73	28 68	116	42,350	6.06	143	51,900	11.08	165	60,000	16.96	202	73,200	31 5
15 16 17	75	32 81 37 32 42.14	1090 1002 565	48,550 55,300 62,500	6.95 7.91 8.95	133 125 118	59,500 67,750 76,500	12.70 14.46 16.32	154 144 136	68,850 78,300 88,400	$\begin{array}{c} 19.49 \\ 22.15 \\ 25.00 \end{array}$	189 177 167	\$4,100 95,750 108,000	36 2 41.2 46.5
18	43-8	42.24	91 56 52	70,000	10 01	111	85,600	18 30	128	99,100	28.05	157	121,200	52.1
10	494	52.68		78,000	11 15	105	95,500	20 10	122	110,200	31.25	149	135,000	58.6
20	\$145	58.32		86,150	12 36	100	105,850	22 60	116	122,200	34.65	142	149,500	64.4
	Diameter	Area		Statue Pros 1 154 Oun			Static Pres 142 Outen			Static Press 1.734 Ours			Static Pro 2 019 Oun	
Dige:	Ri est Wheel Inches	Outlet Square Ft	R.P.M.	Volume Cubic Ft. per Min	H.P.	R.P.M.	Volume Cubic Ft per Min	H.P.	R.P.M.	Volume Cubic Ft per Min	H.P.	R.P.M.	Volume Cubic Ft. per Min.	H.P
3	15%	1 31	1088	3,880	2.21	1215	4,350	3 (18	1332	4,770	4 05	1443	5,150	5.1
31 <sub>2</sub>	18%	1.70	988	5,300	3.01	1010	5,930	4.19	1141	6,195	5 53	1238	7,010	6.9
4	200 g	2 34	817	6,920	3.93	912	7,730	5.47	1000	8,480	7.22	1082	9,160	9.1
41 <sub>2</sub>	253 7	2 05	726	8,750	4 97	810	9,795	6 93	890	10,740	9 14	1864	11,590	11.5
5	253 7	3,61	655	10,820	6,15	730	12,070	8 55	800	13,250	11 26	Ses	14,300	14.2
51 <sub>2</sub>	253 4	4 41	595	13,100	7 43	664	14,600	10 35	728	16,030	13.62	786	17,300	17.2
6	$\frac{315}{364_2}$	5 25	545	15,550	8 85	609	17,390	12 30	667	19,090	16-22	723	20,600	20.5
7		7.14	465	21,200	12 02	522	23,650	16 75	572	26,000	22.10	620	25,650	27.9
8		9 33	466	<b>27,650</b>	15 70	156	30,900	21 90	500	33,950	28-85	512	30,600	36.5
9	47	11.81	364	35,030	19 90	405	39,100	27 70	445	42,950	36 55	482	46,350	46.2
10	32	14.58	397	43,250	24 55	365	48,300	34 20	400	53,000	45 15	133	57,200	57.0
11	38	17.61	297	52,300	29 70	332	58,450	41 45	364	64,100	54 60	394	69,300	69.0
12	63	21.00	272	62,300	35 50	304	69,550	49 25	334	76, 100	65 00	361	\$2,500	82.1
13	65	24.65	252	73,050	41 50	280	81,600	57 80	308	89, 550	76 30	334	96,750	56.1
14	73	28.68	234	84,600	48 45	261	94,600	67.05	286	103, 900	88,70	310	112,050	111.9
15	75	32 80	218	97,250	55 25	243	108,700	77.00	267	119,200	101.50	289	128,800	128.2
16	54	37 32	204	130,750	62 85	225	123,600	87.50	250	135,800	115.60	271	140,100	146.0
17	56	42 14	192	125,000	71 00	214	139,500	99.00	235	153,100	130.80	255	165,300	164.8
18	984	47.24	182	140,000	79 50	201	158,500	110 SU	222	171,800	146 00	241	185,300	181 6
19	584	52.68	172	150,000	88 55	192	174,200	123 40	211	191,200	162 80	228	203 200	206 0
20	105	58.32	164	173,000	98 25	1%3	193,000	136 SB	200	212,000	180 30	217	229,000	228 0

I at J Pressure is 127.4% of the Rated State Pressure,

# Capacities of Buffalo Turbo Conoidal Fans (Type T) Under

Average Working Conditions
70 F. and 29.92' Barometer

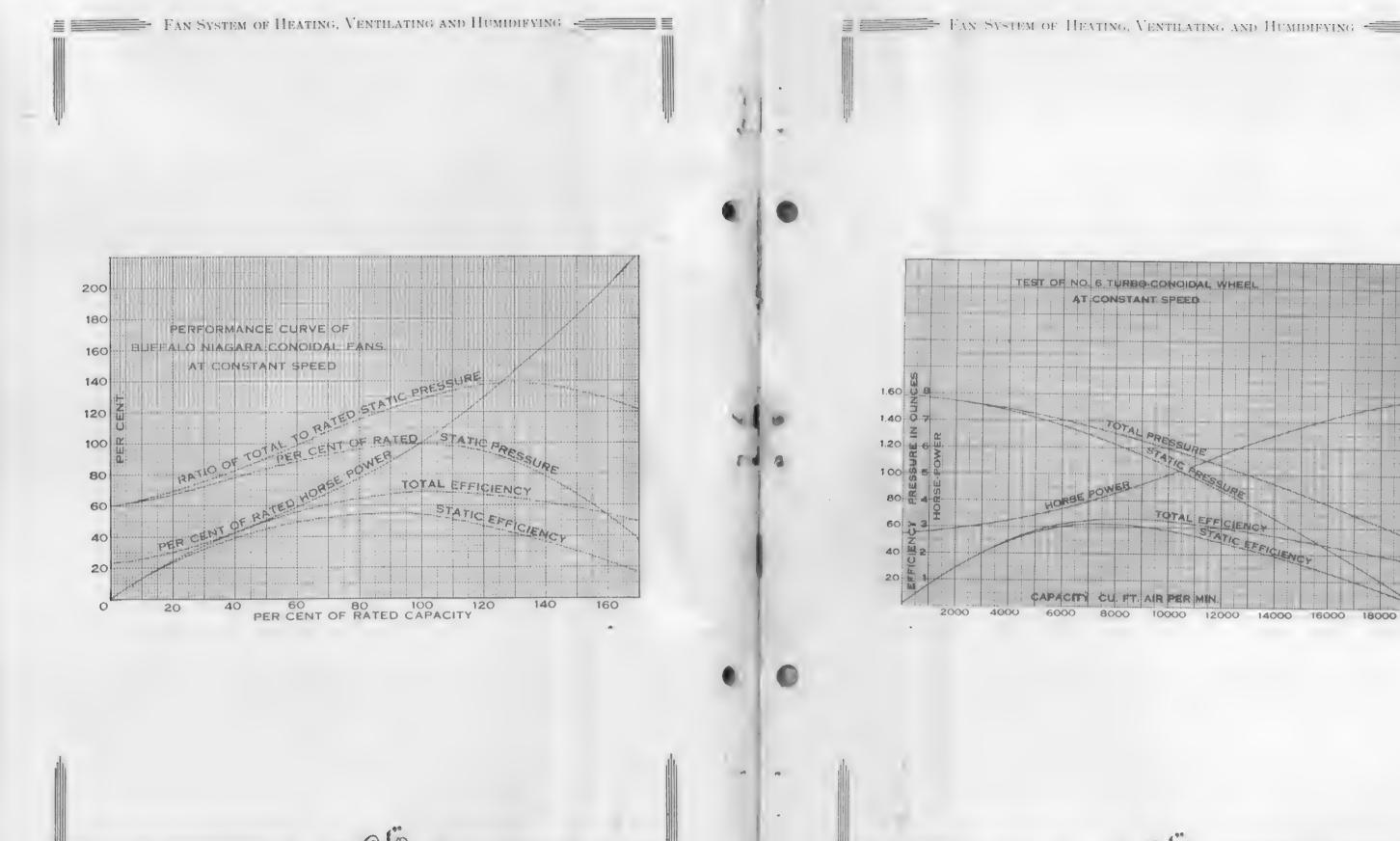
					10	0 / 0(3)50								
I	Dinmater et	Arr &		Static Pres 288 Ounces			Static Press 0.433 Chine			tyro Promi 9,577 Ogne			State Pre 0.865 Oune	
2171	W heed	€ 114t (× 1		Volume			Volume			Volume			Volume	
	Itarija -	Square Ft	R.P. M	Cubic Et per Min	HP	R.P.M.	Calme Ft.	H P	R P.M.	Cubic Ft. per Min	H.P. ]	RPM.	Cubic Ft.	II P.
21 2 3 1 2 4 1 5 2 5 1 2 7 1 7 7 1 7 1 1 1 2 1 3 1 1 5 1 1 5 1 1 5 1 1 5 1 5 1 5 1 5	14 1 4 17 1 4 20 1 2 2 1 4 2 5 1 2 3 1 1 4 3 1 0 6 3 1 1 4 3 1 0 6 3 1 1 4 3	0.91 1.31 1.79 2.33 3.64 4.41 5.25 6.16 7.11 8.19 9.33 10.53 11.81 21.05 21.05 22.68 32.32	1,115 980 797 699 556 565 567 165 328 372 328 319 251 198 1198 171	1,230 1,770 2,410 3,140 3,980 4,940 5,950 7,070 8,500 11,050 12,590 11,950 23,800 24,800 23,800 33,200 35,600 14,200 35,600 10,800	0.20 0.28 0.39 0.51 0.79 0.96 1.14 1.33 2.78 2.26 3.82 2.56 3.82 4.55 3.4 6.20 7.11 8,09	1,368 1,140 976 856 760 684 570 526 456 456 456 456 456 342 341 288 244 228 214	1,500 2,160 2,940 3,850 4,860 6,000 7,270 8,650 10,200 13,500 13,500 17,580 19,450 29,100 34,690 40,600 47,100 54,050 61,500	0 36 0.52 0.71 0 98 1 45 1 45 1 206 2 46 2 25 3.72 4.71 5 82 7 05 5 40 9 85 11.308 14.90	264	1,740 2,500 3,410 4,450 5,610 6,950 10,000 11,750 13,610 17,880 20,100 22,500 27,500 33,700 47,000 54,500 71,200	0.56 0.81 1.10 1.14 1.14 1.15 2.25 2.72 3.24 3.80 5.40 5.40 5.05 5.75 0.60 10.90 12.95 15.20 12.95 20.20 23.00	1,035 3,610 1,380 1,208 1,075 966 840 645 604 536 183 180 182 372 345 345 345 345 345 345 345 345 345	2.120 3.086 4,166 5,440 8,560 10,396 12,256 16,556 16,556 12,756 24,060 44,160 49,060 57,560 87,100 87,100	1 03 1 48 2 02 2 64 3 34 1 12 5 00 5 .77 9 96 9 .27 10 55 11 90 13 .35 16 .50 27 90 3 2 3 5 12 25
Sizi	Districted of Rhyt	Area of Outlit		Static Pres 1.154 Our			Static Pres 1 442 Oun			Static Press		31,	State: Pres 2.019 Ours	12/14
Colffee.	Wheel Inches	Square Ft	R P M	Volume Cubic Ft per Min.	нР	R.P.M	Volume Culue Et per Min	HP.	R.P.M.	Volume Cubic Ft per Min.	H.P.	R.P.M		HP
21 2 2 2 2 2 3 4 4 5 5 1 6 6 7 7 × 8 4 9 1 1 2 5 1 1 1 5 6	3434	0.91 1.31 1.79 2.33 3.64 4.41 5.25 6.16 7.14 8.19 10.53 11.81 14.58 17.64 21.05 21.05 20.08 3.08	2,225 1,895 1,395 1,395 1,217 1,015 1,117 1,015 1,015 799 799 657 621 559 546 1,30 3,30 3,30 4,30 3,30 4,30 4,30 4,30 4	2, 455 3,540 4,500 5,270 9,800 11,120 16,120 16,250 22,100 28,100 28,100 28,100 31,500 56,200 66,200 76,800 88,500	30 85 36 75 43 05 50 00 57 40		2,754 3,950 5,890 7,050 8,920 11,990 13,300 15,800 18,600 21,550 24,750 35,600 4 1,000 55,250 63,500 71,900 86,500 97,900 112,700	2,222 3,19 4 35 5 68 7 19 8 87 10 75 11 278 15 90 22 77 25 66 28 77 25 66 06 00 00 09 78 80 90	2,282 1,958 1,713 1,522 1,570 1,240 1,141 1,150 1,141 1,50 1,141 1,50 1,50 1,50 1,50 1,50 1,50 1,50 1,5	3,010 1,350 5,890 7,700 9,740 12,000 14,550 17,000 26,500 22,556 22,556 30,801 31,755 48,100 60,256 81,400 94,360 118,000	2 94 1 23 5 75 7 52 9 52 11 73 14 23 16 92 24 66 23 66 24 66 33 95 37 96 56 96 67 70 79 14 92 14 120 56	2,463 2,115 1,850 1,850 1,645 1,345 1,345 1,345 1,345 987 925 870 925 870 970 970 970 970 970 970 970 970 970 9	3,2591 1,0891 6,000 8,000 10,550 13,550 15,750 15,750 25,650 25,650 25,650 25,650 25,260 31,660 31,660 31,660 31,660 31,660 31,660 11,750 11,7	3 (9) 5.30 7.22 9.15 11.95 11.75 21.97 22.99 37.77 42.25 47.84 49.66 115.66 133.00

Total Pressure is 122.7%, of the Rutol Static Pressure

170
160
150
140
130
120
110
100
90
80
70
60
50
40
30
0
20
40
60
100
100
120
140
160

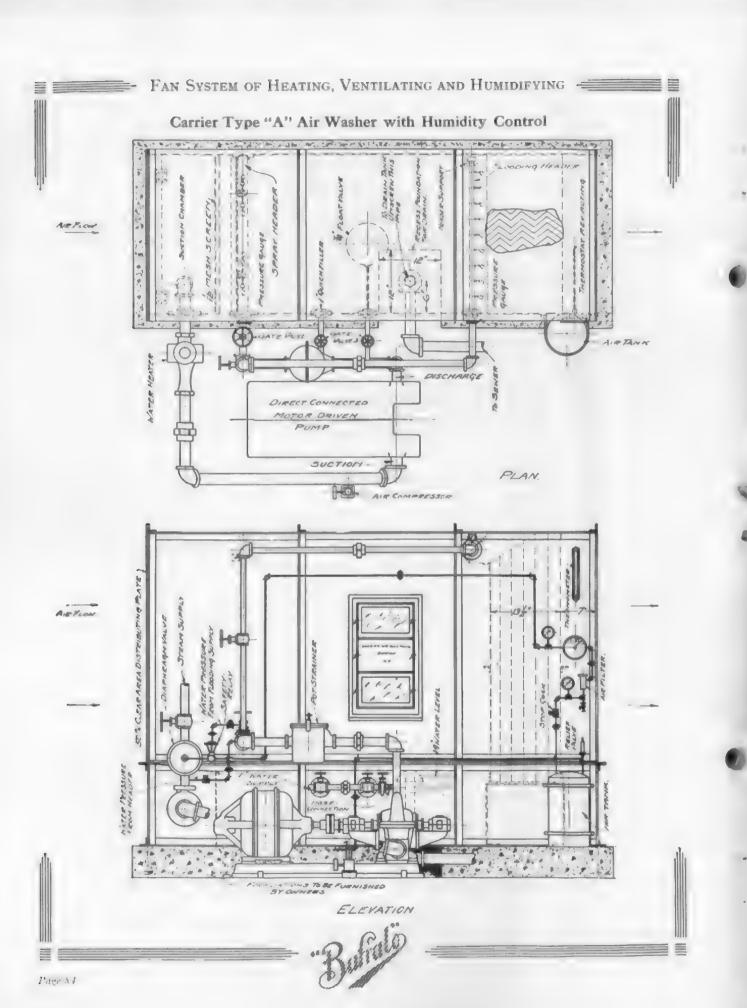
FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

Buffall



Page S2

11.12 33



### Carrier Type "A" Air Washer

Dimensions and Capacities

# 4	Feet			Call or r Min			iter Dens		Pu	mp	P.	Stent	n Pipe				Age .	
Square Feet Prec. Area	Square Feet Washing Surfa	Sign Dear	Sprns	Гонепп	Both	To Pump	Fresh	J.	R P M	Brake	Size Motor	0 Pounds	5 Pounds	Height	Width	Length	Cubic Feet Air	Number
2 95 to 23 to 50	25 6 101 5 92 5		9 18 27	.5 10 15	14 28 42	11,2	3.4 	1,2	1700	1.2 1.5	*3 & b.1	1 1 2 2 2	1 t a 1 t /_		$\begin{array}{c} 1' - 5 \stackrel{!}{\downarrow}_{b} \\ 2' - \eta' \stackrel{!}{\downarrow}_{b} \\ \stackrel{!}{\downarrow}' - 0^{2} \stackrel{!}{\downarrow} \end{array}$		1500 3100 4800	1. 2. 3
12 8 16 0 19 3 22 6	121 135 187 219	532 x 26*	36 15 54 63	20 25 31 36	56 70 85 up	3	**	*** *** ***	**	1.8 2.1 2.1 2.7	3	21, 3	21,2	(-11/3"	$5' - 41_2 - 6' - 87$ $7' - 11^3 - 8$ $9' - 31_3$	- 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1	6400 8000 9700 11300	4. 5 6 7.
25 9 20 1 32 4 35 7	251 282 316 316	15	72 51 90 99	41 46 52 57	113 127 142 156	::	1"	212	* * * * * *	3 (1 3 3 3 6 3 9	(1)	31.9	3		$10' - 71_{\frac{1}{4}}$ $11' - 11'$ $13' - 21_{\frac{1}{4}}$ $114' - 61_{\frac{1}{4}}$	1	1,000 1,000 1,000 1,000 17800	9 10 11
4 13 8 71 13 3	39 2 \$15 129	-	11 22 33	5 10 15	16 32 48	2*	A 6	112	1700	1 0 1 3 1 6	2.	$\begin{smallmatrix} 1^1_4\\ \frac{2}{n} \end{smallmatrix}$	1 1 1 2		$\begin{array}{c} 1' = 5^{\frac{1}{4}} \\ 2' = 9^{\frac{1}{4}} \\ 1' = 0^{\frac{1}{4}} \end{array}$		2100 1400 6700	1 2 3
17 9 22 5 27 1	174 218 263	10 Table 10 10 10 10 10 10 10 10 10 10 10 10 10	43 54 65	20 25 31	63 79 96	212	**	(*)	14	1.9 2.3 2.6	3	2 <sup>1</sup> 2 3	3	* P	5'—43 <sub>2</sub> 6'—8' 7' 11 <sup>2</sup> 4	2 P C -	96000 1 1 3000 1 36000	5 6
31.7 36.2 40.5	351	50	76 57 97	36 11 46	112 128 143		1"	2],	**	3 0 3 3 6		312	319	70	97 31 1 107 -71 1 117 117	î-	15500 18400 20400 23700	7 8 9 10
50 0 54 6	140 185 530		119 130	6 <u>9</u> 57 62	176 176 192	**		**	**	4.4 4.7	734	1 4	4		13'-2t <sub>2</sub> 11' 6' <sub>1</sub> 15' 10'		27.000 27.000	11
6 40 13.7 20.9	62 0 193 203		18 36 54	.5 10 15	23 46 69	112	å	11/2 0	1700	$\begin{array}{c} 1.1 \\ 1.6 \\ 2.1 \end{array}$	2 3	$\frac{11_{2}}{2}$ $\frac{2}{21_{9}}$	$\frac{1}{2}^{1}$ $\frac{2}{2}^{1}$		1' 51 <sub>4</sub> 2' 4" 1' 03 <sub>4</sub>		3,200 6200 10500	1 2 3
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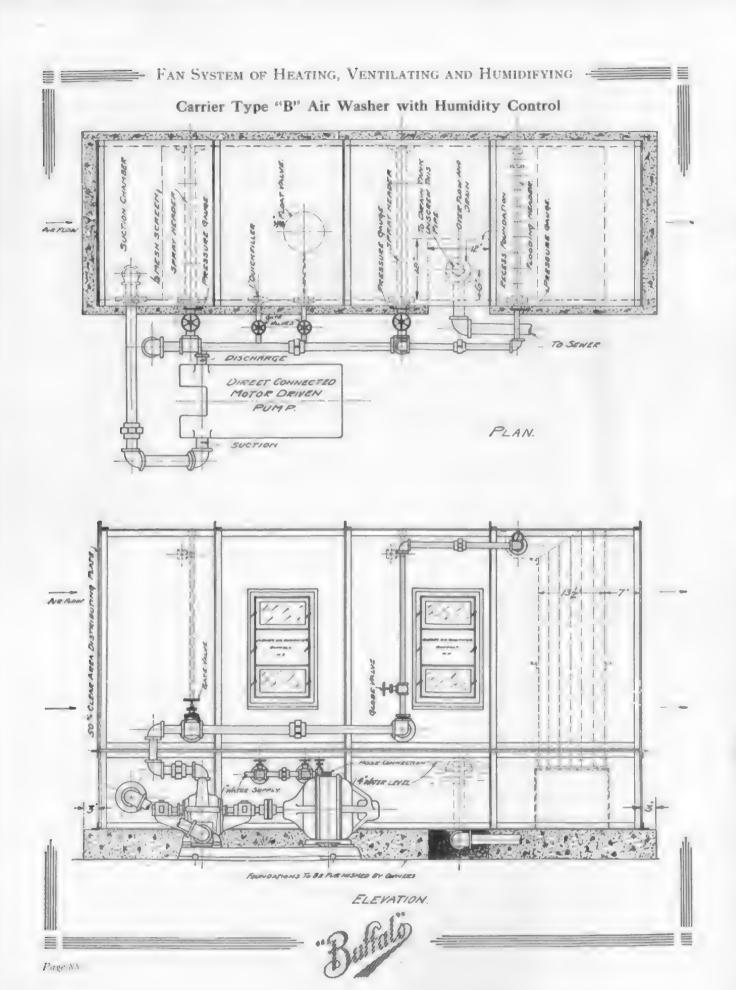
## Carrier Type "A" Air Washer

							Dime	ension	and (	apaciti	N. M.							
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### Carrier Type "A" Air Washer

Dimensions and Capacities

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September 1 or 1	Naching Sud	Size Deve	water	Fleeding	35000	To Pump	I Bereils	.) 12 ° 7.	K. P. M.	Brake	T. Sarra Morton J.	0 Pounds	* Pouttuls	Henglet	M r-ltb	Length	Cale Clery A	Num le :
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122 140 157	LISO Litat Liga		297.1 132 373	.50, E 1 E 1,	326 374 119	**			1120	7.5 8.3 9.0	161	7	7		9' 11', 10' 5', 12' 0'		GICENO TORKOS TORKOS	70
175 343 211	1700 1870 2000	N (36)*	\$1.1 \$50 \$547	52 57 62	166 111 159		**	 3	**	9.8 10.6 11.3	15	8	:: 8	0.00	13' 3'. 14' 7' <sub>4</sub> 15' 11	* ***** ****	55(101) 97(401) [116668]	100 110 120
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### Carrier Type "B" Air Washer

Dimensions and Capacities

es t	Feet	<b>1</b> 2 ( )		inllon r Mim		V n Pij			Pu	пр Н.	P.	Steam	n Pipe	es/		_	t Air	- Bar
Number Ford	News Feet Washing Surface	2004 J ->21%	No.	Floorling	Beth	To Pump	Fresh	Nozer	R. P. M.	Brake	Sire Motor	0 Pounds	5 Pounds	Heagh	Width	Length	Cuble Fort Air	Number
2 95 6 2 1 9 50 12 8 16 0 19 3 22 6 25 9 29 9 29.1 32.4 35 7	28 6 400 5 692 5 124 155 187 219 251 282 315 346	151, 296	18 36 51 72 90 108 126 111 162 180 198	5 10 15 20 25 31 26 41 46 52 57	23 46 49 42 115 189 162 185 248 248 245	1 1 y 2 2 3	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		1700 	1 1 1 6 2.1 2 6 3 0 3 0 4 1 4 5 5.1 5 6 5 8	3 5 71/2	1 112 2 2 2 3 3	1 1 1 4 1 1 7 2 2 2 2 1 2 	20 mm	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	<sup>d</sup> (1)−√19	1500 3500 4500 6400 8600 9700 1300 1300 1500 1500 17500	12 32 32 57 6. 77 8 9
1 13 8.71 13.3 17.0 22.5 27.1 31.7 30.2 40.8 45.4 5000 54.6	39, 2 84 5 129 174 248 263 .08 .651 .566 140 185 380	10 mm mm m m m m m m m m m m m m m m m m	92 44 66 86 108 130 152 174 194 216 268 260	$\begin{array}{c} 5 \\ 10 \\ 15 \\ 20 \\ 25 \\ 31 \\ 36 \\ 46 \\ 52 \\ 57 \\ 62 \\ \end{array}$	27 51 81 106 133 161 188 216 216 216 226 226 322	113 2 2 3 3 3 3 4 4 4 4 4 4 4 4 4 4 4 4 4	1   	152 2 219 3	1700	1.2 1.7 2.3 2.9 3.4 4.0 4.6 5.2 5.7 6.3 6.9 7.4	5 5 71 <sub>2</sub> 10	214 214 313 313	1 1 1 2 2 2 2 3  3 1 2 	D grade on the state of the sta	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	11, -01 <sub>N</sub>	2100 4400 6700 9880 13900 15900 15900 20400 22700 25000 27300	11 21 31 41 51 61 71 81 91 101 111 121
6 40 13.7 20.9 28.5 35.3 42.5 56.9 64.1 771.3 57.8 5.5 7 90.0 107 114 122 129 144 156 144 156 144 158	162 0 1831 293 273 34 1 143 453 553 623 623 693 7733 852 970 1040 1150 1250 1320 1320 1420 1420 1420	14°x386°	36 72 108 1119 216 2524 326 327 327 328 330 332 478 501 516 517 612 612 612 612 612 612 612 612 612 612	5 10 15 20 25 31 36 11 46 52 57 62 67 78 83 99 103 104 114 120	11 \$2 123 164 247 247 247 248 329 370 412 153 153 154 577 615 659 741 753 854 855 856 856 856 857 857 857 857 857 857 857 857	2 2 3 3 4 5 5 6 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	1.4         	11 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	1700	1532 4.109 772 8.602 11.62 9.607 11.62 13.07 14.7 15.7 16.7	2 3 5 7 10 10 15 0 0 0 0 0 0	1 1 2 2 3 3 1 3 3 1 3 3 1 3 4 1 4 1 4 1 4 1 4 1	124 219 319 319 412 412 412 412 413 614 114 115 115 115 115 115 115 115 115 1	7.41%	1'-51 <sub>4</sub> 2'-9" 1'-02 <sub>4</sub> 5'-41 <sub>2</sub> 6'-8" 7'-113 9'-31 <sub>2</sub> 10'-71 11'-11 13'-21 <sub>2</sub> 14'-61 <sub>2</sub> 15'-10 15'-12 15'-12 21'-17 22'-41 <sub>2</sub> 23'-81 <sub>4</sub> 21'-17 25'-0" 25'-0" 25'-0" 28'-11' 2	9°-433,	3.200 6200 10700 14100 21300 21300 22300 22400 25400 45500 45500 57000 55000 57000 55000 72500 72500 72500 72500 72500 72500 72500 72500	10 20 33 44 55 66 90 10 11 12 13 14 15 16 17 18 19 20 21 21 22 23

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# Carrier Type "B" Air Washer Dimensions and Capacities

							Dim	ension	s and	Сарисі	lien							
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5 3	Feet	Direct	1 "		1111		1 = -			H	1					_	17.5	ķ.
Square Feet Free An a	Square Feet Wasking Surfa	Slac D.	Spray	Flooding	Both	To Pump	Freely	271%	RPM	Brake	Sign Mater	H Posttel.	5 Pour de	Height	Width	LAURI	Carenty College A	/ under
\$7.5 +20 × 64 2 184 845 6777 6717 1277 1278 1566 9 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	56 0 1×1 276 373 468 568 754 ×17 930 1040 1140 1140 1150 1610 1710 1800 1900 1900	16" x 36"	48 94 110 158 244 240 325 321 420 468 506 508 156 704 750 790 841 984 1020	1 5 10 15 25 1 25 25 25 25 25 25 25 25 25 25 25 25 25	53   101   156   208   350   311   364   446   520   573   624   675   729   861   881   967   989   1040   1048   1134	983	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	11 y 2 2 1 y 3 1		\$ 2 9.0 9.8 10.7 11.5 12.3 13.1 13.9 14.6 15.3 15.9 16.0 17.3 18.7 19.3	3 5 2 10  15  20  20 	214 312 419 000 000 000 000 000 000 000 000 000 0	14g 21g 3 4 4 5 6  7 	9-13-6	11' 5/4 2' 05' 4' 05' 4' 05' 4' 05' 4' 05' 4' 11' 2 05' 7' 113' 4' 61' 3 16' 71' 11' 11' 11' 11' 11' 11' 11' 11' 11	$\Omega^{r} = (0)^{T_{\frac{1}{N}}}$	1109 9164 11290 24300 24300 25000 35000 35000 35000 35000 35000 88000 98000 163000 163000 163000	1D 2D 3D 5D 6D 7D 8D 9D 10D 12D 14D 15D 15D 15D 15D 20D 20D 22D
11 2 3 6 1 4 8 6 6 1 4 8 6 6 1 4 8 6 7 1 4 8 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 9 2 1 4 9 8 2 1 4 9 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 8 2 1 4 9 2 1 4 9 8 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 9 2 1 4 1 4 9 2 1 4 1 4 1 4 1 1 1 1 1 1 1 1 1 1 1 1 1	2180 100 229 350 472 702 712 833 953 1070 1190 1130 1130 1150 1850 1850 1800 2100 2100 2100 2250 2400 2570	10° x 36°	1076 58 116 117 250 255 116 157 157 157 157 157 157 157 157 157 157	120 5 10 15 20 25 31 46 46 57 62 62 78 78 78 78 111 109 111 120	1106 123 125 189 250 313 377 440 501 864 628 691 754 817 8817 8817 1907 1908 1129 1193 1256 1319 1319 1446	\$ 15 10 10 10 10 10 10 10 10 10 10 10 10 10	2 2 3 4 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	11 y 21 y 3 4 4	17(h)  45  100  12(1)     60  14  17  17  18  18  18  18  18  18  18  18	1 9 3.3 4 6 5.0 7 2 2 8 4 9 1 1 1 1 1 1 1 2 3 1 1 3 1 1 5.2 2 1 5 9 1 1 7 6 1 2 2 2 2 2 2 2 2 2 3 1 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	55 5 71 2 10 0 0 15 10 0 0 0 0 0 0 0 0 0 0 0 0 0	3 3 1 2 4 4 4 5 2 5 5 5 5 5 5 5 5 5 5 5 5 5 5	2 2 2 3 3 3 4 4 1 <sub>2</sub>         	11134	16' 2' 11'4 2' 11'4 3' 11'4 3' 11'4 3' 11'4 3' 11'4 11'5 3' 11'4 11'5 11'5 11'5 11'5 11'5 11'5 11'	; (15 ° )	11.50.00	21D 1E2 2E2 3E3 4E3 5E3 5E3 6E3 11E1 12E1 13E1 13E1 13E1 13E2 14E2 13E2 14E2 14E2 14E2 14E2 14E2 14E2 14E2 14

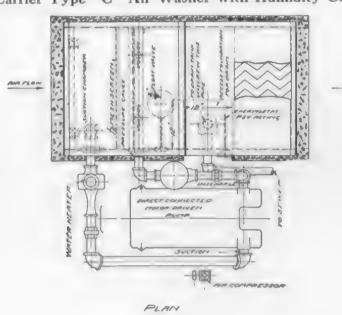
### Carrier Type "B" Air Washer

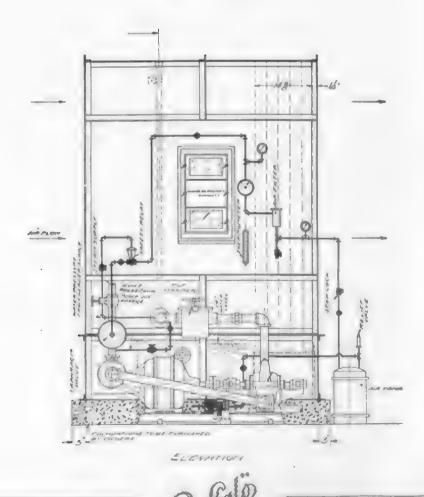
Dimensions and Capacitles

				(miles	15	14:	return.		Į.	nii)i								
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Square best Free Area	Square Peet Washing Surfine	Tire These	Spray	Heeling	Best	To Pump	Fresh	is it.	R. P. M.	Brake	Size Motor	0 Pennels	5 Posses	Height	Wilth	Length	Cups itv Cub. Lect A per Mante	Number
14.5 25.6 1.7	131 278 121		72 144 216	5 10 15	77 154 231	21. 3.	3 4 11	21 <sub>2</sub>	1700	2 2 3 9 5 1	3 71 <sub>2</sub>	3	2 3 3 <sup>1</sup> 3		1' 55 <sub>4</sub> 2' 96 1' 1' <sub>4</sub>		15300 2 0000	1 F 2 F 3 F
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Esh 1 1 3 % 1 - 5 %	[ cr[ 1 ) [ [ r.d 4 ] [ lole )	Ы	571 648	34+ 4.1 64+	540 617 694	¢,	4.7	 	**	[   1) [2 2 [3 4	**	7	6		91 - 11 101 - 72 111 - 111 2		62.800 68.800 67.000	7F 541
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144 B 2 94 172 B	1880 2130 2175	165	1008 1008 1080	73	1003 1081 1138	4.0 4.0 4.0	6.6		**	17.5 18.5 19.6	25		*	1:37	17' 21 <sub>4</sub> 18' = 6" 19' = 91,	ેંદ્ર	97000 105 900 112 900	13F 14F 15E
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2504 33.4 324 33.4	25000 3000 41500 4310		1440 1542 1584 1656	104 109 114 120	1544 1624 1698 1776	10"	11		**	26 1 27 4 25 7 30 0	557 57	41	**		$\frac{2n' - 4^{+}}{27' - 8'}$ $\frac{27' - 8'}{28' - 11^{+}}$ $\frac{30' - 3^{+}}{3}$		15000 15700 16200 17200	201F 21F 22F 23F
15 % 33 % 51 .1	151 026 198		\$1 166 270		891 176 265	21,	1 114	21,	17(10)	2 5 4 4 6 3	3 5 71,	21.2 31.1	$\frac{2}{3}$	ī	$\begin{bmatrix} 1' & 6^{\frac{1}{4}} \\ 2'' & 10'' \\ 1' & 1^{\frac{1}{4}} \end{bmatrix}$		\$109 16800 25700	HCa 20 a 20 a
621 G 54, 7 101	670 842 1010		332 111 195	250 25 31	352 439 539	5	1	, &  	1120	5 0 9 1 10 5	10 15	11 <sub>2</sub> 5	41.		57 51 <sub>2</sub> 67 97 81 02 <sub>3</sub>		24500 13400 52000	5G 5G
127	1180 1000 1520		380 1986 746	36 11 16	616 707 702		44	**		12 2 13 6 14 8	20	7	7		9' 11' 10' 5' 12' 0'		TORENT TORENT THERE	70 80 90
175 193 211	1700 1870 2050	4 354	%2% (41.2 (40.1	100 100 100 100 100	550 969 1056	3	1,14	t <sub>1</sub>	**	15 8 17 1 18 2	44	8	  8	÷ 1	13' 3' 7' 11' 15' -11'	113 x 4	\$5.681 976681 16861001	100. 110. 120.
228 246 263	2210 2390 2309	b 	1078 1100 1211	67 73 75	1245 1243 1322		**	7 · · · · · · · · · · · · · · · · · · ·	**	19.5 20.8 22.3	*) ** *** **	10	**	13/	17' 23' 15' 61' 19' 10' 4	9'-	11 1000 12 1000 13 2000	13G
251 248 316 331	2730 2890 3070 3240		1.026 1.008 1.000 1.57.4	%3 93 98	1309 1396 1583 1673	111	11.7		6.6	23 S 25 3 26 7 28 3	35	# # # # # # # # # # # # # # # # # # #	10		21' - 2" 22' - 51 : 21' - 9 : 1 25' - 1"		141600 140600 158600 167000	160 170 180 190
351 369 388 105	3410 3580 3770 393a		1656 1740 1821 24.6	104 109 114 130	1760 1849 1948 2049		**	11	6.6	29.5 31.3 32.5 34.4	10	12	**		26' 12 <sub>4</sub> 27' 81 20' =0" 30' = 33 <sub>4</sub>		176000 185000 194000 203000	2H - 22H - 2

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

Carrier Type "C" Air Washer with Humidity Control





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FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

### Carrier Type "C" Air Washer

Dimensions and Capacities

t a	100	P <sub>a</sub>	W: Pu	sterr pers		131	mp H.	Р.	Steat	n Pipe			!	Y.   Air nte	
Square Feet Free Area	Squit Feet Washing Surface	Stre Deer	To Pump	Fresh	Size	R. P. M.	sealer the	Size Mortor	0 Pounds	5 Pounds	Heigh	Width	Length	Capacity Calar Pert Ali per Minute	rafain.
3 34 7 05 10 8 14 5 18 2 21 9 25 6 29 3 33.0 36 7 40 5	11 0 23 0 35 2 47 2 59 4 71.4 83 1 95 1 107 6 119 6 132 0	4.5.00 d. 5.00	11 <sub>2</sub> 2 21 <sub>2</sub> 3	2 0 0 0 0 0 0 0	1 to 2 to	17(k)	.775 .95 1 15 1 35 1.55 1.72 1 92 2 10 2 30 2 50 2.70	3 3	1 1 2 2 2 2 3 2 3 3 1 3 3 1 2 3 3 1 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3 3 1 3	17 113 212 212 31 312	i'-!12*	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	4.—10.	1760 3500 5600 7600 9 100 11(400 12500 14600 16500 9 500 20200	1 22 3 4 5 6 7 8 9 10
4 52 9 54 14 5 19 6 24.6 24.6 33 6 39 6 44 6 50 6	14.8 31.0 47.2 63.8 80.0 90.4 112.8 129.0 145.2 162.0 178.0 194.0	1512 x 280	11.2 2 2 2 2.2 2.2 2.2 2.3	5 4 · · · · · · · · · · · · · · · · · ·	11 <sub>2</sub>		\$0 1.05 1.30 1.72 1.97 2.13 2.65 2.90 3.13 3.35	3	$\begin{array}{c} 1^{1}_{\delta} \\ 2^{1}_{2} \\ 2^{1}_{2} \\ \vdots \\ 3^{1}_{2} \\ \vdots \\ 1^{1}_{2} \end{array}$	11 <sub>4</sub> 11 <sub>2</sub> 2 21 <sub>2</sub> 3 31 <sub>2</sub> 4	5'-1,13"	1' - 514 2' - 6' 4' - 036 8' - 842 6' - 8' 7, -113 9' - 312 10' - 715 11' - 11 13' - 219 14' - 615 15' - 10'	4/ -10*	2300 4800 7300 9860 12300 1300 17300 19800 22300 24800 27300 29800	11 23 31 41 51 61 71 51 10 11 12
6 88 14.5 22 1 29 8 37 1 45.1 52.7 60 6 68.0 75.5 8.3 2 91 0 98 3 100 114 121 130 144 152 152 166 175	22 4 47 2 72 72 97 2 122 147 172 197 222 246 272 296 320 346 346 346 346 444 470 462 444 470 462 444 470 462 463 464 470 462 463 464 470 462 463 464 470 462 463 464 470 462 463 464 464 465 464 464 465 464 464 465 464 464	18" x 385"	11-2 22-7 3	1 4 6 00 00 00 00 00 00 00 00 00 00 00 00 0	1 by	1700	95 1 35 1 72 2 10 2 50 2 87 3 05 4 05 4 43 5 20 5 57 6 35 6 73 7 50 7 50 7 50 7 8 95 8 95	2 3 5         	11 <sub>2</sub> 21 <sub>2</sub> 31 <sub>3</sub> 31 <sub>2</sub> 5 6	11/2 21/3 3 31/2 6 41/2 5 6 6 6 7	, z, -1, -, t	17-514 27-97 47-034 55-41, 67-87 77-1144 97-31, 107-714 117-114 137-21, 117-114 157-107 177-124 157-107 177-124 157-107 217-17 227-115 237-814 257-07 267-374 277-712 287-244	1, 10,	3400 7300 11000 13000 18700 25500 26500 30700 30700 44500 44500 44500 44500 60500 60500 72800 72800 72800 72800 800000 800000 800000 800000 800000 800000 800000 800000 8000000	10 20 30 40 50 50 80 90 100 120 130 150 150 150 20 20 22 23

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### Carrier Type "C" Air Washer

Dimensions and Capacities

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) see	and Algeor	d <sub>a</sub>		iter jus		1.	unup H	P.	7m(11,12)	ь Рин					
Equate Feet From Viva	Square Feet Western Feetler	Stee Do it	To Pump	Fresh	E. dep	R. P. M.	Farm No.	Sire Motor	O Pentoda	wheelight of	Hright	Weith	Length	Cula Lost Vi	Nutribar.
9 24 19 5 40, 59 3 69 6 70 8 81 0 91 3 101 112 132 142 142 143 154 194 204 225 225	30 2 63 6 97 2 130 4 163 163 264 264 368 430 166 368 430 560 562 662 663 664 668 734 734	Dr. v.367	1 1 2 2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3	/:. :: :: :: :: :: :: ::	11/2 21/2 31/2 31/3 41/3 31/3 31/3 31/3 31/3 31/3 31/3	1700	1.10 1.57 2.57 3.57 4.57 4.57 5.57 6.57 7.67 7.57 8.30 9.10 9.45 9.45 9.50 10.50	2 3 3 5 7 1 7 1 10 	2 2 2 3 3 4 4 4 7 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	11 2 1 2 1 2 1 2 1 2 1 2 1 2 1 2 1 2 1	9112	1' 51' 2' 91' 1' 02' 1' 02' 1' 02' 1' 7' 11' 9' 3' 1' 7' 11' 13' 2' 11' 12' 15' 10' 17' 15' 21' 1' 22' 1' 22' 1' 22' 3' 22' 3' 22' 7' 28' 11' 28' 11' 28' 11' 28' 11' 28' 11' 28' 11' 28' 11' 28' 11' 28' 11' 28' 11' 28' 11' 28' 11' 28' 11' 28' 11' 28' 11' 28' 21' 28' 11'	4'-10*	10000 100001 100001 200001 200001 200001 300000 5000000	1D
11 6 21 5 30 3 63 1 75 80 102 115 127 140 153 166 179 284 247 247 247 247 248 256 268 268	37 8 50 122 164 296 248 290 382 376 414 456 500 540 584 694 706 706 707 702 86 871 993 993 994 995 995 995 995 995 995 995	10" x 3H.	1 1 2 2 2 2 1 3 3 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	**************************************	11.7 2 21.9  3 4  	1700	1 20 1 52 2 40 2 40 3 65 4 27 5 50 6 72 5 50 6 72 7 7 8 80 9 70 10 20 11 10 11 10 11 20 11 12 90	2 3 3  71.y  10   	23 31 y 4 1 2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	2 21 <sub>2</sub> 3 31 <sub>2</sub> 4 41 <sub>2</sub> 5 	11'-135"	17 514 27 917 17 114 57 57 67 81; 87 61; 97 17 107 714 117 117; 137 37 147 614 157 101; 177 214 187 63 217 11; 227 57 237 831 257 61; 267 11;	4.—10.	5-800 12-300 18-700 26-200 31-600 31-600 31-600 31-600 31-600 4-5000 6-5000 6-5000 6-5000 10-6000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000 11-5000	1E. 2E. 3E. 4F. 5E. 5E. 5E. 5E. 5E. 5E. 5E. 5E. 5E. 5E

### Carrier Type "C" Air Washer

Dimensions and Capacities

\$ 10 m	Surface	7:1		iter ; en	H		H.	£>.	Street	n Pijer	-	-		S THE	
Free loss	National Washing	Sire Don	To Bant	Fresh	Size	R. P. M.	Brake	Size Metor	o Pounds	5 Pounds	Height	Wichbi	15 15 15 15 15 15 15 15 15 15 15 15 15 1	Cuba Lot M per Minate	,
14. 29.5 15. 70. 5 16. 70. 5 16. 167 122 138 140 151 154 160 216 232 246 262 278 388 321 340 356	45.6 96 146 198 248 298 150 520 520 506 606 652 754 756 854 908 1604 1606 1408	165" x 566"	11 2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3		1 *2 2 2 19 3 3 4 4 5 5	1700	1 35 2 12 2 90 3 67 4 42 5 20 7 47 8 10 9 20 9 20 10 95 11 50 12 70 12 70 13 75 14 25 15 25	2 3 5  71,2  10        	2 3 3 3 4 4 4 5 6  8  8  9	2 3 3 <sup>1</sup> x 4 <sup>1</sup> y 5  6     	13'-12'	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	4′ _10°	70000 115201 22,7501 35,0001 45,500 53500 67000 77000 55000 0 1000 110000 110000 110000 125000 125000 125000 125000 125000 125000 125000 175000 175000	3 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
16.4 34.5 52.6 70.7 89 107 125 144 162 180 198 201 214 257 214 257 268 268 270 288 268 270 270 270 270 270 270 270 270	53 4 142 172 230 280 180 180 405 470 528 586 646 700 764 8 20 880 940 1090 1090 1120 1180 1180 1 140	Section X Section	2 21 3 3 4  5       		21.7 3.3 4.5 	1700	1.47 2.35 3.25 5.00 5.90 6.30 8.30 8.95 8.96 10.25 10.45 11.450 12.25 12.20 14.70 14.70 15.25 15.70 16.25	2 3 5  744  10  15        	21 9 31 9 4 4 12 5 6  7  10 	2 3 3 1 2 4 5 5 6 6 7 S S	$\begin{bmatrix} z' - z \\ 0 \end{bmatrix}$	17 604 27 107 47 134 57 512 67 97 87 014 127 814 127 234 137 234 137 234 137 234 137 234 137 234 137 234 137 234 137 234 137 317 137 3	1,-10,	\$200) 17 (00) 12 (00) 26 (00) (510) 14 (50) (52 (00) (52 (00) (52 (00) (50	

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### Sizes and Dimensions of Buffalo Standard Heaters

Number of Pipes	Langth of Section	Section Number	Extreme Height of Section	Width of Section	Lanear Feet of 1° Pipe per Section	Total Fifective Square Feet of Henting Surface	Impair Feet of 1' Pipe per Section	Clear Area for Air Passage Sq. Ft.	Weight Pounds
56	3' 4 Row	1.A 2A 3.A 4A 5.A 6A	3'-4" 3'-10" 4'-4" 4'-10" 5'-4" 5'-10"	812"	140 168 196 224 252 280	54.7 64.2 74.0 83.7 93.3 102.5	159 186 215 243 271 298	4.4 5.2 6.0 6 × 7.6 8.4	473 515 565 616 656 708
72	4' 4 Row	1B 2B 3B 4B	5'-4" 5'-10" 6'-4" 6'-10"	812"	320 356 392 428	119.0 131.5 143.9 156.5	346 382 418 455	9.7 10.7 11.2 12.6	819 877 938 1003
80	4'-6" 4 Row	1C 2C 3C 4C	5'-10" 6'-1" 6'-10" 7'-4"	812"	396 436 476 516	148.2 162.0 174.8 188.6	431 480 507 548	12.1 13.1 14.2 15.3	997 1955 1127 1174
88	5' 4 Row	1D 2D 3D 4D	6'-4" 6'-10" 7'-4" 7'-10"	812"	476 520 564 608	174.3 189.3 204.8 219.8	507 550 595 638	14.1 15.4 16.6 17.7	1182 1262 1325 1407
104	6' 4 Row	1E 2E 3E 4E	7'-4" 7'-10" 8'-4" 8'-10"	812"	674 726 778 830	245.0 262.9 280 8 298.7	712 763 816 868	19.8 21.3 22.7 24.2	1505 1600 1695 1770
128	7' 4 Row	1G 2G 3G 4G 5G 6G	7'-4" 7'-10" 8'-4" 8'-10" 9'-4" 9'-10"	812*	796 860 924 988 1052 1116	291.0 313.2 335.2 357.2 379.2 401.2	\$45 910 974 1037 1101 1163	23.6 25.4 27.2 29.0 30.7 32.5	1845 1950 2055 2160 2280 2380

All Buffalo Standard Heaters are regularly furnished in the return bend pattern. The open area pattern is furnished on special order only.

Note—All heaters furnished in return bend pattern unless otherwise specified.

### Friction of Air Through Buffalo Heaters

Air Measured at 70°F. and 29.92" Barometer.

Loss of Air Pressure in Inches of Water per Square Inch.

Velocity Through				Number	of Sections			
Clear Area	1	2	/ 3	4	5	6	7	8
23(30)	0.009	0.017	0.026	0.035	0.043	0.052	0.060	0.069
400	0.015	0.031	0.046	0.062	0:077	0.092	0.108	0.123
500	0.024	0.049	0.073	0.095	0.104	0.144	0.168	0.191
6300	0.035	0.069	0.104	0.138	0.173	0.207	0.242	0.276
700	0.047	0.094	0.141	0.188	0.235	0.282	0.329	0.376
800	0.061	0.123	0.184	0.245	0.306	0.368	0.429	0.490
1900	0.078	0.155	0.233	0.311	0.388	0.466	0.514	0.621
1000	0.096	0.191	0.287	0.382	0.479	0.574	0.670	0.765
1100	0.116	0.232	0.347	0.463	0.579	0.695	0.810	0.920
1200	0.138	0.276	0.414	0.551	0.689	0.827	0.965	1.10
13000	0.162	0.324	0.486	0.648	0.810	0.972	1.433	1.290
1400	0.187	0.375	0.562	0.750	0.936	1.124	1.311	1.500
1500	0.215	0.431	0.646	0.861	1.077	1.293	1.508	1.723
1600	0.245	0.490	0.735	0.980	1.226	1.471	1.716	1.96
1700	0.277	0.555	0.831	1.110	1.387	1.664	1.940	2.213
1800	0.310	0.620	0.930	1.240	1.550	1.860	2.167	2.48

Buffala

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

### Final Temperatures and Condensations

Buffalo Standard Heater

0 LBS.

0 lbs. Steam Pressure 212.0° F

Velocity of Air in Feet per Minute — Measured at 76" F, and 29 92" Barometer

ite of	ed tendid		Fe(10)	240	(c)	10	000	12	()r)	11	DO DO	166	(31.)	154	(30.)
Temperature of	Namber of Heater Sections	Final Temperature	Conferential jet lineal Frot per Hoar	F. T.	C.	FТ	(-	F. T	C.	F. T.	C.	F. T.	(*	F T	C
50.5 - 4k	1 22 3 4 5 6 7 5	46 69 58 105 120 133 143 152	Pounds 187 459 129 100 375 351 330 340	44 05 83 99 113 125 136 145	900 502 525 194 465 438 413 390	42 61 79 94 107 119 129 139	687 640 614 572 544 515 486	40 59 75 90 102 113 124 133	752 700 685 656 646 583 555 531	39 56 72 86 98 100 119 128	786 786 756 756 756 758 684 684 685 768 768	38 54 68 82 94 104 114 123	.901 849 797 776 742 701 645	37 52 65 78 90 101 110 119	2 2 2 1 1 1 1 1 1 2 2 2 2 2 2 3 3 3 4 5 1 4 1 4 1 4 2 2 2 2 2 2 2 2 2 2 2 2 2 2
mo,	1 2 3 4 5 6 7 %	55 77 95 111 125 137 147 155	\$109 \$40 \$106 \$380 \$357 \$334 \$13 \$293	52 72 90 105 118 130 140 149	550 525 500 460 440 417 392 372	51 69 86 100 112 123 133 142	656 501 583 540 513 484 459 438	49 66 82 96 108 148 128 136	714 674 650 620 586 550 525 389	18 65 79 92 104 114 123 132	.788 .765 .715 .680 .650 .613 .581 .558	47 62 76 88 99 109 119 127	\$51 799 718 726 192 (50 (45)	16 60 73 85 96 106 115 123	
1()°	2345	64 84 102 116 120 140 150 158	150 112 357 356 334 312 294 276	61 80 96 140 123 134 144 152	525 500 466 435 415 392 371 350	60 78 93 105 118 128 138 146	625 593 551 510 488 437 414	58 74 89 102 114 123 132 141	676 -636 -612 -582 -565 -519 -492 -475	57 73 87 99 110 119 125 136	.715 .721 .685 .646 .615 .576 .550	56 70 83 95 105 115 124 132	.801 .749 .715 .689 652 626 600 573	55 68 81 92 103 112 120 128	. 10
\$U°	1 2 3 4 5 6 7 8	72 91 108 122 134 145 154 162	412 354 362 335 316 297 278 262	70 88 104 116 128 139 148 156	500 175 150 113 391 371 349 ,331	69 86 99 112 123 133 142 150	594 546 510 479 457 432 410 391	67 82 96 108 119 129 137 145	638 590 575 545 519 494 466 447	68 80 93 105 115 124 132 140	700 655 .627 .603 .570 .540 .513 .492	65 78 91 102 112 121 120 136	751 689 652 652 692 594 594 598	64 76 85 99 109 117 125 132	. 0
rwyo	1 2 3 4 5 6 7 8	S1 99 114 128 139 149 157 165	389 303 349 346 297 278 289 245	79 95 110 122 133 143 151 150	.474 138 415 388 366 346 325 300	77 93 106 118 129 138 146 153	.531 .515 479 449 482 406 384 364	76 91 103 114 124 133 141 149	580 580 588 508 481 458 481	75 89 100 111 121 130 137 144	.656 .634 .585 .539 .534 .510 482 462	74 87 98 109 118 127 135 141	.701 674 632 614 582 560 545 546	73 85 96 106 115 123 130 136	
711.	1 22 3 4 5 11 27 8	90 106 120 133 144 153 161 168	375 .837 312 296 278 259 243 240	88 103 116 128 139 148 155 162	150 112 383 393 345 325 393 287	86 100 113 124 134 143 150 157	500 468 447 117 ,400 386 366	85 98 110 120 130 138 146 153	502 525 500 469 451 425 407 380	\$1 901 108 117 126 134 142 148	,613 ,569 ,554 ,515 ,191 ,166 ,450 ,426	53 95 105 115 124 132 139	651 624 582 564 541 518 192 463	82 104 113 121 129 185 139	

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### Final Temperatures and Condensations

Buffalo Standard Heater

5 Lbs.

			5 Ibn. S	iteam Pr	essare						227.0	F			2500.
				Velocit	of Air	n Fret j	er Minn	170-	110 00 110	1 st 70	Fatel 2	1927 B.	let estat		
# # # # # # # # # # # # # # # # # # #	r of		1,630,3	51	*()	10	H m )	1.	? H1	1	[es 1	1 (	a 3" }	1 '	MINI
Terriperature of	Number of Heater Sections	Final	Condensation     er     iner	F. T.	C.	F. T.	(°	F. T.	('	F. T	C.	F. T.	C.	F. T.	(,
F 211	A de la Company	48 73 94 112 127 141 152 162	Founds 537 489 467 434 407 381 358 337	46 68 88 105 120 133 144 155	652 610 573 ,536 505 ,476 ,119 ,425	44 64 83 99 113 126 137 117	759 620 661 625 589 568 526 502	42 62 79 91 108 121 131 141	\$35 .795 .745 .702 667 637 600 .573	40 59 75 90 103 145 126 135	907 862 812 .774 737 .702 .668 .635	39 57 72 100 111 121 131	961 .935 875 847 840 766 .726 700	38 34 69 83 95 107 117 126	1.023 966 926 895 885 885 823 786 752
30'	The special sections of the section	57 50 100 117 132 115 156 165	.512 475 441 412 357 363 340 319	55 76 94 110 124 137 147 157	632 581 539 506 476 450 421 400	52 72 89 104 115 130 141 150	728 66 1 .620 .587 .556 .526 .500 .473	51 69 86 100 113 125 135 144	.796 .739 .706 .665 .631 .600 .568 .539	50 67 83 96 109 120 130 139	,885 ,819 ,780 ,730 ,700 ,664 ,630 ,600	48 65 80 93 105 116 126 135	.910 885 840 .706 .760 .724 691 663	47 63 77 90 102 112 122 131	997 937 889 853 820 776 746 716
41)**	1 2 3 1 5 6 7 8	66 88 106 123 137 149 159 168	.494 455 416 393 368 342 321 303	64 83 100 115 129 111 151 160	506 544 505 174 450 425 400 378	62 80 96 111 124 135 145 154	696 631 589 560 532 ,500 473 450	60 77 92 106 119 130 139 148	.759 .700 (56 (26 (601 569 536 .511	59 75 90 103 115 125 134 143	.840 .775 .735 .696 .664 .626 .593 .508	57 73 57 100 111 121 131 140	\$10 \$41 790 758 719 655 630	56 71 85 97 188 118 127 135	940 880 851 810 775 738 705 673
5m°	1238 6 5 6 7 7 7	74 95 112 129 142 153 163 171	455 427 391 374 349 325 305 286	72 90 107 121 134 145 155 164	506 ,505 ,479 ,450 ,425 ,398 ,378 ,350	70 57 103 117 129 140 119 157	0.33 585 556 529 500 473 145 121	69 85 100 113 124 134 134 134	7.20 66.4 681 568 563 531 500 483	67 83 96 109 120 130 139 147	752 730 ,076 652 620 550 561 ,534	117 117 127 136 144	705 740 705 679 648 619 563	65 79 92 101 114 123 132 140	. \$54 \$24 795 768 730 600 605 .638
ėu <sup>s</sup>	1 2 3 4 5 6 7 8	83 102 119 134 146 157 167 175	4.34 401 .373 .349 .326 .306 .288 .272	\$1 99 114 128 140 151 160 168	530 493 455 431 405 381 361 340	79 95 110 123 145 145 145 162	600 768 5 25 496 473 448 125 403	78 93 107 119 130 140 149 157	1852 625 593 592 596 596 482 460	76 91 104 116 126 136 145 153	710 657 647 .618 557 559 544 512	75 101 113 123 152 140 148	759 753 689 6870 638 606 576 535	71 57 100 120 120 120 137 144	796 767 756 710 684 653 621 595
70"	100000000000000000000000000000000000000	9/1 1909 12/6 14/0 15/1 16/9	398 370 333 331 367 287 267	\$9 105 120 133 144 154 166	506 112 126 198 175 353 353	10.2 110 120 130 130 140 140	5.5% 585 4×4 105 111 -415 -392	50 101 113 125 135 144 152 150	4.400 s 7.40 s 7.40 s 7.22 s 4.47 s 4.47 s 4.47 s	\$5 110 122 131 140 148	.665 625 569 575 540 515 492 474	54 169 129 129 137 147	708 683 620 620 .598	\$3 95 107 117 126 135 142	710 710 700 6/8 680 615 584

Buffalia

Party

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

# Final Temperatures and Condensations Buffalo Standard Heater

ure 218 K- F

20 LBS.

Mile	of Heavy		(11)	41	)( )	10	(0.1	12	00	1	100	10	of M }	1	M#)
Air Enterning	Number of Reater Notes in	Final Temperature	Condensation per Lineal Foot per Hour	F. T.	C.	F. T.	C.	F. T.	c.	F. T.	c.	F. T.	C.	FI.	C.
541 <sub>6</sub>	20 00 on 10 00 00 00 00 00 00 00 00 00 00 00 00	52 80 104 125 143 158 171 183	Pounds 620 584 542 566 478 445 418 504	50 75 97 117 134 149 162 174	.775 .710 .663 .630 .591 .556 .522 496	47 71 92 110 127 141 154 166	873 823 774 726 694 652 617 590	45 68 87 105 120 131 147 158	.970 930 856 821 778 736 701 600	43 65 83 100 115 128 141 152	1 052 1 042 (918 (904 (844 (816 (781 (787	42 62 80 96 110 121 136 146	1 108 1 085 1 661 983 942 866 851 815	\$1 586 76 91 105 115 130 141	1 20 1 13 1 08 1 06 1 06 1 94
3110	1235	60 87 111 131 147 162 174 186	580 552 522 488 455 126 308 378	58 82 104 123 139 153 166 177	724 671 686 605 506 530 530 575	56 78 99 116 132 146 158 169	.840 .776 .742 .694 .661 .625 .589	54 75 94 110 125 138 151 162	933 , 73 , 825 , 775 , 740 , 697 , 668 , 640	53 72 91 107 121 134 145 156	1 040 949 918 870 827 785 .742 .713	51 70 87 102 116 129 140 151	1 081 1 032 982 980 891 853 810 782	50 67 98 112 123 136 145	1.16 1.07 1.02 1.03 9.0 9.1 5.5
£11'	1 2 3 4 5 6 7 8	69 95 117 136 152 166 178 188	.561 .534 .496 .464 .485 .406 .881 .068	90 111 129 144 158 169 180	672 645 610 .579 540 508 475 452	64 56 105 122 137 150 162 173	.775 .744 .699 .662 .630 .593 .561 .534	63 83 100 117 131 144 155 166	.894 .834 .775 .746 708 .672 .635 .610	62 81 98 113 127 139 150	.005 926 \$73 \$25 .701 746 .710 680	60 78 95 109 122 134 145	1 084 981 947 892 850 810 773 748	59 76 91 105 118 130 141 150	1 16 1 04 95 -194 96 -50
50°	3 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	78 102 124 142 157 170 182 192	542 504 477 111 115 387 365 341	75 98 118 135 119 162 174 184	646 620 585 553 514 482 456 432	73 94 112 129 142 155 166 176	.743 .711 .667 .638 .597 .565 .534	72 91 105 123 137 149 160 170	.855 795 749 708 677 640 697 581	70 89 105 119 132 114 154 164	935 581 525 750 745 709 671 645	69 87 102 116 129 140 150 159	.982 955 896 854 818 .776 786 745	68 84 99 112 125 136 146 155	1,600 100 100 100 100 100 100 100 100 100
5 yo	1000 100 100 Per X	87 110 129 147 162 175 186 195	.522 485 .445 .425 .398 .371 .348 .327	84 105 124 140 155 167 178 187	620 582 554 520 193 460 435 410	82 102 119 134 148 160 171 180	711 678 635 597 570 538 511 485	80 99 115 130 143 154 163 174	.778 .756 .710 .679 .615 .607 .580	79 96 111 125 138 149 159	\$60 \$1.5 767 .734 .710 671 647 611	78 95 109 122 135 135 135 156	930 951 844 801 776 733 689 672	77 93 106 135 131 142 151 159	185 186 186 186 176 176 176
Tilo	1 2 2 4 7 7	95 117 139 150 166 178 189	485 ,486 ,425 ,300 ,711 148 149	93 13 131 146 159 171 181	595 525 525 495 495 495 498 5391	91 110 126 141 153 165 175	.679 644 603 573 538 512 483 .460	16m) 1222 1655 1.5% 1.5% 1.6%	739 698 671 630 667 575 575 525	SS 105 139 132 144 154 164 172	\$14 791 .737 .700 673 644 685	\$7 102 116 129 140 151 168	\$75 79.1 763 745 1612 1614	56 101 114 125 137 147 156	965 900 85 81 73 74 71

Buffalo

### Final Temperatures and Condensations

Buffalo Standard Heater

40 LBS.

40 lbs. Steam Pressure	2×6.7 F

				Velocit	y of Air	in Fest	per Min	lite	Mensur	ed at 70	and 193	uz" Bure	timiter		
in of	of Figure	-	Scien	Sil	IO .	10	00	11	(101)	14	(h.)	10	s 101	15	(H3
Terriyeriskiise of Air Blike rink	Number of Heater Sections	Final Teny sexuare	Cendensation Feet Breat	F. T.	C.	в. т.	C	F T	C.	FT.	('	F. T.	€.	F. T.	C
ਅਲੂ ਵਿੱਚ	1223456678	55 87 113 136 155 173 188 200	Pounds 1605 1655 1615 1574 1537 1005 1475 146	52 81 106 127 116 163 177 100	845 806 758 707 608 630 592 362	50 76 99 120 158 151 168 181	995 926 874 827 784 736 699 666	772 74 113 131 146 160 172	1 073 1 032 980 924 884 831 792 756	46 69 89 108 125 139 133 165	1 205 1 138 1 065 1 018 975 916 877 ,839	14 66 56 101 120 134 148 160	1 272 1 218 1 168 1 110 1 060 1 005 1 967 927	43 63 83 99 115 129 142 153	1.370 1.282 1.250 1.179 1.133 1.080 1.037
39D <sup>2</sup>	1 22 3 6 6 7 5	64 93 120 141 160 177 191 203	675 625 595 550 517 485 156 429	61 88 112 133 151 168 182 194	.819 767 721 651 642 608 574 542	59 84 106 126 143 159 173 185	.961 .894 .840 .704 .750 .708 .676 .642	56 80 102 120 137 152 165 176	1 032 991 954 804 851 805 765 727	55 76 97 115 132 146 158 169	1 100 1 065 1 035 981 947 803 843 804	53 74 93 110 126 140 152 164	1 220 1 165 1 113 1 058 1 019 968 922 ,888	52 72 90 105 121 135 117 158	1.310 1.252 1 190 1.132 1.085 1.000 994 .955
10.	1 22 4 5 6 7 8	73 101 126 147 165 181 195 207	.655 685 569 530 498 465 439 415	70 96 119 139 156 172 186 197	793 740 697 654 654 584 584 519	67 91 113 132 149 164 177 189	S95   S34   S06   700   724   650   648   617	(45 588 1(9) 127 113 157 169 180	994 952 915 854 820 772 731 697	61 85 105 122 138 151 163 174	1 111 1 043 1 003 940 909 ,855 ,811 ,775	62 82 101 117 132 145 157 168	1 167 1 111 1 078 1 019 976 924 885 847	61 80 97 113 127 140 152 162	1 251 1 192 1 131 1 088 1 039 990 952 910
\$t)°	1 22 3 4 5 6 7 8	82 108 133 153 170 185 198 210	635 575 519 510 478 445 449	79 104 126 145 162 177 189 201	.766 .711 .671 .628 504 559 525 500	76 100 120 138 154 168 181 192	.861 .826 .774 .726 .690 .648 .619 .588	74 96 116 133 148 162 173 184	.955 .913 .875 .824 .780 .739 .607	73 93 112 129 143 156 167 178	1 065 988 957 915 864 815 771 740	71 91 105 124 135 151 162 172	1.113 1.085 1.026 979 9.34 889 846 807	70 89 105 120 134 146 157 167	1.191 1.163 1.001 1.042 1.000 950 909 .873
GIF	122845678	90 116 138 157 175 189 202 213	596 556 546 480 458 425 402 380	88 111 132 150 167 180 193 204	740 671 625 596 568 530 500 476	85 108 127 144 159 173 186 196	\$29 795 740 693 656 620 ,565 564	83 101 122 138 153 166 175 189	916 873 821 774 740 669 642	82 101 118 134 148 160 172 181	1 019 950 896 856 816 769 700	\$4) 99 116 130 114 156 167 177	1 060 1 032 900 925 891 845 809 775	79 96 112 127 140 151 161 171	1.131 1.072 1.031 907 .954 .902 .838 .828
767	1 22 3 4 5 6	124 124 145 163 180 194 206 246	556 546 496 460 448 400 885 385	96 119 139 157 172 186 197 208	1,545 045 045 049 575 544 514 450 456	94 115 134 150 165 178 190 201	,795 745 707 661 630 592 567 542	92 113 130 146 159 171 182 193	\$75 \$53 795 764 709 666 635 643	91 110 127 142 155 166 177 187	975 927 880 84 789 747 705 676	107 123 137 150 161 172 182	1 008 937 886 840 800 771 731	88 105 120 133 146 157 167	1.074 1 042 992 989 996 861 824 798

Buffild

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

### Final Temperatures and Condensations

Buffalo Standard Heater

60 LBS.

			60 lbs. 5	iteam Pr	esusure						307.3"	F.			
				Velocity	of Air is	n Feet p	er Minut	. :	Monsured	at 70	F and 28	92" Ba	respector		
erature of	Sections		tid II t	80	110	3 (	F 34 3	1:	200	1-	100	11	r{ ≥ }	1	501
Temerature of Air lentering	Namber Heater Sec	Temperature	Combination per lineal Foot per Hour	F. T.	c.	F. T.	C.	F. T.	C.	F. T.	C.	F. T.	C.	F. T.	C.
217	1 2 3 4 5 6 7 8	58 91 119 141 166 184 200 214	Pounds .761 .715 .670 1.25 .580 .551 .516 .489	55 55 111 131 155 173 155 202	.934 .874 .819 .768 .721 .681 .644	52 80 105 127 145 164 179 192	1.070 1.007 9.56 900 .84.3 806 701 .722	50 76 99 120 139 155 170 183	1.201 1.129 1.075 1.109 958 969 861 822	18 72 94 114 132 148 163 176	1 310 1 225 1 168 1 197 1 050 1 005 959	46 69 90 109 126 141 155 168	1 300 1 318 1 262 1 197 1 138 1 085 1 035	44 66 86 103 121 136 150 162	1 440 1 390 1 339 1 270 1 218 1,160 1 120 1,073
30"	1 2 3 4 5 6 7 8	67 98 126 150 170 187 203 216	711 1850 1650 1690 5692 5628 1995 1693	63 92 118 141 160 177 192 203	907 834 .792 .747 .696 656 620 588	61 111 133 151 167 182 195	1 035 975 911 858 810 767 729 693	50 \$1 107 126 145 161 175 187	1.161 1.088 1.049 969 925 581 533 792	57 81 102 120 138 154 167 180	1.262 1.200 1.136 1.060 1.013 975 919 .883	55 78 98 116 132 147 160 173	1 335 1 290 1 226 1 143 1 004 1 049 .986 962	33 75 93 111 127 142 155 167	1 380 1 360 1 279 1 225 1 170 1 130 1 079 1 036
41r°	12315674	76 106 132 153 174 192 206 219	721 .666 6.22 .570 .538 .511 .476 451	72 100 125 147 165 182 196 200	\$54 \$06 765 627 670 684 597 568	70 95 118 138 157 173 187 189	1 002 925 878 825 783 746 .705 668	68 92 114 133 150 166 179 192	1.122 1.019 1.019 9.59 9.55 5.17 790 .766	66 89 109 127 144 159 172 184	1 218 1 153 1 089 1 025 975 931 885 848	64 86 105 122 138 153 166 178	1 283 1 238 1.171 1 103 1 054 1.013 966 929	62 83 101 118 134 148 160 172	1 329 1 300 1 238 1 180 1 134 1 000 1 035 997
500	12134567	88 113 138 160 170 195 200 222	681 685 595 555 518 487 456 433	84 108 132 152 170 186 200 212	\$26 780 738 665 643 607 574 545	78 103 125 144 162 177 191 203	9665 891 844 791 750 711 675 643	76 99 120 130 156 170 183 195	1 042 987 953 899 853 807 764 731	75 97 116 133 150 164 177 188	1 170 1 107 1 040 977 937 895 851 813	73 94 112 129 144 158 171 182	1 280 1 182 1 119 1 062 1 009 967 927 889	71 91 109 125 140 153 166 177	1 204 1 240 1 196 1 134 1 086 1 009 1 000
F5(1/2	1 2 3 4 5 6 7 8	93 121 145 166 185 201 214 226	661 615 575 565 502 471 1442 1418	90 115 138 158 176 191 205 216	\$00 .740 .702 659 622 585 551 524	87 111 132 131 168 183 196 208	902 857 810 765 728 689 652 622	85 107 127 145 161 175 188 201	1 003 947 912 858 813 773 735 700	83 104 123 140 155 169 182 193	1.075 1.035 994 942 890 856 817 783	82 102 149 135 150 163 175 187	1 175 1 130 1 064 1 010 965 923 882 855	80 99 116 132 146 150 171 181	1,201 1,179 1,185 1,089 1,039 1,998 1,958 1,915
719"	1233 4 237 /	101 128 151 172 189 201 217 229	621 585 518 515 478 450 421 400	99 121 115 161 181 195 208 219	.771 .725 .675 .632 .865 .865 .865 .868 .891	96 119 139 157 173 187 200 212	524 524 776 731 666 665 634 566	94 116 135 152 167 181 193 204	968 926 855 8780 746 706 676	92 113 130 147 161 174 186 197	1 030 1:013 946 906 852 816 777 748	91 110 127 142 156 169 151	1.121 1.075 1.028 969 921 857 851	589 107 123 139 152 165 176 186	1.141 1.119 1.075 1.013 989 968 966 876

Buffals

#### Final Temperatures and Condensations

Buffalo Standard Heater

80 LBS.

80 lbs. Steam Pressure

323.7 F

			OU TON. :	SHERINGER R.	CHARLE						sharp. d	· C			
				Velocity	of Air in	Fret pe	r Mimite	7	leasured	nt 70° F	5. aml 29.	92" B.iri	due terr		
ार भी सम्ब	of trons		500		4304	10	H H 3	1:	2011	1-	100	10	800	17	500
Temperative of Air Enferring	Number of Beater Sections	Frail Temps rature	Condensation per l'unal Fest per Hour	F. T.	C.	F. T.	C.	F. T.	C.	F. T.	C.	F. T.	C.	F.T.	C.
1F 20P	1 2 3 4 5 6 7 8	60 95 124 151 173 193 240 224	Founds ,515 ,769 ,709 ,670 ,624 ,589 ,554 ,520	57 88 116 141 162 181 198 212	1 006 925 871 825 770 730 691 ,653	54 83 109 132 153 171 187 201	1 155 1 072 1 079 956 903 ,888 ,813 ,769	52 79 103 125 145 162 178 192	1 305 1 205 1 130 1 072 1 019 966 921 879	49 75 98 119 138 155 170 185	1 350 1 310 1 240 1 182 1 121 1 071 1 021 .984	48 72 94 113 132 148 163 177	1.522 1.419 1.343 1.269 1.160 1.112 1.069	46, 69, 90, 109, 129, 132, 156, 169	1.591 1.502 1.430 1.357 1.294 1.294 1.159
₹1¥"	1 2 3 4 5 6 7 8	103 132 157 179 196 213 227	. 795 . 748 . 695 . 613 . 666 . 565 . 534 . 502	65 96 123 146 167 185 201 215	952 899 844 790 744 704 689	62 91 116 138 158 176 191 205	1 088 1.039 975 922 .868 .830 .783 .744	\$6 110 131 150 167 182 195	1 .224 1 115 1 089 1 032 .979 .942 889 .843	58 83 105 125 144 160 175 188	1,332 1 264 1,191 1,136 1 081 1,031 1,990 1942	87   80   101   120   138   154   168   181	1.460 1.363 1.289 1.228 1.172 1.124 1.073 1.028	55 77 97 115 132 147 161 174	1 530 1 440 1 369 1 365 1 245 1 192 1 147 1 100
der	1 2 3 4 5 6 7 4	77 109 138 162 182 200 216 230	.755 .707 .667 .618 .578 .544 .513	74 104 130 153 173 190 205 219	.925 .874 816 .770 .721 .680 611 608	71 99 123 145 164 181 195 209	1.052 1.004 .941 .896 .841 .801 .754 .719	69 94 117 137 155 172 187 200	1.182 1.104 1.049 1.942 1.938 1.807 1.860 1.818	67 91 112 132 150 166 179 192	1.286 1.215 1.144 1.100 1.043 1.000 .947 .905	66   88   108   126   113   150   173   185	1 414 1,310 1 234 1,172 1,129 1 079 1 085 ,986	54 86 105 128 139 153 167 179	1,470 1,410 1,329 1,275 1,206 1,153 1,111 1,062
Fago	1 22 3 4 5 6 7 5	\$6 117 141 167 157 204 219 233	734 GS6 640 503 508 524 493 466	83 111 136 159 178 191 209 222	,870   \$30   781   783   653   653   648   585	80 107 130 151 169 185 200 212	1.020 970 .907 .962 .807 .766 .730 .689	78 102 121 144 161 177 101 204	1.141 1.062 1.068 961 .965 .864 .825 .787	76 90 119 138 155 171 154 196	1 .239 1 168 1 096 1 051 .908 (60 .914 .870	75 96 115 133 1 150 165 1 178 1 190	1.360 1.255 1.180 1.132 1.085 1.085 1.042 996 .952	73 94 112 129 145 159 172 184	1 409 1:350 1 267 1 212 1 159 1:111 1:069 1:024
97835	1 2 3 4 5 6 7	95 124 150 173 192 289 224 287	.714 .655 .612 .572 .537 .507 .479 .451	91 119 113 164 185 190 1 213 226	.844 803 753 708 607 631 565	89 114 137 157 174 190 201 217	.986 .920 .873 .827 .774 .739 .701 .668	87 111 131 150 167 182 196 208	1.105 1.041 956 920 873 830 .795 .756	85 107 127 145 161 176 189 201	1 190 1 120 1 065 1 016 958 920 879 840	84 104 123 140 156 150 183 195	1 305 1 200 1 143 1 091 1 043 996 ,957	102 120 130 151 165 177 180	1.347 1.288 1.225 1.168 1.110 1.071 1.024 986
711	1233 4 5 6 7	103 132 157 178 197 213 227	673 685 591 518 517 , 486 459	100 127 150 170 188 204 217	\$15 775 726 682 4640 64 \$	100 111 103 150 150 200	953 886 846 794 746 746 710 672	96 118 139 157 173 188 200	1.061 .980 .910 .890 .810 .802 .760	94 115 131 151 167 181 193	1.144 1.072 1.018 969 929 881 848	92 111 130 147 162 177	1 251 1 119 1 090 1 656 1 000 156 519	91 110 127 143 157 170 182	1 . 286 1 . 228 1 . 165 1 . 121 1 . 060 1 . 020 98 [

Buffild

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

### Final Temperatures and Condensations

Buffalo Standard Heater

100 LBS.

			100 lhs.	Steam	Pressur	e					337 6	F			
_				Velocity	of Air is	Feet pa	r Minute		Mentare	dat 70	F and 2	92" Ba	rometer.		
ing of	of		(15 H )	-	4141	1	CHID	11	918CF	1	4(1)	14	1 <sub>3</sub> 8 9( )	11	~! +
Temper duft of Air lintering	Number of Heaver Sections	Timperatio	Cambusation per Lama Foot per Hour	F. T.	C.	F. T.	C.	F. T.	C.	F. T.	c.	F. T.	C.	F. T.	C.
5m.	11 11 11 11 11 11 11 11 11 11 11 11 11	129 129 156 179 258 218 244	Pounds 80.9 80.5 75.2 70.1 65.5 62.0 58.1 .651	5% 91 120 145 16% 205 220	1 040 979 920 861 814 773 728	55 86 112 137 158 177 194 200	1 209 1 139 1 060 1 009 9 47 903 855 815	52 81 106 120 150 168 185 180	1,319 1,290 1,190 1,129 1,072 1,106 ,976 ,928	50 77 101 123 143 160 176 190	1 449 1 371 1 363 1 242 1 184 1 128 1 076 1 027	48 74 96 117 146 153 169 183	1 543 1 486 1 800 1 545 1 274 1 223 1 172 1 125	#7 71 92 112 139 147 162 175	1 680 1 578 1 491 1 427 1 560 1 515 1 285 1 202
.ser	1	71 100 150 162 185 201 221 230	\$17 754 759 683 660 564 533	67 98 196 152 173 192 208 223	1 020 -937 -884 -840 -786 -745 -700 -665	63 93 119 142 164 182 198 212	1 139 1 086 1 028 967 920 874 826 785	64 88 113 135 156 173 189 203	1 279 1 199 1 118 1 085 1 040 989 .940 .897	59 84 107 128 148 165 184	1 400 1 300 1 240 1 182 1 136 1 088 1 032 991	57 82 103 124 142 158 173 187	1.489 1.480 1.345 1.204 1.231 1.177 1.126 1.082	55 78 99 148 136 152 167 180	1 554 1 485 1 190 1 300 1 300 1 263 1 212 1 163
\$11	1 2 3 5 6 8	\$113 1142 167 189 208 224 239	.827 .754 704 657 611 570 512 515	76 106 134 158 178 196 219 226	.904 940 865 813 .759 .718 676 .642	72 100 126 148 169 187 202 216	1.102 1.034 995 932 886 .845 796 .760	70 96 120 141 161 178 194 207	1 234 1 157 1 105 1 044 1 000 954 912 865	68 92 115 135 154 170 186 199	1 351 1 252 1 209 1 148 1 098 1 006 1 008	66 90 110 130 148 161 179 192	1 434 1 375 1 290 1 240 1 188 1 140 1 094 1 019	64 87 107 125 142 158 172 185	1 494 1 155 1 389 1 349 1 291 1 291 1 169 1 125
7atr°	1 23 4 5 6 7 8	89 120 148 173 194 213 228 242	\$00 .723 676 636 503 562 525 ,497	\$4 143 140 163 183 201 216 229	.989 .868 .828 .770 .731 .604 .653 .618	84 108 133 155 174 194 206 220	1 070 1 000 939 906 852 810 767 734	79 104 127 148 167 184 198 214	1.194 1.115 1.053 1.013 965 926 875 835	77 100 122 132 160 176 190 203	1 305 1 204 1 160 1 10 1 060 1 015 965 925	75 97 118 137 154 170 183 196	1 379 1 293 1 253 1 199 1 142 1 103 1 048 1 007	73 95 114 132 149 164 177 190	1 431 1 391 1 326 1 271 1 225 1 189 1 121 1 086
GII <sup>2</sup>	123 45 67 8	97 128 156 179 199 217 202 246	.765 702 655 615 572 .511 .507 .481	93 122 147 169 189 206 221 234	910 854 800 751 709 672 634 600	90) 117 140 161 180 196 211 224	1 035 981 924 871 826 782 713 707	88 113 136 154 173 189 293 216	1,154 1 075 1 036 973 932 591 846 800	56 160 160 140 166 151 195 205	1 255 1 180 1 127 1 075 1 021 1 974 931 895	84 105 175 144 160 175 188 201	1 323 1 239 1 196 1 158 1 100 1 638 1 007 975	82 103 122 149 155 170 182	1 .509 1 .550 1 285 1 224 1 .180 1 1.89 1 (680 1 (6.9)
711`	1233 100 07	105 135 161 184 204 221 235	724 671 628 200 551 52) (86)	101 129 154 175 193 210 221 237	N13 772 721 641 641	104 134 147 168 183 284 215 228	1,000 930 890 815 700 753 713	96 120 142 161 175 193 207	1.071 1.033 1992 944 894 850 810	94 116 136 135 172 187 200 212	1 159 1 109 1 062 1 026 982 942 897	\$63 1.1.1 1.3.3 1.5.0 1.6.6 1.5.1 1.6.3	1 269 1 210 1 160 1 102 1 055 1 021 969	91 111 120 131 161 175 187	1 0005 1 200 1 221 1 170 1 130 1 087 1 035

Buffali

#### Final Temperatures and Condensations

Vento Cast Iron Heater

Regular Section Standard Spacing 5" Centers of Sections Steam 5 lb. Gauge 227"

				Ve	docity T	hrough I	lenter in	First per	r Minute	. M	lensured	nt 70° F			
Air	Jo diana	6	UKE	4	ы	16	KH)	12	200	14	ECH 1	16	1001	15	d)#)
Temperature of Entering Air	Number of Stacks Deep	Final Terriper- atter Art Lenvinsk Heater	Cord, Ibs. per Sq. Ft. per Hour	F. T.	C.	F. T.	c.	F. T.	C.	F. T.	C.	F. T.	C.	F. T.	C.
207	1235+5674	58 87 110 130 144 156 167 175	1.46 1.29 1.15 1.06 93 .87 81	54 81 103 122 136 148 159 167	1.75 1.57 1.42 1.31 1.10 1.10 1.02 94	51 76 97 115 130 142 152 161	1 99 1 80 1 65 1 52 1 41 1 30 1 21 1 13	49 72 92 110 124 186 146 155	2 23 2 00 1 85 1 73 1 60 1 49 1 130	47 (0) 88 105 1 119 1 30 141 150	2 42 2 2 1 2 06 1.91 1.78 1 65 1.55 1 16	45 66 85 101 114 126 136 145	2 56 2 35 2 22 2 08 1 93 1 81 1 70 1 60	4.3 6.1 5.2 97 110 122 132 141	2 65 2 54 2 38 2 22 2 08 1 96 1 85 1 .74
Mr. P	1 2 3 4 5 6 7	156 93 115 134 148 159 169 177	1 39 1 21 1 09 1 00 9 1 .83 .76	62 87 108 126 140 151 161 169	1 64 1 46 1 33 1 23 1 13 1 04 96 89	60 83 103 129 134 145 155 163	1.92 1.70 1.56 1.44 1.33 1.23 1.15 1.07	58 79 98 115 128 139 149 158	2.17 1.89 1.75 1.63 1.51 1.40 1.31 1.23	56 76 94 110 123 134 144 153	2 33 2 06 1.91 1.80 1.67 1.56 1.46 1.38	54 73 91 106 118 130 139	2 46 2.21 2.08 1.95 1.80 1.71 1.60 1.51	52 71 88 102 115 126 135	2.54 2.37 2.23 2.08 1.96 1.85 1.73 1.64
40°	1 2 3 4 6 6 7 8	74 100 121 138 151 162 171 170	8 31 8 15 8 05 9 5 78 72 67	70 94 114 130 144 154 164 171	1 54 1 39 1 26 1 15 1 07 97 97 91	68 90 100 124 138 148 158 165	1.80 1.60 1.47 1.35 1.20 1.15 1.08	66 86 101 119 132 143 153 160	2 00 1.77 1 64 1 52 1.42 1.32 1.21 1.15	64 83 100 115 127 138 148 155	2.16 1.93 1.79 1.68 1.56 1.47 1.39	62 81 97 111 123 134 143 151	2 26 2 10 1 95 1 82 1.70 1 60 1.51 1.42	61 79 94 108 120 131 159 147	2 42 2 27 2 08 1 96 1 85 1 75 1 53 1 54
(11:	1 2 3 4 5 6	901 112 131 146 158 167	1 15 1 00 ,91 83 ,75	86 107 124 139 151 160	1 34 1.21 1 (7) 1.01 93 .85	84 103 120 184 145 155	1 54 1 38 1 28 1 19 1 09 1 02	82 100 116 129 140 150	1 60 1 54 1 44 1 33 1 23 1 15	81 98 113 125 136 146	1.89 1.71 1.58 1.40 1.36 1.29	80 96 110 122 133 142	2.05 1.85 1.71 1.50 1.50 1.40	79 94 108 119 130 139	2.19 1.96 1.55 1.70 1.62 1.52

### Friction of Air Through Vento Cast Iron Heaters

Friction Loss in Inches of Water. Air Measured at 70° P.

Regular Section

Velomity Feet per	Sections				NUMBER (	DF STACKS			
Minute	Inches	1	2	3	14	5	ß	7	s
600	.5	0.021	0.040	0.058	0.076	0.094	0.112	0.130	0.149
700	, P	0.028	0.054	0.079	0.105	0.130	0.155	0.180	0.205
800	5	0.037	0.070	0.103	0.135	0.167	0.200	0.232	0.265
1100	ő	0.047	0.088	0.129	0.170	0.211	0.252	0.293	0.335
1000		0.059	0.109	0.160	0.211	0.262	0.313	0.364	0.415
1100	5	0.071	0.132	0.193	0.255	0.316	0.377	0.438	0.501
1200	5	0.084	0.157	0.230	0.303	0.376	0.149	0.522	0.596
1300	ő	0.099	0.185	0.271	0.356	0.142	0.528	0.614	0.701
1.100	5	0.115	0.214	0.314	0.111	0.513	0.612	0.712	0.813
1500	5	0.132	0.246	10.360	0.474	0.588	0.702	0.516	0.932
16600	5	0.150	0.280	0.410	0.540	0.670	0.800	0.930 .	1.060
1700	5	0.169	0.316	0.463	0.609	0.756	0.903	1.049	1.197
1800	.5	0.190	0.351	0.518	0.683	0.545	1.012	1.177	1.342

Buffalo

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

### Buffalo Single Vertical Engines-Class "A"

Maximum Horsepower Allowable for Corresponding Frame

High Pressure

Maximum Iorsepower	Махиони	Cslimiter		Floor Space			icharel Whool		m and et Pipes	Shipping
Horsepower	R P M.	D. ameter and Stroke	Length	Width	Height	Diameter	Face	Steam	Exhaust	Weight
6	550	4 x 4	34	3:2	46	27	512	114	11.,	1260
12	475	5 x 5	37	34	55	31	6	112	2 "	1740
20	450	6 x 6	41	37	65	33	614	2	21.,	2400
20	425	7 x 7	41	37	65	33	612	2	21,	2800
45	400	SXS	43	40	78	39	7	215	3	3270
45	\$00	10 x 8	43	40	78	39	7	3	31,	3420
65	350	8 x 10	52	52	96	49	1115	$21_{2}$	3 "	6070
65	33,543	10 x 10	52	52	96	49	1115	3	31.,	6240
6.5	350	12 x 10	52	52	96	49	1132	315	4	6460
95	300	10 x 12	62	64	118	57	13	31,	-1	5530
95	300	12 x 12	62	64	118	57	13	4	5	SHIRDE

 Decem	

18	450	8 x 6	41	37	65	33	614	21.,	3	2450
45	400	12 x 8	43	40	78	39	7	3 ~	31.	3750
45	400	13 x 8	43	40	78	39	7	3	315	\$ 1660
45	400	15 x 8	43	40	78	39	7	31.,	4	154500
65	350	15 x 10	52	52	96	41)	1114	3 ~	314	7150
95	300	15 x 12	62	64	118	57	13	4	5	10830
95	300	18 x 12	62	61	118	57	13	5	6	11270

### Buffalo Horizontal Engines, Center Crank-Class "A"

						1			
300	5 x 10	70	30	30	40	81.,	11,	21,	1980
300	6 x 10	70	30	30	40	814	115		2080
250	7 x 12	86	34	32	-4()	S1.,	2 -	9	2750
250	8 x 12	86	34	3:2	40	815	2	2	2970
225	8 x 14	102	4()	37	-15)	10	216		3850
225	9 x 14	102	40	37	49	10	21,	31,	4070
	300 250 250 225	300 6 x 10 250 7 x 12 250 8 x 12 225 8 x 14	300 6 x 10 70 250 7 x 12 86 250 8 x 12 86 225 8 x 14 102	300     6 x 10     70     30       250     7 x 12     86     34       250     8 x 12     86     34       225     8 x 14     102     40	300     6 x 10     70     30     30       250     7 x 12     86     34     32       250     8 x 12     86     34     32       225     8 x 14     102     40     37	300     6 x 10     70     30     30     40       250     7 x 12     86     34     32     40       250     8 x 12     86     34     32     40       225     8 x 14     102     40     37     49	$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$

### Buffalo Single Vertical Engines-Class "I"

Cylinder Below Shaft

Maxin.um	Maximum	Cylinder Diameter	Steam and E	Ixhaust Pipes	DD: 6
Hotsquare	H P M.	and Stroke	Steam	Exhnust	Weigh
5	600	3 x 31,	1	11,	310
712	500	4 x 3½	1	132	370
41	\$100	412 x 5	111	11,	780
1812	325	512 x 7	111	11.5	1100
25	275	615 x 8	113	9	1500
30	220	732 x 9	2	13.3	2000



# Planoidal Fans With Proper Combinations of Heaters and Engines for Public Buildings and Industrial Installations

A see E		Let of Manute	Buttal	o Standard	Heater	Ha	gitti.	ber	Cubic Vir per	Feet of Minute	Buffal	Standard	Henter	Ling	52.7×**
Fats Naturber	1. Static	Promise	Armign	Size	Clear And Spure Feet	Low	High	Fan Number	l' Marie Presente		Arrelight	Size	Char tress	Low	High
50	1,550	6,140	Hangle	2'0"x3'1" 3'0"x3'10" 3'0"x1'1"	4 i 5 2 6 0	5 x 6	4x1A 4x31 <sub>2</sub> 1	120	24,200	37,05)	Single	0/8748/107 7/0747/107 7/0748/17 7/0748/107	21 2 25 1 27 2 28 (1	15 x 8	8±4A 7x12N
55	5,5(x)	7,750	Single	3'0"x3'10" 3'0"x4'1" 3'0"x4'10" 3'0"x5'1"	5.2 6.0 6.8 7.8	8 x 6	4x4A 4x31 <sub>2</sub> 1				Rack To Buck	7'0"x9'4" 7'0" 9'10" 4'0"x6'10" 4'6"x5'10" 4 6"x6'4" 4'6"x6'10"	24.2 26.2 28.1		
€40	6,550	0,2170	Single	3'0"x4'10" 3'0"x5'1" 3'0"x5'10"	6.8 7.6 8.1	% x 6	fixad Hazal					4'6"x7'4" 5'0"x6'1" 5'0"x6'10" 5'0"x7'1" 5'0"x7'1"	190 6 28 2 30 8 34 2 35, 4		
70	5,9(30)	12,630	Single	3'0"x5'10" 1'0"x5'1" 1'0"x5'10" 1'0"x6'10" 1'0"x6'10"	5.4 9.7 10.7 11.2 12.6 12.1	10 x S	5x5A 11 <sub>2</sub> x51	130	30,550	43,250	Single	7'0"x8'10" 7'0"x9'4" 7'0"x9'40" 4'0"x6'10" 4'0"x7'4" 5'0"x6'10"	291.0 30.7 32.5 25.4 30.6 30.8	15x8	8x5A 7x12N
50	14,630	16,450	Single	1'0"x6'1" 1'0"x6'10' 1'0"x5'10' 1'0"x5'10'	11.2 12 h 12.1	10 x 8	6x6A 5½x71 5x10N	51-x71	Ш		To Back	5'0"x7'4" 5'0"x7'10" 6'0"x7'1" 6'0"x7'10"	33 2 35 4 39 6 12 6		
				1'6'x6'10" 4'6'x7'1" 5'0'x6'1" 5'0"x6'10"	13 1 14.2 15.3 14.1 15.4				35,650	50,400	Back To Back	5'0"\7'4" 5'0"\7'10" 6'0"\7'10" 6'0"\7'10"	83.2 85 ± 89.6 12.6	16x10	10x8A 7x12N
90	14,730	20,850	Single	4'6"x6'10" 4'6"x7'1" 5'0"x6'4"	14.2 15.3 14.1	10 x 8	7×7A 51/×71 5×10N		Ш			6'0"x8'4" 6'0"x8'10" 7'0"x7'4"	45.4 45.4 47.2		
				5'0"\$6'10" 5'0"\$7'4" 5'0"\$7'10" 6'0"\$7'4"	15 4 16 6 17.7 19 8		JEII.V	150	60,(HR)	57,900	Back To Back	6/07x7/17 6/07x7/10* 6/07x8/17 6/07x8/10* 7/07x8/10*	29 6 42.6 15 1 48.4 17 2	18x12	\$\(\)10\\ \$\(\)12\\
100	18,200	25,750	Single	5'0"x7'4" 5'0"x7'10" 6'0"x7'4"	16 6 17 7 19 8	12 x 8	x 8 7x7A 61 y NI 5x 10 N			1	7'0"\7'10" 7'0"\8'4"	50 S 51 F			
				6/0"\7'10" 6/0"\8'\" 6/0"\8'10" 7'0"\7'10" 7'0"\7'10"	21.3 22.7 24.2 23.6 25.4		6XUN	160	46,450	65,700 `	Back To Back	6'0'x8'1' 6'0'x8'10' 7'0'x7'1' 7'0'x7'10' 7'0'x8'1'	15 1 18 1 47.2 50 8 54 4 55 0	18x12	5x10A 9x14N
110	22,000	31,100	Single	6'0"x7'10' 6'0"x8'11' 6'0"x8'10' 7'0"x7'11' 7'0"x7'10' 7'0"x8'10' 7'0"x8'10' 7'0"x8'10'	21.3 22.7 24.2 2.4 25.4 27.2 20.0 30.7	15 x 8	\$15.1 715.291 55.105 65.105			Back 70°×7°1° 47.2 70°×7°10° 50.8 70°×8°10° 54.4 70°×8°10° 58.0 70°×8°10° 61.1		61 T 63 H			

-Ruffalo

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

### Niagara Conoidal Fans

With Proper Combinations of Heaters and Engines for Public Buildings and Industrial Installations

N N	Cular Air per	Ministr	Buffal	o Standard			ngine Stae	1		Feet of Minute	Buffal	o Standard	Heater		ito Kitie
Fan Autaber	Presult	Persone	Arrang .	Size	Cear Ama	Low	Migh Preventer	Fan Number	l' statir	Statio	Armuge	Size	Char Area Square Free	Present	The state of the s
ŧ	4,895	(),4),1))	Single	3'0"\3'10"	5.2			10	30,550	13,250	Back To	1'6"\6'10" 1'6"\7'1"	25 1	1515	1000
11;	6,145	8,750	Single	3'0"x4'4" 3'0"x4'10" 3'0"x5'11"	6.0 6.8 7.6		4x1A 8x81 <sub>2</sub> 1				Back	5'0"x6'10" 5'0"x7'1" 5'0"x7'10" 6'0"x7'11" 6'0"x7'10"	30 K 31, J 35 8 19 6 12 6	1	7) Vot 3,100
5	7.645	10,520	Single	3'0"\3'1" 3'0"\3'10" 1'0"\3'11"	7 6 8 4 9 7	515	5x11 1x3131	11	37,000	52,300	Back To Back	5'0"x7'10" 6'0"x7'11" 6'0"x7'10"	42.6	15x8	5151 71 <sub>93</sub> 91 5110 V
¥1,	9,250	13,100	Single	FOTAS 10" FOTAS 10" FOTAS 10" FOTAS 11"	8.4 9.7 10 7	656	5x5 \ 4x3] <sub>2</sub> ]					6/0*x8/3* 6/0*x8/10* 7/0*x7/3* 7/0*x7/10*	15 1 15 1 47 2 50 S		
				F6"x5'10" F6"x5'10" 4'6"x6'4"	12 f 12 f 13 f	1		12	11,050	12,300	Hyek To Back	6'0"\7'19" 6'0"\5'1" 6'0"\5'10"	12.6 15.1 18.1	1548	100 S V 7x12N
1)	11,000	15,550	Single	4'0"x5'10" 4'0"x6'1" 4'0"x6'10" 4'6"x5'10" 4'6"x6'4"	10.7 11.2 12.6 12.1 13.1	SaG	3x3A 44gx31					6 0735/10* 7'0*37'1 7'0*37'10' 7'0*38'11' 7'0*38'10' 7'0*38'10'	47.2 50 \$ 54 4 58 0 61.4		7.12.4
				116" v6" 111" 116" v7" 1"	14.2 15.3	1		13	\$1,650	73,050	Back To	7/0*\7'10* 7/0*\7'10*	50 S	15x10	3011
7	14,050	21,200	Single	4'6" w/10" 4'6" x7'1" /'0" x /'10" 5'0" x7'10" 5'0" x7'10" 6'0" x7'10"	14.2 15.1 15.1 15.4 17.7 19.8 21.3	10x8	50.571 51.571				Three Sale By Sale	707x8'10" 7'07x9'10" 7'07x9'10" 7'07x7'19" 100'x7'10" 6'07x8'10" 6'07x8'10" 7'07x7'1"	58.0 61.4 65.0 53.1 59.4 63.9 98.1 72.6 70.8		7842N
`	19 %0	27,650	Single	5'0x7"10" 6'0"x7"4" 6'0"x7"10" 6'0"x8"10" 7'0"x8"10" 7'0"x7"10" 7'0"x8"1"	17.77 19.8 21.3 22.7 23.6 23.7 23.7 23.7 23.7 23.7 23.7 23.7 23.7	10π8	17.2.71	11	eSCE <sub>a</sub> (m3t)	54,900	Back To Back Thus Side	7'0"\\\'10" 7'0"\\\9'\\" 7'0"\\9'\\" 6'0"\\7'\\" 6'0"\\7'\\" 6'0"\\7'\\\ 7'0"\\7'\\*	58.0 61.3 65.0 59.4 63.6 68.1 72.6	16210	8x10A 7x12N
9	21,750	35,06e)	Single	u/mxs/gr u/mxs/gr 7/mxs/gr 7/mx7/gr 7/mx8/gr 7/mx8/gr 7/mx8/gr 7/mx8/gr 7/mx8/gr	99.7 21.2 2.16 25.1 97.2 30.0 40.7 42.5	1258	6X6A 107,881				184 Side	7107471107 7107481107	70 8 2 5 6		I
111	30,530	13,250	S. r. gla	7'07x8'47 7'04x8'4 7 7'07x9 4' 7'07x9'40'	27 2 29 0 30 7 12 5	111	7×7 \ 61 ×1		ı						

Buffalo

### Turbo Conoidal Fans

With Proper Combinations of Heaters and Engines for Public Buildings and Industrial Installations

b.		Feet of Minute	Buffale	Standard l	Howter	Du	gine	7. X	Cubir Air je r		Martful.	Standard	Henter	Em	M1124.
Fan Namber	Pressure	Promise Promise	Armige	Size	Clear Nn a Aquanti Foot	Link	High	Fan Number	Pressure	Presente	Arrange	Size	Clear Area Square Even	Low	Pressure
4	4,450	6,270	Single	3'0"x3'4" 3'0"x3'10"	\$ 4 5 2			812	251,100	25,400	Single	1/0"x7"1" 1/0"x7"10" 1/0"x8"1"	19 S 21 3 22 7	10x8	658A 515571 757A
\$1 <sub>2</sub>	5,640	7,950	Single	8'0"x8'10" 3'0"x8'10" 3'0"x8'10" 3'0"x5'1"	5.2 6 (1 6 × 7 6		4×4.5 4×33.2 I		1		Back To Back	6'0"\\\"10" 7'0"\\\"1" 7'0"\\\"7'10" 7'0"\\\\'1" 4'0"\\\'1" 4'0"\\\"4"	24 2 23 6 25 4 27 2 19 4 21 4 22 4 25 2		
5	6,950	9,500	Single	3'0"x4'10" 3'0"x5'1" 3'0"x5'10" 1'0"x5'1"	6,8 7,6 8,1 9,7	Tou.S	3x3A 4x83 <sub>2</sub> 1				Innex	1/0/x6/10* 1/6/x5/10* 4/6/x6/4* 1/6/x6/10*	212		
ăt <sub>y</sub>	K,100	11,880	Single	8'0"x5'10" 4'0"x5'1" 4'0"x5'10" 4'0"x6'4"	8 4 9.7 10 7 11 2	tinti	5x5A Pyx5I	Ü	22.500	31,500	Single	6'0"x7'10" 6'0"x8'4" 6'0"x8'10" 7'0"x7'1" 7'0"x7'10" 7'0"x8'4"	21 3 22 7 24 2 23 6 25 1 27 2 29 0	12x8	7×7A 61 y × SI 6×10 N
6	1 се, синст	11,120	Single	#10"x5"#" #10"x510" #10"x510" #10"x6110" #16"x6110" #16"x614"	9.7 10.7 11.2 12.6 12.1 13.1	Sa6	5x5A 41 <sub>7</sub> x5I				Back To Back	7'0"\\\"10" 7'0"\\\"4'" \$'0"\\\\$'10" \$'0"\\\\$'10" \$'0"\\\\$'10" \$'0"\\\\\$'10" \$'0"\\\\"10" \$'0"\\\"1" \$'0"\\\"1" \$'0"\\\"1" \$'0"\\\"1"	29 0 7 4 4 2 2 2 1 6 2	7	
$6^{t_g}$	11,730	16,600	Single	1'00'x6'10" 1'0"x5'10"	121	856	axiA Paxil					5'0°x6'10°	30.8		
				4'6"x6'4" 1'6"x6'10" 4'6"x7'4" 5'0"x6'1" 5'0"x6'10" 5'0"x7'1"	13 1 14 2 15 3 14.1 15.4 16.6			10	27,860	39,300	Single Back To Back	7'0"x8'10" 7'0"x8'10" 7'0"x9'4" 4'6'x6'4" 4'6'x6'10" 4'6'x7'4' 5'0"x6'4"	25 4 29 0 30 7 26 2 25 4 30 6 28 2	15x5	7x7A 64 x81 6x10N
7	13,640	19,250	Single	4'6"×6'10" 4'6"×7'4"	15.3	10x8	6x64 54yx71				Dack	5/07\6/10* 5/07\7/10* 5/07\7/10*	30 S 33 2 35.1		
				5'0"x6'10" 5'0"x6'10" 5'0"x7'1" 5'0"x7'10"	16.6			11	33,700	17,150	Back To Back	5/0*x7/1* 5/0*x7/10* 6/0*x7/1* 6/0*x7/10*	3318.45	15x8	SESA 71,x91 Galon
719	15,610	22,100	Single	5'0"x6'10' 5'0"x7'4" 5'0"x7'10' 6'0"x7'11' 6'0"x7'11'	16 6 17 7 19 8	10%	086 \$ 51 <sub>23</sub> 71					ETPATT	15 1 17.2		
`	17,5681	25,160	Smel	5/01x7/81 5/01x7/10/ 6/01x7/10/ 6/01x7/10/ 6/01x8/10/ 7/01x7/17/	19 S 21 3 22 7	BIAN	51,x71								

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

B. T. U. Transmitted per Hour per Square Foot of lature Between Inside and Outside Air	He:	ating S	Surface	For Va	arious D	ifference	es in T	emper-
Material	-5	1-	50	1,12	70	50	×1,	14.1
Windows, Single Glass, Full Sash Area.	а	1.09	51.5	65 1	76.3	87.2	92.7	98.1
Double Full Glass, Sash Area.	14	0.46	23.0	27 6	32.2	36.8	39.1	11 1
Plate Glass, Full Sash Area	1	1.00	50.0	60 ()	70.0	80.0	No 1)	() ()
Skylight, Single Glass, Full Sash Area	71	1 16	58.0	6501 (5	81.2	92.5	50% ()	101-1
Double Glass, Full Sash Area.	a	0.48	21.0	25 8	33 6	38 1	10.5	43.2
Doors ) 1" Thick	11	0.41	20.5	24.6	28.7	32 8	34.9	25(5-1)
or Pine 1 by "	23	0.32	16.0	19.2	22.4	25 6	27.2	24 4
Partitions 2" "	21	0.27	13 5	16.2	18.9	21.6	23 0	21.3
Brick Wall, Plain, 812 Thick.	41	0.37	18.5	22.2	25 9	29 6	31.5	33.3
1:3"	- 23	0.29	14 5	17.4	20/3	23.2	217	26.1
1712" "	21.	0.25	12.5	15.0	17.5	20.0	21.3	22.5
1)-30 11	21.	0.22	11.0	13 2	15.4	17.6	18.7	19 8
261," "	31	0.19	9.5	11 4	13 3	15 2	16.1	17 1
<sup>3</sup> 4" Plaster on one side, 8 <sup>1</sup> 2" Thick.	- 24	0.36	18.0	21.6	25 2	28.8	30 6	32 6
13"	23	0.28	14.0	16.8	19.6	22.4	2018	25.2
171,,"	- 31	0.24	12.0	14.4	16.8	19.2	20.4	22 6
·3·3* " · · ·	24	0.21	10.5	13 6	15.7	17.8	15 9	19.9
2614" "	- 21	0.18	9.0	10.8	12.6	11 1	15.3	16 2
2.4" Air Space, 34" Plaster on one side, 812" Thick.	28	0.25	12.5	15.0	17.5	20.0	21/3	22.5
1215" 0	- 21	0.21	10.5	12.6	15.7	17.8	18 9	19.9
17" "	11	0.19	9.5	11.4	13 3	15.2	16 1	17.1
2112" "	18	0.16	8.0	9.6	11.2	12.8	13.6	11-1
26"	23	0.14	7.0	8.4	9.8	11.2	11.9	12 6
Furred and 34" Plaster 1" Thick	- 23	0.28	14.0	16 S	19.6	22 1	23 8	25 2
S1." "	23.	0.23	11.5	13.8	16.1	18 1	19 6	20.7
13"	13	0.20	10.0	12.0	14.0	16 0	17 0	18.0
171,"	11	0.18	9.0	10.8	12 6	14.4	15.3	16.2
· 21.3 °	11	0.16	8.0	9.6	11.2	12.8	13.6	14.4
Frame Wall, Clapboard, Stud and Plaster. 5" Thick	11	0.44	22.0	26.4	30.8	35 2	37.4	39 6
Clapboard, Paper, Stud and Plaster "		0.31	15.5	18.6	21.7	24.8	26 4	27.9
Clapboard, Sheathing, Stud and Plaster.	11	0.28	14 0	16.8	19.6	22 4	23.8	25 2
Clapboard, Paper, Sheathing, Stud and Plaster.	:1	0.23	11.5	13.8	16.1	18.4	19 6	20.7
Concrete, Solid, 2" Thick.	Ь	0.78	39.0	16 S	54.6	62 4	66 3	70.2
37 11	b	0.71	35 5	42 6	49.7	56 S	60.4	63.9
40 4	1	0.66	33 0	39 6	46.2	52 S	56 1	59.4
G	Ь		28 0	33.6	39 2	44.8	17 6	50.4
Partition Hollan Tile 14" Plaster both sides 2" Thick			20.5	24 6	128 7	2012 52	214 9	3365 49

F CELLULY TRIVE & T SCHOOL F. F. C. C.						
N1 ." "	11	0.23	11.5	13.8	16.1	18 1
13° "	13	0.20	10.0	12.0	14.0	16.0
1-1,"	11	0.18	9.0	10.8	12 6	14.4
6303° 65	11	0.16	8.0	9.6	11.2	12.8
Frame Wall, Clapboard, Stud and Plaster. 5" Thick	- 11	0.44	22.0	26.4	30.8	35 2
Clapboard, Paper, Stud and Plaster "	11	0.31	15 5	18.6	21.7	24.8
Chapboard, Sheathing, Stud and Plaster.	:1	0.28	14 0	16.8	19.6	22 4
Clapboard, Paper, Sheathing, Stud and Plaster.	:1	0.23	11.5	13.8	16.1	18.4
Concrete, Solid, 2" Thick.	Ъ	0.78	39.0	46 S	54.6	62.4
3° ''	Ъ	0.71	35 5	42 6	49.7	56 S
40 (1	b	0.66	33.0	39 6	46.2	52 S
6" "	1	0.56	28 0	33.6	39 2	44.8
D 44 - 11 11 7721 1 /8 701 4 1 41 11 - 0/ 773 1 1		O 44	1300 F	13.4 42	1341 ***	1843 61

Linker and A Lineson i Thick		2.5	All march	19.U	117 (5	1 12 11	and the P		mar P au
×1 ." "		21	0.23	11.5	13/8	16.1	18 1	19.6	20.7
13" "		13	0.20	10.0	12.0	14.0	16 0	17 0	18 0
1712" "		11	0.18	9.0	10.8	12.6	14.4	15.3	16.2
· > > * * * * * * * * * * * * * * * * *		11	0.16	8.0	9.6	11.2	12.8	13.6	14.4
Frame Wall, Clapboard, Stud and Plaster. 5	" Thick		0.44	22.0	26.4	30.8	35 2	37.4	39 6
Clapboard, Paper, Stud and Plaste			0.31	15.5	18.6	21.7	24.8	26 4	27.9
Clapboard, Sheathing, Stud and P			0.28	14 0	16.8	19.6	22 4	23.8	25 2
Clapboard, Paper, Sheathing, Stud and Pla		:1	0.23	11.5	13.8	16.1	18.4	19 6	20.7
Concrete, Solid, 2" Thick.		Ь	en 100 (1)	39.0	16 S	54.6	62 4	66 3	70.2
30 11		1	0.71	35 5	42 6	49.7	56 S	60.4	63 9
40 (1		1,	0.66	33 0	39 6	46.2	52 S	56 1	59.4
0" "		1,	0.56	28 0	33.6	39 2	44.8	47 6	50.4
Partition, Hollow Tile 1/2" Plaster both sides	2" Thick	b		20.5	24 6	28 7	32 8	34.9	36 9
Latition, Honow The 78 1 mater both and	40 11	b		16.5	19.8	23 1	26.4	28.1	29.7
	6" "	h	0.28	14.0	16.8	19.6	22 4	23 8	25 2
Stud, Lath and Plaster on one side	C)	n!	0.60	30.0	36.0	42.0	48.0	51.0	54.0
Lath and Plaster on both sides.		0	0.34	17.0	20.4	23.8	27.2	28.9	30.6
Solid Plaster 2" Thick		h		30 0	36.0	42.0	48.0	51 0	54.0
3" (1		b	0.50	25.0	30.0	35.0	40.0	42.5	45 0
Floor, Single 3/" no Pluster beneath Joists.		a	0.45	22.5	27.0	31.5	36.0	38.3	40.5
Lath and Plaster beneath Joists.		8	0.26	13.0	15.6	18.2	20.8	22.1	23 1
Double 11/2" no Plaster beneath Joists.		8	0.31	15.5	18.6	21.7	24.8	26.4	27.9
Lath and Plaster beneath Joists.		8	0.18	9.0	10.8	12.6	14.4	15.3	16.2
Single on Brick Arch.		b	0.15	7.5	9.0	10.5	12.0	12.8	13.5
Fireproof construction.		b	0.10	5.0	6.0	7.0	8.0	8.5	9.0
Concrete on Brick Arch.		b	0.20	10.0	12.0	14.0	16.0	17.0	18.0
Laid on Ground		6,51	17. 247	80.0			10,11		
Cement or Tile laid on ground no Wood ab	WWO.	al	0.31	15.5	18.6	21.7	24.8	26.4	27.9
Wood Floor	alvara	8	0.10	5.0	6.0	7.0	8.0	8.5	9 ()
Dirt, no Floor whatever	4887474.0	8	0.20	10.0	12.0	14.0	16.0	17.0	18 0
Roof. Tile 1" Thick		B	0.80	40.0	48.0	56.0	64.0	68.0	72 0
Hollow Tile, 6" thick, Concrete 8" thick, tar	and arrayo	wer		17.5	21.0	24.5	28.0	29.8	31.5
Slate on 1º Planks	min Riman	- 60	0.42	91 5	95.0	30 1	34 4	26 6	38 7

	Slate, on 1° Planks.	a	0.43	21.5	25.8	30.1	34.4	36.6	38	
	" on Wooden Framing.	8	0.85	42.5	51.0	59.5	68.0	72.3	76	
	Tar, Paper and Gravel on 2" Planks.	a	0.26	13.0	15.6	18.2	20.8	22.1	23.	1
0	Sheet Iron.	a	1.20	60.0	72.0	84.0	96.0	102.0	108.	0
	Corrugated Iron.	al	1.50	75.0	90.0	105.0	120 0	127.5	135	0
	Concrete with Cinder Fill. 2" Thick.	al	0.80	40.0	48.0	56.0	64.0	68.0	72.	0
	4" "	8	0 60	30.0	36.0	42 0	48.0	51.0	54	ĺ
	80 11	8	0.54	27.0	32.4	37.8	43.2	45.9	48.	1
	Asbestos Shingles on 1° Torque and Groove Boards.	(*	0.30	15.0	18.0	21.0	24.0	25.5	27.	(
Aja:	x Built up Roofing, 3 ply, on 4° Concrete with two layers			25.4	30.5	35.6	40.6	43 2	45	-
Ti			0.303		18.2	21.2	24.2	25.8	27.	0
		C	0.30	15.0	18.0	21.0	24.0	25.5	27	. {
	with two layers.	,								
	" of Double Neptune Felt.	e	0 21	10.5	12.6	14.7	16 S	17.9	18	4
A	uthority:a, Buffalo Forge Company. b, American Secrety of H	1 40	ing and	Venulse	mg Engm		dins-Mai	ville Comp	7373	



# Properties of Dry Air Barometric Pressure 29.921 Inches

To t que fixture Dispress Later,	Weight per Ca Ft Pos	Per Cent of Velume at 708 F.	B. T. U. Absorbed by ore Cu. It. Dry Arr per Degree F.	Cu Fr Dry Air Warmed Om degres per B T U.	Temperature Thegrees Fahr.	Weight per Cu. Ft. Pounds	Per Centre of Voltamerat 70° F	P. F. I. Ab- collection Car Et Dry Air per Degree F.	Cu la Dry Air Warried Op. Di gree per B.T.1
()	.08636	.8680	.02080	48,08	130	.06732	1.1133	.01631	61.32
	08544	.8772	.02000	48 55	135	. Obb75	1.1230	.01618	61.81
10	.08153	22017	.02000	49.05	140	.06620	1.1320	.01605	62.31
15	08363	.8962	.02018	49.56	145	(00000	1 1 1 1 7	.01592	62.82
20	.08276	.9057	.01998	50.05	150	.06510	1.1512	.01578	113 37
2.5	08190	.9152	.01977	50.58	160	(06)(06)	1.1700	.01551	64 35
30 -	.08107	.9246	.01957	51.10	170	(1650)(1)	1.1890	.01530	65 36
3.5	.08025	.193(4)	.01938	51.60	180	(162)15	1/2080	.01506	191-10
1()	.07945	.9434	.01919	52.11	190 .	.06110	1.2270	.01484	67.40
45	.07866	.9530	.01900	52 61	200	CHSOTS	1.2455	.01462	68.41
50	.07788	.9624	.01881	53 17	220	.05840	1.2833	.01419	70.48
.).)	.07713	.9718	.01863	53.68	240	.05673	1.3212	.01380	72.46
e5()	.07640	.9811	.01846	54.18	260	.05516	1.3590	.01343	74.46
63.3	.07567	.9905	.01829	51 68	280	.05367	1.3967	.01308	76.46
70	.07495	1.0000	.01812	55 19	300	.05225	1.4345	.01274	78.50
6 - 3	.07424	1.0095	.01795	55.72	350	.04903	1.5288	.01197	83.55
×(1)	.07356	1.0190	.01779	56.21	100	.04618	1.6230	.01130	88.50
5.5	.07289	1.0283	.01763	56.72	450	.04.084	1.7177	.01070	93.46
5913	.07222	-1.0380	.01747	57.25	500	.04138	1.5113	.01018	98 24
95	.07157	1.0472	.01732	57.74	550	.03932	1 90660	.00967	103.42
[400]	.07093	1.0570	.01716	58.28	600	.037.46	2.0010	.00923	108 35
105	.07030	1.0660	.01702	58.76	700	.03423	2.1900	.00817	148 07
110	.06968	1.0756	.01687	59.28	800	.08151	2.3785	.00782	127 88
115	SHEED,	1.0850	.01673	59.78	900	.02920	2.5670	.00728	137.37
120	.06848	1.0945	.01659	60.28	1000	.02720	2.7560	.00680	147.07
125	.06790	1.1040	.01645	60.79	1200	.02392	3.1335	.00603	165.83

### Properties of Saturated Steam

Pemperature F.	Approximate Gauge Pressure	Density	Specific Volume Cubb Feet Per Pound	Heat of Liquid B. T. U.	B. T. H.	Total Hea B. T. U.
212	()	0.03732	26.79	180.0	970.4	1150.4
215	1	0.08945	25 35	183.0	468.4	1151.5
219	2	0.04243	23.57	187.1	965.9	1152 9
()()()	2 3	0.04477	22.34	190.1	963.9	1154.0
224		0.04640	21.55	192.1	962 6	1154.8
207	- <b>1</b> -5	0.04892	20.14	195.2	960.7	1155.8
230	6	0.0516	19.39	195.2	955 7	F156.9
232	7	0.0534	18.72	200.2	957.4	1157.6
*)·1·2·2·3	S	0.0562	17.78	203.2	9554	1158 7
237	0	0.0582	17.17	205.3	954.1	1159 4
239	10	0.0602	16.60	207.3	952 8	1160.0
250	15	0.0724	13.82	218.5	945.3	1163.8
259	20	0.0837	11.95	227.6	939.1	1166.7
267	25	0.09049	10.54	205.8	933.5	1169.3
274	30	0.1057	9.46	242.9	928.6	1171.5
281	3.5	0.1174	8.51	250.1	923.5	1178 €
257	40	0.1283	7.79	256.2	919.1	1175.3
208	50	0.1504	6.65	267.5	911.0	1178 3
307	60	0.1707	5 16	276.8	904.2	. 1181.0
316	70	0.19(30)	5.19	286.1	×97.3	1183.3
324	50	0.2148	1.66	294.3	5910	1185.4
3331	500	() 2.15.3	1.250	301.6	11.5.5	1187.1
11.15	100	0.2575	3 554	308.9	879.9	11888
344	110	0.2778	3 o(H)	315.1	\$75.1	119002
350	120	0.2992	3.312	321.4	\$70.1	1191.3
256	1014	0.3221	3 105	327.7	867.2	11923
301	140	0.3123	2.022	3.12.9	861.0	1198 9

Condensed from Marks and Davis Steam 1.31 s.

FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

### Weight per Lineal Foot for Galvanized Iron Pipes

U. S. Standard Gauge

Di ameter of	Square Feet per	1		NUMBER (	OF GAUGE		
Piper	Ray day Food	24	21	20	20	18	11.
*567 59 10 112 13 14 56 17 12 19 19 19 29 29 25 10 17 25 19 10 112 13 14 56 67 59 10 112 13 14 56 67 10 19 19 19 29 29 25 10 17 25 19 10 112 13 14 56 67 10 10 10 10 10 10 10 10 10 10 10 10 10	1 13 1 .86 1 .95 1 .91 2 .18 2 .44 2 .76 2 .44 2 .76 2 .44 2 .76 2 .44 2 .76 2 .44 2 .76 2 .46 2 .76 2	1.39 5 1 1 4 7 5 2 2 8 1 7 7 0 2 7 1 4 5 9 2 7 1 5 1 1 1 1 1 2 2 2 2 2 3 3 3 7 4 4 5 5 5 5 5 6 6 6 6 6 6 7 7 7 7 8 8 8 8 8 9 9 9 9 10 10 10 10 11 11 12 12 13 13 14 14 15 15 15 15 16 16 17 17 18 19 10 10 10 11 11 11 11 11 11 11 11 11 11	1.50 1.48 1.48 1.48 1.48 1.50 1.48 1.50 1.50 1.50 1.50 1.50 1.50 1.50 1.50	S' Dan, 24 Ga 17 0 22 0 17 1 20 1	1.2435.44.812.72.813.051.014.72.0104.813.72.004.014.813.72.014.812.72.813.051.014.72.0104.73.72.014.813.72.014.7	这里在新山口2分的山坳22024区的建筑的有足口的设置了跨近7228区域设置的现象是多点的各种水的现象的可能是多种的通过设备的和1220分的山坳22024区的建筑的有足口的设置了1220区域设置,1220区域	10.2.5.7.4.11.7.33.4.5.7.7.4.5.11.7.5.5.7.1.1.1.7.5.1.2.5.0.7.0.4.5.2.5.3.0.0.7.5.4.0.0.7.5.4.0.0.7.5.4.0.0.7.5.4.0.0.7.5.4.0.0.7.5.4.0.0.5.7.4.4.6.5.7.4.4.6.5.5.5.5.5.6.0.0.3.3.4.4.5.5.6.0.0.7.5.4.6.0.0.7.5.4.6.0.0.7.5.4.6.0.0.0.7.5.4.6.0.0.0.7.5.4.6.0.0.0.7.5.4.6.0.0.0.0.7.5.4.6.0.0.0.0.0.0.7.5.4.6.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0.0
Wright	pur Segment Land	1 461	1.01	1.50	1.75	2 30	2.70

Weights in The Average Problems ag 11

### Weight of Black Steel Pipes in Pounds (Avor.) per Running Foot

Din.	Material			NUMBE	R OF GAUGE	, U. S S		
Pipe	Si Ft per Running Ft.	No. 24	No. 22	No. 20	No. 18	No. 46	No. 14	No. 12
4	1.13	1.30	1.58	1.86	2.43	2.99	3.62	5 08
5	1.39	1.60	1 95	2.29	2.99	3.68	4.45	6.25
G	1 65	1.90	2.31	2.72	3.54	4.36	5.28	7.42
7	1.91	2.20	2.67	3.15	4 10	5 05	6.11	8.58
8	2.18	2.50	3.05	3.60	4.68	5.77	6.97	9.80
5)	2.44	2.80	3.42	4 03	5.25	6.47	7.80	10.98
10	2.70	3.10	3.78	4.45	5 80	7.15	8.61	12.15
11	2.96	3.40	4.15	4.88	6.36	7 85	9.47	13.31
12	3.22	3.70	4.50	5.31	6.91	8.52	10 30	14 48
				5.74	7.48	9.21		15.66
13	3.48	4 00				9.21	11 15	16 81
14	3.74	4.30	5.23	6.17	8.03		11.97	
15	4.01	4.61	5.61	6 61	8 61	10 61	12.83	18 03
16	4.27	4.91	5.97	7.04	9 16	11.29	13.65	19.17
17	4.53	5.21	6 35	7.48	9 74	12.00	14,49	20.40
18	4.87	5.60	6.81	8 03	10.45	12 89	15.55	21.90
19	5.14	5.91	7.20	8.48	11 04	13 60	16.42	23 10
20	5.40	6.21	7.56	8,90	11.60	14 30	17.26	24.30
21	5.59	6.43	7.83	9.22	12 00	14.80	17.87	25.10
22	5.92	6.80	8.28	9.75	12.70	15 65	18 90	26 60
23	6.18	7.11	8.66	10.20	13 29	16 38	19 80	27.80
24	6.45	7.41	9.04	10 63	13.85	17.08	20 65	29,00
25	6.71	7.71	9.40	11.06	14.40	17.75	21 50	30 20
26	6.97	8.01	9.75	11 48	14.96	18.41	22.30	31 30
27	7.23	8.31	10.11	11 93	15.51	19.12	23.10	32.50
28	7.50	8.62	10.50	12 38	16.10	19.87	24.00	33.75
29	7.75	8.91	10.85	12.78	16 67	20.50	24 80	34.90
30	8.10	9.32	11.34	13.37	17.40	21.45	25.90	36 40
31	8.36	9.61	11.70	13.80	18 00	22 15	26.75	37.60
32	8.62	9.92	12.07	14.25	18 52	22.83	27.60	38 S0
33	8.88	10.21	12.45	14 66	19 10	23 50	28 40	40 00
34	9.15	10.21	12 81	15.10	19.68	24 43	29 30	41 20
35	9.41	10.82	13.18	15.51	20.20	24.90	30 10	42 30
36	9.67	11.11	13.54	15 95	20.78	25.60	30 90	43.50
				16.40	21 38	26 30	31.80	44.70
37	9 93	11.42	13 90					45.80
38	10.19	11.71	14.28	16 SO	21.90		32 60	
39	10 46	12.03	14 65	17.27	22.50	27.74	33 50	47.10 48.25
40	10.72	12.33	15.00	17.70	23.01	28.40	34 30	
41	10.98	12.62	15.38	18 11	23 60	29.10	35.10	49.40
42	11.24	12 93	15.75	18 55	24 20	29.80	36 00	50 60
43	11.59	13.32	16.21	19.10	24 90	30.70	37.05	52.10
44	11.85	13.64	16.60	19.55	25 50	31,40	37.90	53.30
45	12.11	13 93	16 97	20.00	26.00	32 10	38.75	54.50
46	12.37	14.23	17.31	20.40	26.60	32 80	39 60	55.70
47	12 63	14 52	17.70	20.85	27.20	33.45	40 40	56 80
48	12.90	14 83	18.07	21.30	27.75	34 20	41.30	58.00
49	13.15	15.11	18,40	21.70	28.25	34.80	42 10	59.20
50	13.41	15.42	18 80	22 15	28.80	35 35	42.90	60.40
51	13.66	15.71	19.13	22.55	29,40	36 20	43.75	61.50
52	13 94	16 01	19 50	23.00	30 00	36 90	44,60	62,65
54	14.46	16 62	20 25	23 85	31.10	38.30	46 30	65,00
56	15.07	17.32	21.10	24 85	32.40	39.90	48 20	67 80
58	15.58	17.91	21.80	25.70	33.50	41 30	49.80	70.20
60	16.12	18 53	22.60	26 65	34.70	42.75	51.60	72 60
62	16.65		23.30	27.50	35 80	44.10	53 30	75.00
64	17.16	19.16 19.72	24.00	28.30	36 90	45 50	54 90	77.20
66	17.66		24 70	29 15	38.00	46 80	56 50	79.40
68	18.21			30 00	39 15	48.25	55 30	81.80
70			25 50 26 25	30 90	40 30	49.70	60 00	84.30
72	18.75 19.25	21 55 22 15	26 25 27 00	31 80	41.40	51.00	61 60	86 60
74	19.79		27.70	32,65	42.60	52.40	63 30	89 00
9.1	10.70	22.75	40.00	92,00	Tai . 1317	*7	1407 1307	1

. Q. Poly

### FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

#### Carrying Capacity of Pipes

This table specifies the diameters of pipes required for the passage of stated volumes of air at given velocities. The column, "Cubic feet of air per minute," indicates various quantities of air to be moved per minute. The figures at top of table give the velocities in feet per minute at which the air is to be moved, and the figures in the body of the table state the required diameters of pipes for the passage of the volumes mentioned at the given velocities.

DIAMETER	6322	SPESSES.	133	2 32 6 12 2 4 5
121/10/10 14 14 14 14	5 7 10	6 6 6 6 6	4 . 7	1.55 1111.

Culor Feet)					VI	SLOC	ITIE	15					Cubic Feet				VEL	ocr:	THES			
of Air per Minute	200	eggs.	908	1000	1210	1500	1810	2000	25001	3000	3500	4000	of Air per Minute	100	1200	1500	3 5000	9	2 1 ( ) ( ) ( )	- KK	3,000	Calda.
21 H 1 GER	9 13 15 N 20 1 22 3 2 2 2 2 3 N 20 2 2 3 N 20 2 N 20 N 20 2 N 20	711462021824577250000288455567789040	7 10 2 1 1 16 7 1 N 2 2 1 2 2 3 2 4 5 5 6 7 2 2 2 3 3 4 4 3 3 5 5 5 6 6 7 3 7 8 8 8 9 3 8 9 0 0 0 4 1 1 4 2 3 3 3 3 4 4 3 5 5 6 7 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	7 9 11 3 14 5 16 8 19 20 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	680222116671899912255555555555555555555555555555555	68910213115151617144190001112222344455555577746888213133313132233333884443556678844435567471555535555785404	678901112344546171119971111222233444555566727111224800000033111123223386784444311647145658667656	67 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 7 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 7 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 8 9 10 1 1 2 3 1 3 1 4 5 1 6 6 7 8 9 10 1 2 3 1 3 1 4 5 1 6 6 7 8 9 10 1 2 3 1 3 1 5 1 6 6 7 8 9 10 1 2 3 1 3 1 5 1 6 6 7 8 9 10 1 2 3 1 3 1 5 1 6 6 7 8 9 10 1 2 3 1 3 1 5 1 6 6 7 8 9 10 1 2 3 1 7 8 1 8 1	667 8 9 10 11 11 21 33 34 55 55 56 667 8 8 8 9 9 9 9 9 9 9 2 2 2 2 2 2 2 2 2 2	6678890011122333411555666777884899500011111122235554411455554890123111223	666789900111122233311115556867777777778899990000000000000000000000	6 6 6 7 7 8 9 9 10 10 11 11 11 12 12 13 13 14 14 14 15 15 16 16 16 17 17 17 17 18 18 18 18 18 18 18 18 18 18 18 18 18	31000 32000 33000 35000 35000 35000 35000 35000 35000 35000 36000 36000 40000 40000 50000	777 78 78 72 78 78 78 78 78 78 78 78 78 78 78 78 78	690233456789912233456678900011236456667899999	033 615 667 K 9 0 0 1 1 2 2 3 3 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	577 589 660 665 666 667 689 700 771 772 773 80 770 771 773 80 770 771 773 80 770 771 773 80 770 770 770 770 770 770 770 770 770	555565788966612335455566768869890717722737777777777779991122233347554867788889960113	4.4.6.2.1.1.1.1.1.1.1.1.1.1.1.1.1.1.1.1.1.1	445461717×49.0005112253445555667778889000012223334446666677888000770777777777777777777777	11124441445666774×446660555525354455566675775×5566666111002686666666666666667656566667777777777777	

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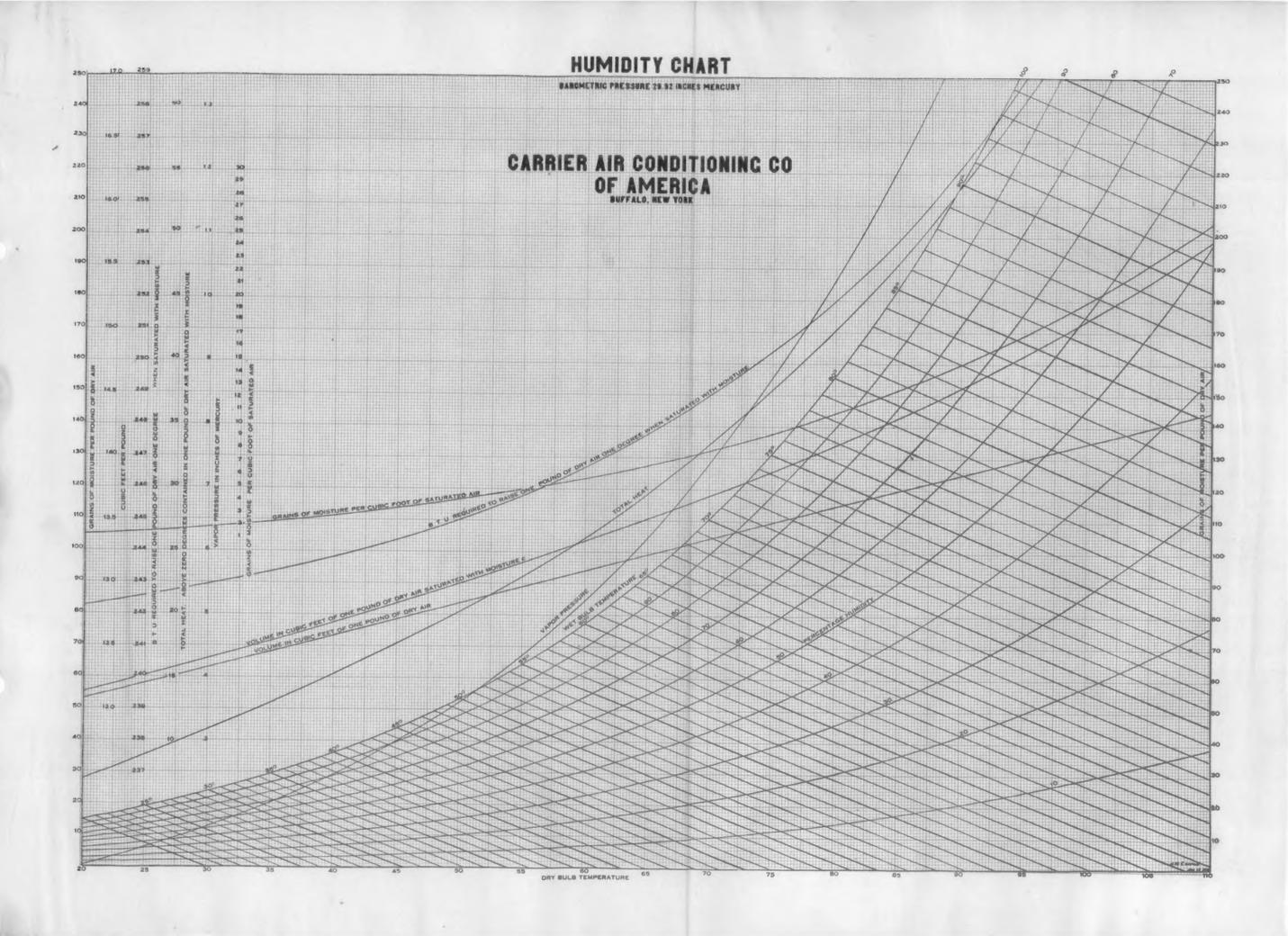
FAN SYSTEM OF HEATING, VENTILATING AND HUMIDIFYING

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HUMIDITY CHART CARRIER AIR CONDITIONING CO OF AMERICA 16.6 L 286 P 170 180 190 200 DRY BULB TEMPERATURE



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